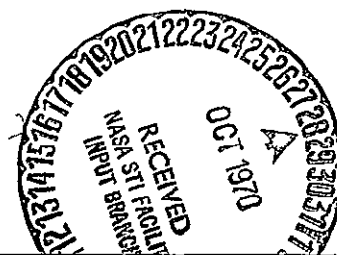
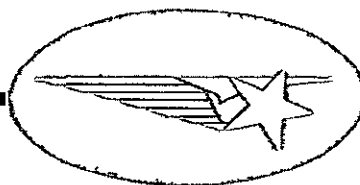


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CR-102P53
SCALING PARAMETERS FOR THE
SIMULATION OF HIGHLY EXPANDED
ROCKET EXHAUST PLUMES AND
THE RESULTANT IMPINGEMENT
FORCES ON AN IMMERSED BODY


July 1970

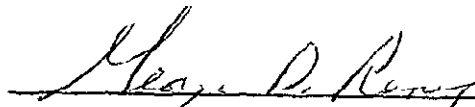
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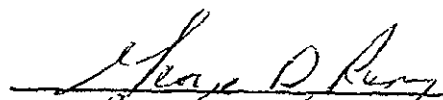
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FOREWORD

This document presents results of work performed by Lockheed Missiles and Space Company, Huntsville Research and Engineering Center under Contract NAS8-24437, Scaling Parameters/Low Density Plume Impingement Force Data, to the Aero-Astroynamics Laboratory of NASA/Marshall Space Flight Center. The Technical monitor was Mr. V. K. Henson of the Aero-Astroynamics Laboratory.

SUMMARY

Literature dealing with the proper scaling of rocket exhaust plumes with nonreacting gas mixtures is reviewed. From this background, a technique was developed to select gases which will properly simulate a region of a prototype plume, and the technique is outlined. A gas simulant selection computer program is then presented and discussed. The computer program performs the gas simulant selection based upon the parameter desired to approximate, i.e., impingement forces, Mach number, or Reynolds number. Results of this program for two typical engines are discussed.

A specific parameter of a region of a prototype plume can, in general, be simulated. In particular, the momentum flux of a plume appears to be rather easily duplicated for a definite region of a plume. Typical selections resulted in about a three percent error in momentum flux. This result lends credence to the goal of simulating experimentally the impingement forces of high altitude plumes on orbital bodies.

In addition, the Mach number may possibly be simulated by adjusting gas composition and chamber temperature. (These results are based on the possibility of simulating the condensation phenomena.) This simulation does appear to be feasible if the chamber properties can be varied enough to match the point of vapor saturation in the flow field.

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NOMENCLATURE

Symbol

a	speed of sound
A	area
C_v	specific heat at constant volume
C_p	specific heat at constant pressure
D	diameter dimension
E	constant defined by equation of text
f_1	scale factor for the 1 th parameter
F	force
g	number of molecules per drop
G	generalized function
h	specific enthalpy
H	enthalpy
J	drop formation rate
k	Boltzmann's constant
Kn	Knudsen number
ℓ	representative length
m	mass of molecular of vapor
\dot{m}	mass flux of gas
M	Mach number
n	weight fraction
N	constant defined by equations of text

N_g	fractional condensation rate
P	pressure
Pr	Prandtl number
r	radius
s	radial distance from exit plane of nozzle
SF	geometric scale factor
T	temperature
v	velocity
V	volume of drop
X	axial direction

Greek

α	Knudsen number correction factor
β	momentum correction factor
γ	specific heat ratio
δ	boundary layer thickness
ζ	surface tension
θ	flow angle
λ	molecular mean free path
μ	viscosity
ν	Prandtl-Meyer expansion angle
ρ	density of gas
σ	collision cross section of molecule
ϕ	nozzle lip angle
ψ	molecular weight of gas

Subscripts

a	ambient conditions
cont	continuum flow conditions
d	drop
e	exit plane
FM	free molecular flow conditions
liq	liquid
m	model
o	stagnation conditions
p	prototype
S_{∞}	stagnation condition for drop of infinite radius
t	throat conditions

Superscript

*	denotes drop of critical size
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INTRODUCTION

Orbiting vehicles of the Apollo Applications Program and other space programs are generally maneuvered by reaction control rocket engines. In many cases, interaction and impingement of the exhaust plumes on the parent vehicles create control thrust degradations in conjunction with undesirable reaction forces and moments. If these plume impingement effects are not defined, inadequate control systems may result. Since orbiting vehicle configurations are generally complex (including extensive external hardware such as solar power cells, communication antennas, etc.) theoretical procedures for predicting vehicle plume impingement forces are quite complicated. By analyzing properly simulated experimental investigations, impingement forces on complex structures can be adequately defined. Because full-size tests are costly and complex, scale model testing should be used. To have "proper simulation," the tests should provide good scaled simulation of both the vehicle and the plume, otherwise techniques for applying the test results to a full-scale condition must be developed. There are, however, two primary problems involved in this simulation. One involves scaling a model in the flow field, (the same problem is encountered in conventional wind tunnel testing of aerodynamic configurations and is scaled on the basis of Reynolds number and Knudsen number), the second problem involves simulating the gas dynamics of the flow properties of the rocket exhaust plume. Both problems must be satisfactorily resolved in order to obtain correctly scaled impingement forces from scale model testing.

The exhaust plumes of a rocket that operates in a near vacuum are characterized by three flow regimes, (1) continuum center portion, (2) a transitional regime surrounding the continuum region, and (3) a highly expanded free molecular regime which may include flow expanding to a direction more than 90 degrees away from the nozzle centerline. The

experimental evaluation of the forces on bodies from such plumes requires that the local plume parameters and model parameters be scaled exactly, or that techniques be provided to relate and correct the test results to full-scale conditions. The basic problem is complicated by the fact that in many instances (due to test facility limitations) the plume itself will be modeled with a gas which is different than that of the full scale system. Gas dynamic relationships between the model and the full-scale system must therefore be established in terms of

- Plume gas dynamic properties
- Reynolds number of the model in the plume
- Knudsen number of the model in the plume
- Scale model motor chamber conditions and nozzle geometry
- Condensation considerations

With these facts in mind a survey on plume scaling was made of state-of-the-art literature. Using results of the survey as a base, a computer program was written which performs a rapid search of possible simulant gas mixtures and selects the mixture that best simulates the prototype plume based on Mach number and momentum considerations. The impingement forces predicted by the model simulation are then adjusted by a momentum correction factor to account for discrepancies in the gas dynamic simulation.

In the following technical discussion, the more important sources of information are discussed, techniques used in the computer program to test and select a gas mixture are outlined and two sample cases that have been run to provide experience with the method are presented. Results for these two cases show that a simulant gas mixture can be selected which will approximate in a scaled experiment the impingement forces on a body immersed in a prototype nozzle plume.

Section 2 TECHNICAL DISCUSSION

An integral part of the plume scaling study was a literature survey carried out to obtain a working knowledge of accomplishments in the past several years in the field of scaling techniques. Thus, before the approach taken in the current study is described, the work carried out by others is outlined. Problems or limitations of the existing methods are examined, which have pointed the way to development of the procedures used in the current effort. The work applicable to this study is centered in two areas (1) general scaling of plumes, and (2) analytical models of the plume. These subjects are discussed in the following subsections.

2.1 LITERATURE REVIEW

Templemeyer (Ref. 1) performed a most pertinent study of the simulation of hot jet exhaust with mixtures of cold gases. Since the exact parameters that need to be satisfied in order to simulate one gas with another are not readily obvious, Ref. 1 examined a gaseous flowfield and found that by equating specific heat ratio, specific internal energy, pressure ratio and mass flow per unit area, the simulation between a prototype and model was achieved at the exit plane of a nozzle. By assuming a perfect gas with constant specific heats, the equations can be reduced to a set of three linear algebraic equations with weight fractions as the unknowns. Reference 1 then solved the following set of equations:

$$C_{vp} (T_{op}/T_{om}) = n_1 C_{v1} + n_2 C_{v2} + n_3 C_{v3} \quad (1a)$$

$$R_p (T_{op}/T_{om}) = n_1 R_1 + n_2 R_2 + n_3 R_3 \quad (1b)$$

$$1 = n_1 + n_2 + n_3 \quad (1c)$$

where the simulant mixture is made up of three gases. By selecting a combination of gases Eqs (1) can be solved to provide the weight fractions, N_1 . If the weight fractions are all real numbers, the gas mixture is a possible simulant.

With the solution of the above equations, the inviscid flow of a nozzle can be simulated for certain cases. The boundary layer thickness ratio (δ/D_e) can be duplicated by duplicating the Reynolds number, or

$$\rho_M \sqrt{\frac{\gamma P}{\rho}} \frac{l}{\mu} \bigg|_p = \rho_M \sqrt{\frac{\gamma P}{\rho}} \frac{l}{\mu} \bigg|_m \quad (2)$$

Since

$$M_p = M_m, \quad \gamma_p = \gamma_m, \quad P_p = P_m$$

is assumed, then

$$l_m = l_p \left(\frac{\mu_m}{\mu_p} \right)$$

Now since the viscosity of a hot exhaust gas is generally large compared to a cold gas mixture, it is difficult to achieve Reynolds number duplication if the nozzle length is to scale. As a result, Ref. 1 resorted to computing a scale factor by which the nozzle length is varied in order to achieve viscous similitude. For example in Ref. 1 a turbulent boundary layer was assumed and then the boundary layer thickness was expressed as

$$\delta = l / R_N^{0.2}$$

and

$$\delta_p (SF) = \delta_m$$

Then

$$\left(\frac{l}{\rho u \mu} \right)^2 \bigg|_p (SF) = \left(\frac{l}{\rho u \mu} \right)^2 \bigg|_m$$

Reducing

$$\ell_m = \left[(SF) \left(\frac{\mu_p}{\mu_m} \right)^{0.2} \ell_p^{0.8} \right]^{1.25}$$

Thus the viscous and inviscid one-dimensional flow properties will be duplicated at the exit plane. Several combinations of hydrocarbons were then found that fulfilled the necessary requirements for simulation of the exit plane properties of a turbojet engine.

Marsh (Ref. 2) developed a technique for searching for combinations of gases that duplicate the exit plane conditions of a rocket nozzle to provide plume flowfield simulation. Real gas effects were included in the analysis by a variable ratio of specific heats. Basically the following three similarity laws involving P , M , and μ were satisfied:

$$\text{Pressure Ratio} \quad (P_a/P_e)_m = (P_a/P_e)_p \quad (5a)$$

Nozzle Lip Turning Angle

$$\left. \frac{\gamma_e M_e^2}{\sqrt{M_e^2 - 1}} \right|_m = \left. \frac{\gamma_e M_e^2}{\sqrt{M_e^2 - 1}} \right|_p \quad (5b)$$

Viscosity

$$\frac{D_p}{D_m} \sqrt{\frac{\ell_m}{\ell_p} \left(\frac{\mu_m}{\mu_p} \right) \left(\frac{\rho_m}{\rho_p} \right) \left(\frac{u_m}{u_p} \right)} = 1 \quad (5c)$$

These requirements reduce to the necessity of duplicating γ_e , M_e , and $(\rho u / \mu)_e$. Reference 2 computed these parameters as a function of pressure ratio, chamber temperature and gas mixture. By plotting the data it was possible to determine graphically a binary or ternary mixture of gases which approximate the prototype conditions. The gas mixture generally contained one gas with a low specific heat ratio and one with a high specific heat ratio.

Gopin (Ref 3) was also interested in duplicating flowfield conditions near the exit plane of a rocket nozzle and he included the additional requirement that the impingement forces due to the exhaust gases shall be similar. With this in mind, Ref 3 then specified that the momentum flux per unit area be similar

$$\text{That is, momentum flux} = \rho u^2 A \quad (6a)$$

$$\text{Since} \quad \rho = P / RT$$

$$u^2 = a^2 M^2 = \gamma R T M^2$$

$$\text{Then, momentum flux} = \gamma M^2 P A \quad (6b)$$

Equating prototype and model conditions

$$\gamma M^2 P \Big|_p = \gamma M^2 P \Big|_m \quad (6c)$$

Reference 3 points out that by choosing high density gases, which is almost synonymous with gases having multiple species, a high mass flow rate can be attained. Assuming isentropic perfect gas relationships, Ref 3 shows that

$$\begin{aligned} m/A &= \rho u = P / RT \\ m/A &= \frac{P_o}{\left(1 + \frac{\gamma-1}{2}\right)^{\gamma/\gamma-1}} \sqrt{\frac{\gamma}{RT_o \left(\frac{2}{\gamma+1}\right)}} \\ &= \sqrt{\left(\frac{\gamma+1}{2}\right)^{-\left(\frac{\gamma+1}{\gamma-1}\right)}} P_o \sqrt{\frac{\gamma}{RT_o}} \end{aligned} \quad (7)$$

If P_o , T_o , and γ are assumed to be constant, then mass flow is a direct function of molecular weight. Choosing polyatomic gases (multiple atomic species) provides a high mass flow per unit area with a low flow rate of molecules. Thus, it becomes much easier to maintain a vacuum

chamber at a high simulated altitude, (i.e., low pressure) for a longer period of time. Finally, to avoid condensation the simulant gas mixture was heated.

With these stipulations in mind, Ref. 3 selected several binary gas mixtures from a group of gases that were presumed to have desirable simulation traits. An experimental program was undertaken using a mixture of argon and sulfur hexafluoride to simulate the exhaust gases of the J-2 engine. Force measurements were made for impingement of the exhaust on an S-II afterbody. The major results of interest here are

- Generally there was little change in forces due to a change in specific heat ratio from $1.18 \leq \gamma \leq 1.28$, but there was significant variation for $1.28 \leq \gamma \leq 1.40$.
- Although changes in γ result in modifications of the momentum distribution in the exhaust flow field, very small variations have little effect on impingement forces. Hence, minor errors in the gas mixture used to simulate γ are negligible.

Note that in Ref. 3, $M_{ep} = M_{em}$, and thus for similarity, $\gamma_{ep} = \gamma_{em}$. The authors admit that simulating the exit plane momentum by simulating the specific heat ratio is only an assumption, an assumption that has been justified by previous experimental work. (This point is discussed further in Section 2.2.1.)

References 4, 5 and 6 are also interested in simulating the impingement of a highly expanded plume on a nearby surface. In particular it was desired to simulate the impingement of exhaust gases from the APS ullage motor and the O_2H_2 burner motor on the J-2 engine of the S-II stage. The added requirement that non-continuum effects be duplicated makes Refs. 5 and 6 different from the works previously mentioned.

In designating the experimental conditions, nitrogen gas was selected as the simulant gas since it came closer than any other single gas to

matching the prototype engine gas characteristics. Also of importance was the fact that nitrogen is readily pumped by helium cryopanel (as are most gases except hydrogen). To achieve proper nozzle exit plane conditions area ratios were selected that would produce the proper Mach number at the exit plane. Simulation of Knudsen number throughout the flow field was obtained by duplicating the nozzle exit plane Knudsen number.

If flowfield similarity is assumed, as noted above, scaling parameters between model and prototype conditions can be computed.

First

$$K_n = \lambda / D \quad (8)$$

Where

$$\lambda \sim m / \sigma^2 \rho \quad (9)$$

Solving for ρ and writing a ratio

$$\rho_p / \rho_m = (SF) \frac{\sigma_m^2}{\sigma_p^2} \frac{\psi_p}{\psi_m} \frac{K_{nm}}{K_{np}} \quad (10)$$

Thus the density ratio provides scaling of non-continuum gas dynamics between prototype and model. To obtain a pressure scale factor between model and prototype conditions it is assumed that pressure can be written

$$P = P_{cont} + a (P_{FM} - P_{cont}) \quad (11)$$

Where a is assumed to be of the form

$$a = e^{-\frac{1}{K_n}} \quad (12)$$

and K_n is based on R_b the local body radius. Now if Mach number and momentum flux (Eq 6b) are similar, then scaling relations can be developed to match Knudsen number. Or

$$\frac{(P_s - P_{cont})_m}{(P_s - P_{cont})_p} = \frac{e^{-1/K_n}}{e^{-1/K_n}}$$

And

$$P_{s_p} = (P_s - P_{cont}) \left(\frac{a_m}{a_p} \right) + P_{cont_p} \quad (13)$$

These scaling parameters (Eqs 10 and 13) produced remarkable agreement between prototype and model conditions of Refs. 5 and 6

In Ref 7, a rocket plume was simulated by the actual combustion of gaseous fuels to simulate the exhaust of a liquid propellant rocket engine. A shock tube technique which permitted short run times was used to maintain proper background pressure. This technique provided for the duplication of stagnation enthalpy and a good approximation to the desired molecular species concentration. The Mach number in the nozzle can be reproduced by simple geometric similarity since the boundary layer was made to scale by maintaining the full scale Reynolds number. Full scale Reynolds number was attained by increasing the chamber density. This technique has several advantages, the most obvious in that the prototype species concentration can be obtained in the model plume. Also by the simple expedient of raising the chamber pressure, the proper Reynolds number can be attained. A drawback pointed out in Ref 7 is that the steady state flow conditions over a complex body with concave shapes cannot be obtained in the testing time available.

To obtain the proper mixture of gaseous reactants to duplicate the combustion products of liquid propellants, two basic rules given in Ref 8 are used

- 1 The atomic composition (i.e., atomic species and atom ratios) of the liquid and gaseous propellants must be the same
- 2 The initial energies of the two propellant combinations must be equivalent (i.e., the quantities must be the same) $\sum_{j=1}^r n_j (H_{T_1})_j$

Condition 1 is easily satisfied, however, condition 2 involves a trial and error approach to arrive at a proper mixture of gaseous components

Many techniques (Refs 1 through 7 were some of the most pertinent) have been employed to simulate the flow field of a rocket engine. Some techniques appear more applicable to the problem of this present effort for which the basic objectives of the present effort are related here. First, a mixture of non-reacting gases is used to simulate plume impingement forces for the hot products of combustion of a liquid propellant engine. Second, conditions in the far flow field of a plume are to be duplicated rather than conditions near the exit plane of a nozzle. This stipulation leads to the second section of this literature review.

2.1.1 Models of plumes

To simulate the conditions in a highly expanded plume, flowfield parameters in the far field region must be predicted. After a method is developed that permits the flow field to be predicted, various combinations of gases can be used to simulate the desired flowfield parameters of the prototype plume. Many documents first published in this area were basically interested in simulating jet boundary conditions near the nozzle. Representative reports are briefly reviewed in the following paragraphs for this problem. More extensive discussions which should prove useful in the present study, are then given to models of plumes.

Assuming that there is a finite back pressure, the expression for the Prandtl-Meyer expansion angle can be written

$$\frac{\Delta P}{P} = \frac{\gamma M^2}{\sqrt{M^2 - 1}} (\Delta \nu) + \text{higher order terms} \quad (14)$$

Thus Goethert (Ref 9) proposed to match the parameters $\gamma M^2 / \sqrt{M^2 - 1}$ and θ_j in order to duplicate the jet boundary of a highly underexpanded jet. Pindzola (Ref 10) carried out a study in which better boundary similarity was obtained by matching θ_j and $\gamma M^2 / \sqrt{M^2 - 1}$, where the Mach number is now based on the boundary conditions rather than on the nozzle exit conditions. Finally, in a later study Herron (Ref 11) concluded that even better simulation was obtained by matching the parameters θ_j and M / γ . All these results were obtained through experimental research.

As shown, these studies are not quite applicable to the problem currently under study, however, they were mentioned to underline previous work in jet plume simulation. Although the present effort is directed toward simulating plumes at high altitudes, it may prove useful at some later date to add the capability of simulating the shape of a plume near the nozzle. With this in mind, attention is now turned to the problem of similarity parameters for highly expanded plumes far downstream. Little work has been done previously in the area which is the objective of the present study.

To accomplish this objective the first task is to predict flowfield conditions for a highly underexpanded rocket nozzle of given conditions. The method-of-characteristics solution has been shown to be a highly accurate technique to describe analytically the flow field of a rocket plume. The method is accurate even for highly expanded plumes (Ref. 11). Method-of-characteristics solutions are relatively fast on a computer, however, for far field flow prediction, a source flow model has been found to be faster and to agree closely with method-of-characteristic solutions (Fig 1). A description of this method as given by Ref. 12 is next outlined.

Consider the exhaust jet of an ideal inviscid gas issuing isentropically into a vacuum. The flow is steady and the ratio of specific heats is constant. At large distances from the nozzle the streamlines seem to emanate from a source near the nozzle exit. It is then assumed that the pressure rapidly approaches zero and thus the velocity can be assumed to be constant. The

density then takes the form $\rho \sim 1/h^2$, where h is the radial distance from the nozzle exit (Fig 2 from Ref 13). It is assumed that the density on a spherical cap of distance h is of the form,

$$\rho / \rho_e = \frac{E}{2} \left(\frac{h}{r_e} \right)^{-2} \cos^N \theta \quad (15)$$

Then solving the equation of continuity and momentum for the unknown constants N and E , (Ref 12) obtains the following expression for Mach number

$$M = \left[\frac{2}{\gamma-1} \left\{ \left[\frac{E}{2} \left(\frac{A_t}{A_e} \right) \left(\frac{h}{r_e} \right)^{-2} (\cos \theta)^{E-1} \left(\frac{\gamma+1}{2} \right)^{\frac{1}{\gamma-1}} \left(\frac{\gamma-1}{\gamma+1} \right)^{\frac{1}{2}} \right]^{1-\gamma} - 1 \right\} \right]^{\frac{1}{2}} \quad (16)$$

Thus Mach number is dependent only upon the location in the flow field for a given gas and nozzle geometry. The most obvious shortcoming of this analysis is the restriction to systems with a constant ratio of specific heats

References 14 and 15 also discuss the similarity of highly expanded rocket exhausts. These references, however, are devoted to the description of flow fields inside a barrel-shaped shock emanating from the Prandtl-Meyer expansion fan. Thus, these studies are not quite applicable to the current problem which considers expansion into a vacuum.

This brief discussion concludes the literature review of simulation parameters and plume models. The techniques outlined in the next section draw liberally from the sources which were discussed. In many cases, slightly different methods are employed because of complicating factors in the problem at hand.

2.2 METHOD OF APPROACH

Obviously a simulation of a full-scale rocket plume could be attained by duplicating Reynolds number, chemical species, Mach number, stagnation

enthalpy, and environmental pressure. Noncontinuum effects would automatically be satisfied, since Knudsen number is defined by the Mach number and Reynolds number. Since in the present analysis the chemical species cannot be simulated, the Mach number distribution will not necessarily be identical throughout the prototype and model plumes. In addition, simulating stagnation enthalpy as obtained by Ref. 6 is difficult, since the extremely high total temperature attained in the prototype case is out of the range of the experimental test equipment that is available.

As an introduction to the problem of simulation, the rules of flowfield similarity are reviewed here. With this requirement in mind, the model established to analytically test a gas for simulation ability is discussed. The computer program which was written to select a simulant gas mixture is next described. Finally, analytical results comparing impingement forces predicted from model conditions are compared with those predicted for prototype conditions.

2.2.1 Similarity Parameters

For two flow fields to be comparable in the region of interest, the terms in the equations of flow must be similar. To simplify the calculations, the analysis is carried out one-dimensionally. Writing the one-dimensional flow equations,

Momentum

$$u \frac{du}{dx} = \frac{1}{\gamma M^2} \frac{dP}{dx} + \frac{1}{R} \frac{d^2u}{dx^2} \quad (17)$$

Energy

$$u \frac{dT}{dx} = \frac{1}{P_r R_n} \frac{d^2T}{dx^2} + (\gamma - 1) M^2 u \frac{dP}{dx} + \frac{4}{3} \frac{(\gamma - 1) M^2}{R_n} \frac{d^2u}{dx^2} \quad (18)$$

Equation of State

$$P = \rho RT \quad (19)$$

Continuity

$$\frac{d(\rho u)}{dx} = 0 \quad (20)$$

The equations of state and continuity add no new information to the dimensional analysis and are included only for the sake of completeness. Thus, from momentum, equivalent terms from the model and prototype situations can be equated. On

$$\gamma_p M_p^2 = \gamma_m M_m^2 = f_1 \gamma_p f_m^2 M_p^2$$

where f_1 is a scale factor for the 1th variable

Then

$$f_m = \frac{1}{\sqrt{f_1}} \quad (21)$$

Similarly, from the energy equation

$$(\gamma_p - 1) M_p^2 = (\gamma_m - 1) M_m^2 = (f_1 \gamma_p - 1) f_m^2 M_p^2$$

Or

$$(\gamma_p - 1) = (f_1 \gamma_p - 1) f_m^2$$

Substituting from the momentum equation into the energy equation yields

$$f_1 = 1 \quad (22)$$

Thus for complete flowfield similarity, all of the following parameters must be equated

$$\gamma_p = \gamma_m \quad (23a)$$

$$M_p = M_m \quad (23b)$$

$$Rn_p = Rn_m \quad (23c)$$

$$P_{rp} = P_{rm} \quad (23d)$$

Complete similarity may never be achieved, however, since the primary interest in this study is the force produced on a body immersed in a rocket exhaust plume. Conditions leading to force similarity are examined. The force exerted on a body can be written in the general form

$$F = G(\rho, u, \ell, \mu, a) \quad (24)$$

Using dimensional analysis, the expression can be written in a familiar form

$$\frac{F}{\rho u^2 \ell^2} = G\left(\frac{\rho u \ell}{\mu}, \frac{u}{a}\right)$$

If viscous effects are ignored, then

$$\frac{F}{\rho u^2 \ell^2} = G(M) \quad (25)$$

But this expression can be written in more familiar terms as the pressure coefficient

$$\frac{F}{\rho u^2 \ell^2} = \frac{\Delta P}{\rho u^2} = G(M)$$

Or

$$C_p = \frac{\Delta P}{\frac{1}{2} \rho u^2} = G(M) \quad (26)$$

Thus, for identical gases, if the Mach number is equal, the pressure coefficient C_p is identical. However, the pressure exerted on a body is also a function of gas composition or γ . In other words, pressure is a function of momentum flux ρu^2 and Mach number, where

$$T = \text{momentum flux} = \rho u^2 = \gamma P M^2 \quad (27)$$

Now, as shown in Ref. 3, the impingement pressure can be duplicated by approximating the momentum flux. This assumption is also borne out by the work of Ref. 4, in which computation of the impingement pressure by Newtonian calculations is analogous to computing the momentum flux. Thus, when a duplication of impingement pressure was desired, a simulant gas mixture has been selected on the mixture's ability to duplicate momentum flux at a point in the plume. In addition, options have been included in the computer program that will compare Mach number or Reynolds number and select a simulant gas mixture that best duplicates the parameters.

2.2.2 Gas Selection

As stated in the introduction, two objectives of the study are (1) select a binary or ternary mixture of gases to simulate in a scaled model the forces produced on a body immersed in a plume, and (2) include real gas effects in the analysis and attempt to duplicate such esoteric flowfield phenomena as condensation.

An ideal technique to strive for is to develop a closed form solution for the mixture ratios of a possible simulant gas (Ref. 1). However, since real gas effects are to be included in the analysis, this avenue of approach is closed. If as in Refs. 2, 3 and 5 duplication of exit plane conditions will

suffice to duplicate the entire flow field of interest, once again the analysis is simplified. But, as shown in Ref. 5 the immersed body is relatively close to the exit plane of the nozzle and the specific heat ratio in that region is relatively constant at 1.4. In the present study, the specific heat ratio varies from about 1.3 at the exit plane to 1.4 in the expanded region.

To duplicate this specific heat ratio, the technique suggested in Ref. 2 was adopted. Using gases suggested by Refs. 1, 3 and 16, the gases were separated by inspection into three basic groups, those which

- 1 Exhibited high γ
- 2 Exhibited low γ , and
- 3 Those that would condense relatively soon in an expanding gas

Some of the more obvious reasons for eliminating a gas from the above groups are

- 1 Toxic or easily formed toxic compounds
- 2 Cost and availability
- 3 Condensability

However, an extremely important criterion is the ability of the gas to be pumped by helium or nitrogen cryopumps in vacuum chambers. For this reason hydrogen will generally be deemed non-acceptable unless its mixture ratio in the simulant gas is very low. The actual limits are determined by the capability of the facility available for testing. One additional comment should be included concerning the thermodynamic properties of the gases used as possible simulants. Thermodynamic properties in highly expanded plumes were desirable where temperatures much below 100°K occur. Thus thermodynamic properties good down to 10°K were generated and stored on magnetic tape using the methods of Ref. 17. A list of the gases currently on the data tape which can be used as possible simulant gas components is given in Table 1.

Table 1
GASES CURRENTLY AVAILABLE FOR ANALYSIS
AS POSSIBLE SIMULANTS

Chemical Formula	Name	Molecular Weight	Ratio of Specific Heats at 1 atm Pressure
A	Argon	39.948	1.667 at 86°F
CClF ₃	Carbon Chlorotrifluoride	104.465	1.2 at 77°F
CF ₄	Carbon Tetrafluoride	88.01	1.217 at 100°F
CHF ₃	Trifluormethane	70.018	1.22 at 30°F
CO ₂	Carbon Dioxide	44.01	1.3 at 86°F
H ₂	Hydrogen	2.016	1.4 at 86°F
N ₂	Nitrogen	28.02	1.405 at 26°F
N ₂ O	Nitrous Oxide	44.02	1.303 at 59°F

2 2 3 General Discussion of Simulant Selection Program

Using a mixture of the gases the Chemical Equilibrium Composition computer program (CEC) Ref 18, calculates the thermodynamic properties of the mixture. Then utilizing a modified source flow model, the momentum flux and Mach number at a specified point in the plume are compared to those produced by the real gas under prototype conditions also in a modified source flow plume. In addition, the Reynold's number at the exit plane is computed to ensure that the boundary layer effect is similar. The boundary layer calculation is discussed later, however, the most important point to note is that automating the computations allows possible gas mixtures to be thoroughly searched. Thus not only can the mixture ratio be varied, but the stagnation pressure and temperature can be altered within specified limits. Unfortunately, if one particular gas mixture does not meet the desired specifications, another set of gases must be tried at random. However, this is the same procedure employed in Ref 1, and no real alternative appears to be available. After a set of gases is chosen for a specified chamber temperature and pressure, it is possible to determine rather quickly if any possible combination will meet the desired criteria. This calculation is described in detail in Appendix A.

Thus, after a possible gas mixture has been selected, the ability of this gas to simulate forces on a body immersed in a plume formed from these gases must be predicted. This can be done by use, again, of a source flow model of the plume.

• Plume Source Flow Model

As illustrated in Fig 1 taken from Ref 12, the flow field computed by a source flow model predicts quite well the parameters of the far flowfield region. Since real gas effects are to be included in the analysis, the technique of Ref 12 discussed in Section 2 1 could not be used to obtain a closed

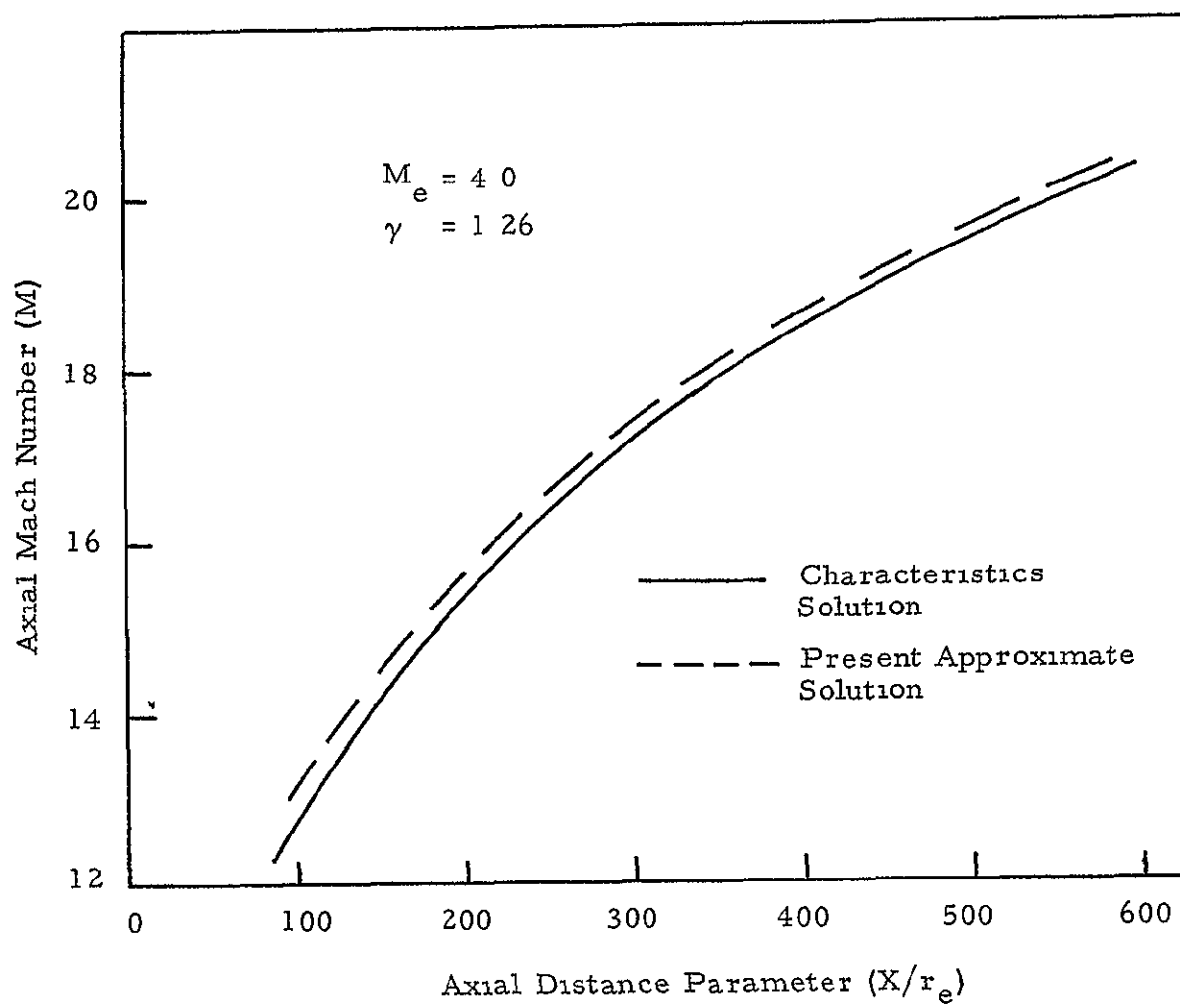


Fig 1 — A Comparison of the Approximate and Characteristics Solution for a Rocket Exhausting into a Vacuum ($M_e = 4.0$, $\gamma = 1.24$) Ref 12

form solution for the flow properties at a point. Instead, a numerical solution using the method of false position was employed to solve for the flow field properties that satisfied the specified area ratio of the flow field. In addition, rather than assuming a hemispherical flow field as Ref 12, the Prandtl-Meyer expansion angle at the nozzle lip is computed and the area ratio of the plume is calculated using this as the boundary of the plume (Fig 2). Reference 13 discusses this program more fully. The centerline Mach numbers for the R1E exhaust plume as computed by the MOC and source flow programs are shown in Fig 3 taken from Ref 13. Once again the comparison is acceptable.

After the plume is generated, corresponding points of the model and prototype plume flow fields can be compared. The technique thus produces a flexible but bulky method of determining a good simulant mixture. It should be noted, however, that not only must points in the inviscid plume be compared, but also viscous effects in the nozzle which are similar must be ensured.

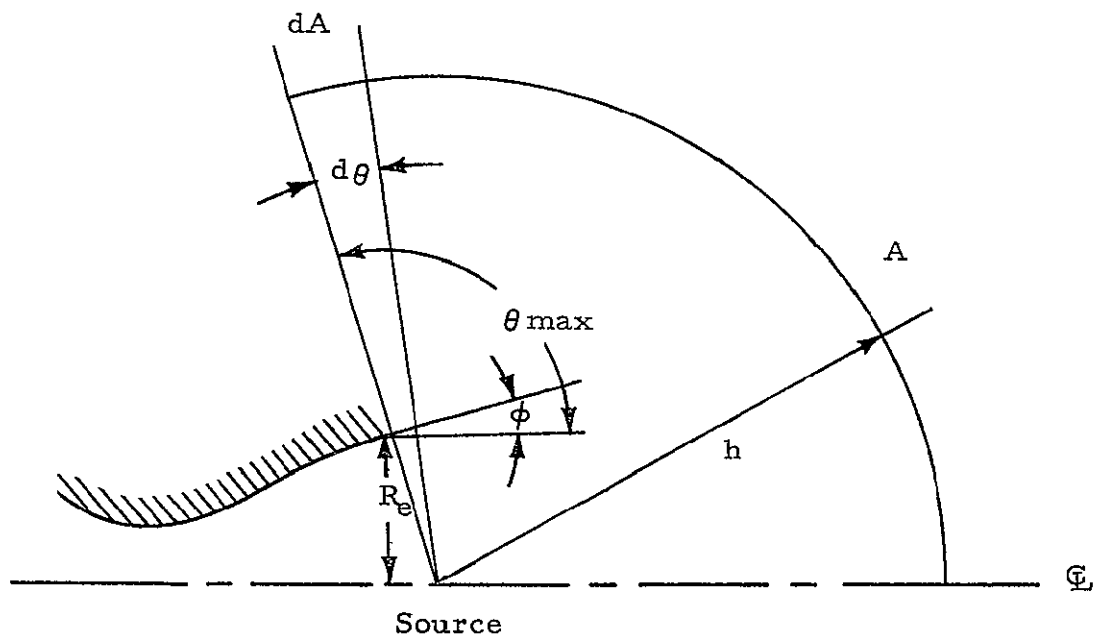
• Boundary Layer

To simulate the viscous flow effects in the nozzle the ratio, δ/D , must be equal for both model and prototype. The following analysis is carried out assuming turbulent flow in the nozzle. Similar statements can be made regarding laminar flow. In general the boundary layer thickness can be written as a familiar function of Reynolds number

$$\delta/\ell = k \left(\frac{\rho u \ell}{\mu} \right)^{-1/5} = k \left(R_\ell \right)^{-1/5} \quad (28)$$

where k is a constant for turbulent flow and R_ℓ is Reynolds number based on a characteristic length of the nozzle. Now obtaining a ratio of (δ/D)

$$\left(\frac{\delta}{D} \right) \frac{1}{\ell} = \frac{k}{d^{4/5} \ell^{1/5}} \left(\frac{1}{R_D} \right)^{1/5}$$



θ_{max} = Prandtl -Meyer Expansion Angle

ϕ = Nozzle Lip Angle

Fig 2 - Source Flow Model of Plume Showing the Model Geometry

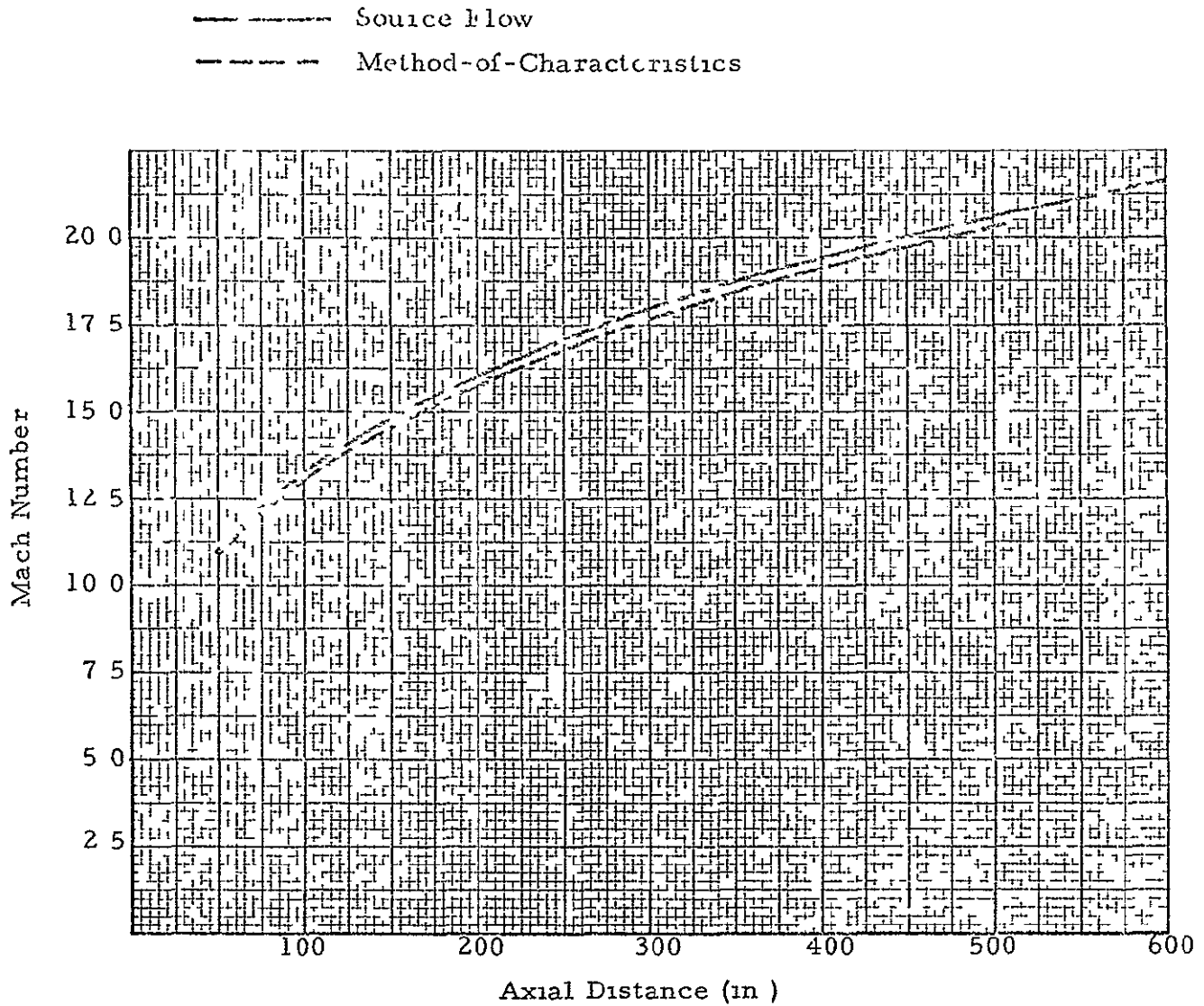


Fig 3 - Comparison of the R-1E Engine Centerline Distribution of Mach Numbers Using Data from the Method-of-Characteristics and Source Flow Computer Programs ($\gamma = 1.259$)

or

$$\left(\frac{\delta}{D}\right) = k \left(\frac{\ell}{D}\right)^{4/5} \left(\frac{1}{R_D}\right)^{1/5} \quad (29)$$

Equating the ratio for model and plume cases

$$k \left(\frac{\ell}{D}\right)^{4/5} \left(\frac{1}{R_D}\right)^{1/5} \Big|_m = k \left(\frac{\ell}{D}\right)^{4/5} \left(\frac{1}{R_D}\right)^{1/5} \Big|_p$$

Thus

$$\left(\frac{\ell}{D}\right)^{4/5} \left(\frac{1}{R_D}\right)^{1/5} \Big|_m = \left(\frac{\ell}{D}\right)^{4/5} \left(\frac{1}{R_D}\right)^{1/5} \Big|_p \quad (30)$$

Now if Reynolds number can be duplicated, then near geometric similarity assures similitude. However, from Refs. 1 and 2 it may be difficult to duplicate Reynolds number. In order to ensure viscous similarity it may be necessary to modify the length of the model nozzle, or

$$\begin{aligned} \ell_m^{4/5} &= \left(\frac{D_m}{D_p}\right)^{4/5} \ell_p \left(\frac{R_{Dp}}{R_{Dm}}\right)^{1/5} \\ &= (SF)^{4/5} \ell_p^{4/5} \left(\frac{R_{Dp}}{R_{Dm}}\right)^{1/5} \\ \ell_m &= (SF) \ell_p \left(\frac{R_{Dp}}{R_{Dm}}\right)^{1/4} \end{aligned} \quad (31)$$

In the present study the primary concern is that the boundary layer shall be no greater in the model situation than in the prototype situation. To meet this requirement, the simulant selection program specifies that the Reynolds number of the model must be equal to or greater than the Reynolds number of the prototype nozzle. Transport properties of the gases in question are computed, using the methods reported in Ref. 19.

For the sake of completeness, a modified nozzle length can be calculated after a gas mixture has been established for a specified chamber condition. Besides simulating the basic flowfield parameters (such as Mach number and Reynolds number) one other phenomenon, condensation, must be matched.

• Condensation

Generally, in highly expanded rocket plumes having temperatures well below 100°K, heterogeneous systems are of considerable importance. In particular, as the partial pressure of each gaseous component drops below its vapor pressure, the probability of the formation of liquid droplets increases. In general, the theory of condensation is felt to be understood. In fact, calculations of condensation in steam nozzles or of water vapor in air seem to bear out this theory. See for example Refs. 20 and 21. Unfortunately, corresponding calculations cannot be as easily made for the gaseous substances such as nitrogen or carbon dioxide. Much of the problem lies in the lack of accurate knowledge of material properties such as surface tension and density. The problem may be illustrated by writing the expression for fractional formation rates (Ref. 20)

$$\frac{1}{N_g} \frac{dN_g}{dT} = g^* \frac{J(g^*)}{N_g} = \frac{P}{kT} \frac{4r_d}{3} \sqrt{\frac{2\pi\zeta}{m}} e^{-4\pi\zeta r_d^2 / 3kT} \quad (32)$$

The dominant term in the expression is the exponential

$$e^{-4\pi\zeta r_d^2 / 3kT} \quad (33)$$

which may be written

$$e^{-16\pi\zeta^3 V_{liq}^2 / 3(kT)^3 \ln(P/P_{s\infty})} \quad (34)$$

Since surface tension ζ is a cubed quantity, any error in it greatly alters the computed condensation rate

Because of this problem, no attempt was made to match condensation rate. Rather, an attempt was made to duplicate only the location of condensation. Currently condensation is assumed to occur when the partial pressure of the gaseous species drops below the vapor pressure for that corresponding temperature. The point at which condensation occurs is modified by adjusting the chamber temperature. Since this adjustment could upset simulation of impingement forces or viscous effects, it is carried out last. Noncompliance with the condensation requirement does not eliminate the gas mixture, however, the search is continued for other combinations that might better duplicate the prototype flow field.

This concludes a brief description of the approach taken to simulate a plume flow field. Obviously some differences exist between the model and prototype condition. In order to analytically scale from the model to the prototype condition the following approach is used.

2.2.4 Scale Factors

After a gas mixture and chamber condition have been selected, the veracity of the choice must be tested. In order to transfer analytically from the model to the prototype case, a scale factor is defined. Although the methods of Ref. 4 were considered for use, a much simpler analytical correlation between the prototype and model cases is supplied by comparing the momentum flux in the corresponding plume regions. This factor thus corrects for mismatches of any pertinent parameters. The correction factor for momentum is designated as β where

$$\beta = \frac{(\text{momentum flux})_p}{(\text{momentum flux})_m} \quad (35)$$

This concludes the description of the method of analysis. A discussion now follows of the results obtained thus far with the simulant selection computer program

2.3 DISCUSSION OF ANALYTICAL RESULTS

Table 2 compares the operating characteristics for a prototype rocket motor and its corresponding model nozzle. For this case, the simulant gas mixture was a gaseous binary mixture. Since the simulant mixture was binary, condensation was not accounted for. Significantly, with the higher operating pressure of the model case, the exit plane Reynolds number was higher than the prototype case. Thus the boundary layer should be at least no greater a factor in the model case than in the prototype case. The ability to minimize the importance of the boundary layer for both the binary and ternary simulant mixtures greatly facilitates a search for a suitable simulant mixture. The centerline Mach number distribution is compared for the prototype and model case in Fig. 3. The error in the momentum flux at the center of the region of interest is 2%. Thus impingement forces in this region should be very closely scaled.

Again Table 2 compares the operating parameters for another prototype nozzle and its correspondent model nozzle. Now, the simulant gas was a gaseous ternary system. The additional gas CO_2 was assumed to be a condensable gas in the model system. Once again it was possible to minimize the boundary layer effect in the model case.

A rather surprising result occurred when the point of condensation or point of vapor saturation in the model and prototype plume was computed. For both cases, the point of condensation was found to occur far out in the plume. Realistically, this result may be more a reflection of the calculational methods used than of the physical situation. However, since the prototype and model calculations are independent, it appears significant that this result was obtained for both cases. Figure 3 compares the centerline Mach

Table 2

COMPARISON OF MODEL AND PROTOTYPE ENGINE
OPERATIONAL CHARACTERISTICS

Engine	Binary Mixture			Ternary Mixture		
	Gases	Percent	Chamber Pressure (psia)	Gases	Percent	Chamber Pressure (psia)
Model	CF ₄	0.6405	200	CF ₄	0.7151	200
	N ₂	0.3595		N ₂	0.0849	
				CO ₂	0.2000	
Prototype	Fuel C ₂ H ₄	0.5	100	Fuel CH ₃ NHNH ₂	0.5	100
	Oxidant O ₂	0.5		Oxidant N ₂ O ₄	0.5	

number distribution for the model and prototype case. The error in the momentum flux at the center of the region of interest is 3%. Because of time limitations the two sample cases were the only results obtained to date. However, some general comments may be made concerning the simulant selection program.

First, the program is quite fast. The two cases discussed above were executing in approximately 5 to 6 minutes on the IBM 7094. From work performed while the program was being checked out, it appears that if new gases must be selected, then the run time will approximately double. Thus, it does appear that this computer program is a practical and economical tool to use in the design of an experiment to test impingement forces on bodies immersed in a plume.

A result of perhaps a more serious nature occurred for the ternary case. Here with a mixture of CF_4 , N_2 and CO_2 at elevated temperatures, some decomposition and reaction of the gases was predicted by the CEC routines. One of the resultant gases was COF_3 . This gas is quite toxic, being related to phosgene, the nerve gas. Although mixtures of CF_4 and CO_2 were used in Ref. 3, this mixture should not be used in a practical experimental situation until a thorough study of reaction rates is made. Suitable substitutes for CF_4 might be the inert gases such as neon, krypton and xenon. Krypton and xenon are rather expensive, but they are becoming more commonplace. Only neon exists on the products tape to date, however, if necessary, the others could be readily included.

Section 3

CONCLUSIONS AND RECOMMENDATIONS

In general, simulation of rocket exhaust plumes and the subsequent impingement force can be attained by using nonreacting gas mixtures in model nozzles. A computer program which performs the arduous task of selecting a suitable simulant gas mixture has been written and checked out. Although several options are available, the most important consists of selecting a simulant gas based upon its ability to duplicate momentum flux or impingement force on a body immersed in a plume. A set of gases was established which, when mixed, provide good simulation properties. Data for these gases are stored on magnetic tape. Additional gases can be added to the tape when deemed desirable. For the two test cases examined, simulant gases were obtained that duplicated the prototype case very well.

Since in an experimental situation it may be difficult with available equipment to attain the necessary parameters for exact simulation, an experimental program to examine the effects of nonsimilarity is recommended. Such a program was outlined in Ref. 22. In brief, by operating a single nozzle at several chamber conditions, the variation in impingement force with chamber enthalpy may be ascertained. Then, using two scaled nozzles -- one as model and the other as prototype -- the simulant selection program will be used to select a gas mixture for the model. Using this gas mixture in the model, impingement forces on a submerged body will be measured and compared to those for the prototype case. Facilities exist to carry out such a study and such an investigation would add validity to the analytical results developed in the current contract.

Before concluding this report this speculative note will be advanced. In order to duplicate the flow field of a gas the properties of the model gas

must be known. There is at this time some preliminary effort to use numerical techniques on electronic computers to solve the equations of quantum mechanics for various molecules (Ref 23). With techniques of this type available, a tremendous number of possible molecules could be studied and their resultant thermodynamic properties predicted. Thermodynamic properties of these molecules could then be compared with the properties of the molecules of the prototype nozzle, and a simulant gas could be selected on the basis of this comparison. Although such a study was beyond the state-of-the-art for the current effort, these techniques might be considered in future efforts.

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APPENDIX A

EFFECT OF MIXTURE RATIO ON MACH NUMBER

Appendix A

The goal of this analysis is to determine if, for specified chamber conditions, any combination of a set of gases can duplicate the conditions at a point in the prototype plume. If duplication is possible, the mixture ratio which will produce the desired conditions must be computed.

Although this search could be made simply by modifying the mixture ratio and observing the resultant change, the ability to make an intelligent estimate concerning the amount of change required is desirable. The estimate need not be exact, it merely points the iteration process in the correct direction and supplies a rough figure for the amount of change necessary in the gas mixture, given the chamber conditions. Now the simulant gas will be selected by its ability to match Mach number and momentum. Appendix B shows that for large values of Mach number, the rate of change of pressure is small compared to the rate of change of Mach number. Hence, the change in momentum becomes a strong function of Mach number.

To determine the mixture ratio, the equations of motion are employed with the definition of Mach number, all written in differential form. In this manner, when the initial mixture ratio is known, the necessary change in mixture ratio can be computed. Before proceeding with the analysis note that mixture ratio can be related to mean molecular weight of a mixture. Thus, molecular weight of the mixture is used as a variable in the following analysis. In the computer program, this is related back to mixture ratio. With this in mind the variation of flow parameters is formulated for one-dimensional flow.

The following assumptions are made

- a Flow is one-dimensional and steady
- b Changes in stream properties are continuous
- c Gas is semi-perfect, specific heat varies with composition and temperature

Writing the basic equations in differential form,

Equation of State

$$\frac{dP}{P} = \frac{d\rho}{\rho} + \frac{dT}{T} - \frac{d\psi}{\psi} \quad A 1$$

Continuity

$$\frac{d\dot{m}}{\dot{m}} = \frac{d\rho}{\rho} + \frac{du}{u} + \frac{dA}{A} \quad A 2$$

Energy

$$\frac{1}{C_p T} \frac{d\dot{m}}{\dot{m}} + \frac{1}{h_o} \left(\frac{dh}{C_p T} + \frac{\gamma-1}{2} M^2 \frac{du^2}{u^2} \right) = 0 \quad A 3$$

Momentum

$$\frac{dP}{P} + \gamma M^2 \left(\frac{dA}{A} + \frac{du^2}{u^2} + \frac{d\rho}{\rho} \right) = 0 \quad A 4$$

and the definition of Mach number

$$\frac{dM^2}{M^2} = \frac{du^2}{u^2} + \frac{d\psi}{\psi} - \frac{d\gamma}{\gamma} - \frac{dT}{T} \quad A\ 5$$

Now Eq (A 5) is rewritten

$$\frac{d\psi}{\psi} = \frac{dM^2}{M^2} - \frac{du^2}{u^2} + \frac{d\gamma}{\gamma} + \frac{dT}{T} \quad A\ 6$$

And Eqs (A 1) through (A 4) are then used to write du^2/u^2 , $d\gamma/\gamma$, and dT/T in terms of M and ψ

The equation obtained after all the algebraic manipulation is

$$\begin{aligned} \frac{d\psi}{\psi} = & \frac{dM^2}{M^2} - 2 \left\{ -\frac{h}{h_o} \left[\frac{dh}{h} - \frac{\gamma-1}{2} M^2 \left(\frac{dT}{T} - \frac{d\psi}{\psi} \right) - \frac{dA}{A} \right] \right. \\ & \left. + \frac{dh}{h} - \frac{d\psi}{\psi} - \frac{dA}{A} \right\} + \frac{d\gamma}{\gamma} + \frac{dh}{h} \end{aligned} \quad A\ 7$$

Where h has been substituted for $C_p T$ to simplify the equation slightly

Now assume that h and γ are linear functions of ψ or molecular weight. Although this is not true, the assumption can be shown to yield results which are in error a maximum of 5 to 10%. See Figs A-1 and A-2 and refer to Ref 2. Changes in γ and h may then be expressed as

$$dh = m_1 d\psi \quad A-8a$$

$$d\gamma = m_2 d\psi \quad A-8b$$

The expression for the change in molecular weight or mixture ratio required to produce a desired change in Mach number becomes

$$d\psi = \frac{dM^2}{M^2} \left/ \left[\frac{1}{\psi} + \frac{2h}{h_o} \left\{ -\frac{m_1}{h} + \frac{\gamma-1}{2} M^2 \left(\frac{m_1}{h} - \frac{1}{\psi} \right) + \frac{dA}{A} \right\} \right. \right. \\ \left. \left. + \frac{2m_1}{h} - \frac{2}{\psi} - \frac{2dA}{A} - \frac{m_2}{\gamma} - \frac{m_1}{h} \right] \right. \quad A 9$$

Now an expression for dA/A can be obtained easily by assuming an inviscid expansion at the nozzle lip and computing the change in the Prandtl-Meyer expansion angle caused by changing the gas composition. Since the nozzles under consideration in this study have large area ratios (A/A^*), assume that the gas in expansion is frozen thermodynamically. The limiting expansion angle can then be expressed,

$$\nu = \frac{\pi}{2} \left[\sqrt{\frac{\gamma+1}{\gamma-1}} - 1 \right] \quad A 10$$

Or θ , the flow, angle can be written

$$\theta = \nu - \nu_e + \phi \quad A 11$$

then the one-dimensional area of the plume at some radial distance S from the source is,

$$A = S \theta \quad A 12$$

Now with a small change in gas composition or γ the resultant area change is approximated by

$$dA = S d\theta = S \left[d\nu - d\nu_e \right] \quad A 13$$

$$\nu_e = \sqrt{\frac{\gamma+1}{\gamma-1}} \tan^{-1} \sqrt{\frac{\gamma-1}{\gamma+1} (M_e^2 - 1)} - \tan^{-1} \sqrt{M_e^2 - 1} \quad A 14$$

$$d\nu = -\frac{1}{(\gamma-1)^2} \frac{\pi}{2} \sqrt{\frac{\gamma-1}{\gamma+1}} d\gamma \quad A 15$$

$$d\nu_e = -\frac{1}{(\gamma-1)^2} \sqrt{\frac{\gamma-1}{\gamma+1}} \tan^{-1} \sqrt{\frac{\gamma-1}{\gamma+1} (M_e^2 - 1)} +$$

$$2 \sqrt{\frac{\gamma+1}{\gamma-1}} (M_e^2 - 1) \left[1 + \frac{\gamma-1}{\gamma+1} (M_e^2 - 1) \right] \left[\frac{1}{2} \frac{\gamma-1}{\gamma+1} (M_e^2 - 1) \right]^{1/2} d\gamma \quad A 16$$

$$\frac{dA}{A} = \frac{(d\nu - d\nu_e) d\gamma}{\theta} \quad A 17$$

This expression for dA/A can then be substituted into Eq A 9 to complete the analysis. Obviously, the final expression is not strictly correct, however, it does allow an estimate of the change required in gas mixture to obtain the desired parameter.

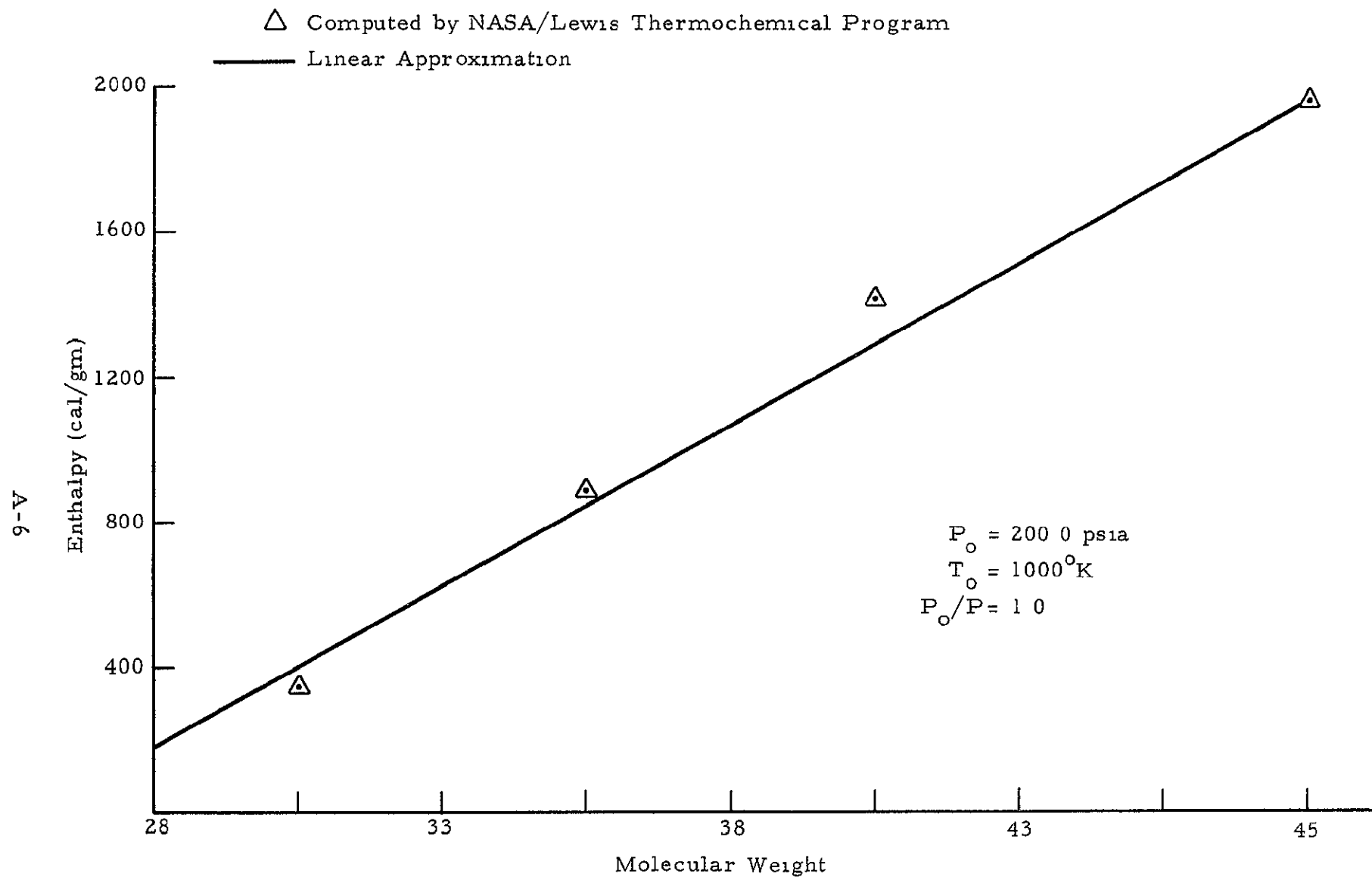


Fig A-1 - Enthalpy Versus Molecular Weight for Various Mixtures of Gaseous Nitrogen and Carbon Dioxide

A-7

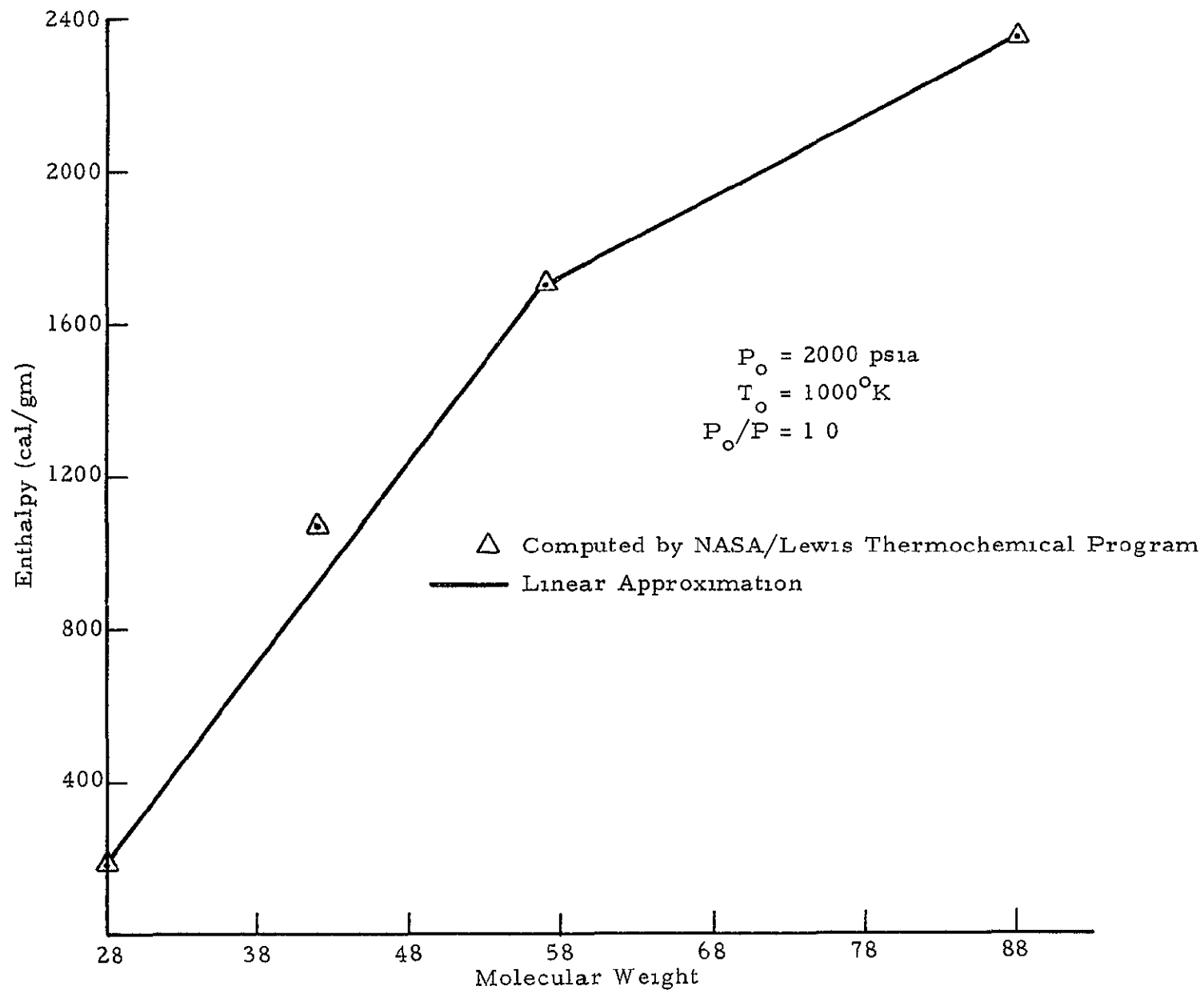


Fig A-2 - Enthalpy Versus Molecular Weight for Various Mixtures of Gaseous Nitrogen and Carbon Tetrafluoride (CF_4)

APPENDIX B

ISENTROPIC EXPANSION IN TERMS OF THE
VARIABLES PRESSURE AND MACH NUMBER

"

Appendix B

Assuming isentropic conditions hold at a point, then we may write

$$P = P_o / \left(1 + \frac{\gamma - 1}{2} M^2 \right)^{\gamma / \gamma - 1} \quad (B-1)$$

Now let M change by an amount ΔM Then

$$\Delta P = \frac{P_o}{\left[1 + \frac{\gamma - 1}{2} (M^2 + 2 M \Delta M + (\Delta M)^2) \right]^{\gamma / \gamma - 1}} - \frac{P_o}{\left(1 + \frac{\gamma - 1}{2} M^2 \right)^{\gamma / \gamma - 1}} \quad (B-2)$$

assuming some typical values for P_o , M and γ in an expanded plume,

$$P_o = 1000$$

$$\gamma = 1.4$$

$$M = 20$$

Then for a 10% change in M,

$$\Delta P = 0.059 \times 10^{-3}$$

Since ΔP is an inverse function of M, it obviously becomes greater for smaller Mach numbers. However, the region of interest in this project is the highly expanded region and in that case changes in pressure are small for changes in Mach number.

APPENDIX C

USER'S MANUAL

DESCRIPTION OF A DIGITAL COMPUTER PROGRAM FOR
SELECTING A GAS MIXTURE TO SIMULATE THE PLUME OF A
ROCKET NOZZLE

Appendix C

C.1 INTRODUCTION

To determine accurately impingement forces on complex bodies immersed in the plume of a rocket nozzle experimental testing on scale models of the prototype situation is needed. To simplify the experimental procedure nonreacting cold gases should be used to simulate the plume. If cold nonreacting gases are introduced in the test situation, duplication of the entire prototype plume is impossible and selecting a simulant gas mixture becomes difficult.

To overcome the numerical magnitude of selecting the simulant, Lockheed Missiles & Space Company, Huntsville Research & Engineering Center, developed under contract to the Aero-Astrodynamics Laboratory of Marshall Space Flight Center, a digital program which rapidly searches among possible simulant gases to determine a gas mixture that best approximates a region in the prototype plume. The program is applicable for problems involving the high altitude expansion of a nozzle exhaust. Input to this program has been kept as simple as possible in order to enhance the usefulness of the program.

This document was prepared to facilitate operation and understanding of the program. Questions involving initial assumptions made in this program can be answered by referring to the main body of this report. Inevitably questions will arise concerning any newly created program. These should be referred to the author.

C 2 DISCUSSION

The program consists of 28 active subroutines or functions which perform the gas thermodynamic calculations, the source flow expansion and the comparison of prototype and model plumes. A general flow chart of the method of solution is given in Figure C-1. In addition, the overlay structure necessary for use on the IBM 7094 computer is illustrated in Fig C-2.

The Input procedure and output interpretation is covered in the Input/Output Section. The input instructions are simple and self-explanatory. The output instructions are in the form of flagged comments which refer to a corresponding section on a typical page of output. An IBM 7094 Instruction card is included at the end of the Input/Output Section.

To aid in the study of this program a commented listing of the program is included in this document as Appendix D.

Table 1 of the basic report tabulates the gases which are currently stored on the master tape as possible simulant gases. This array can be expanded using results from Refs 17 or 18.

Table C-1 (From Table 1)

Gases Currently Available for Analysis as Possible Simulants	
Ar	Argon
CClF ₃	Carbon Chlortrifluoride
CF ₄	Carbon tetrafluoride
CHF ₃	Trifluormethane
CO ₂	Carbon dioxide
H ₂	Hydrogen
N ₂	Nitrogen
N ₂ O	Nitrous oxide

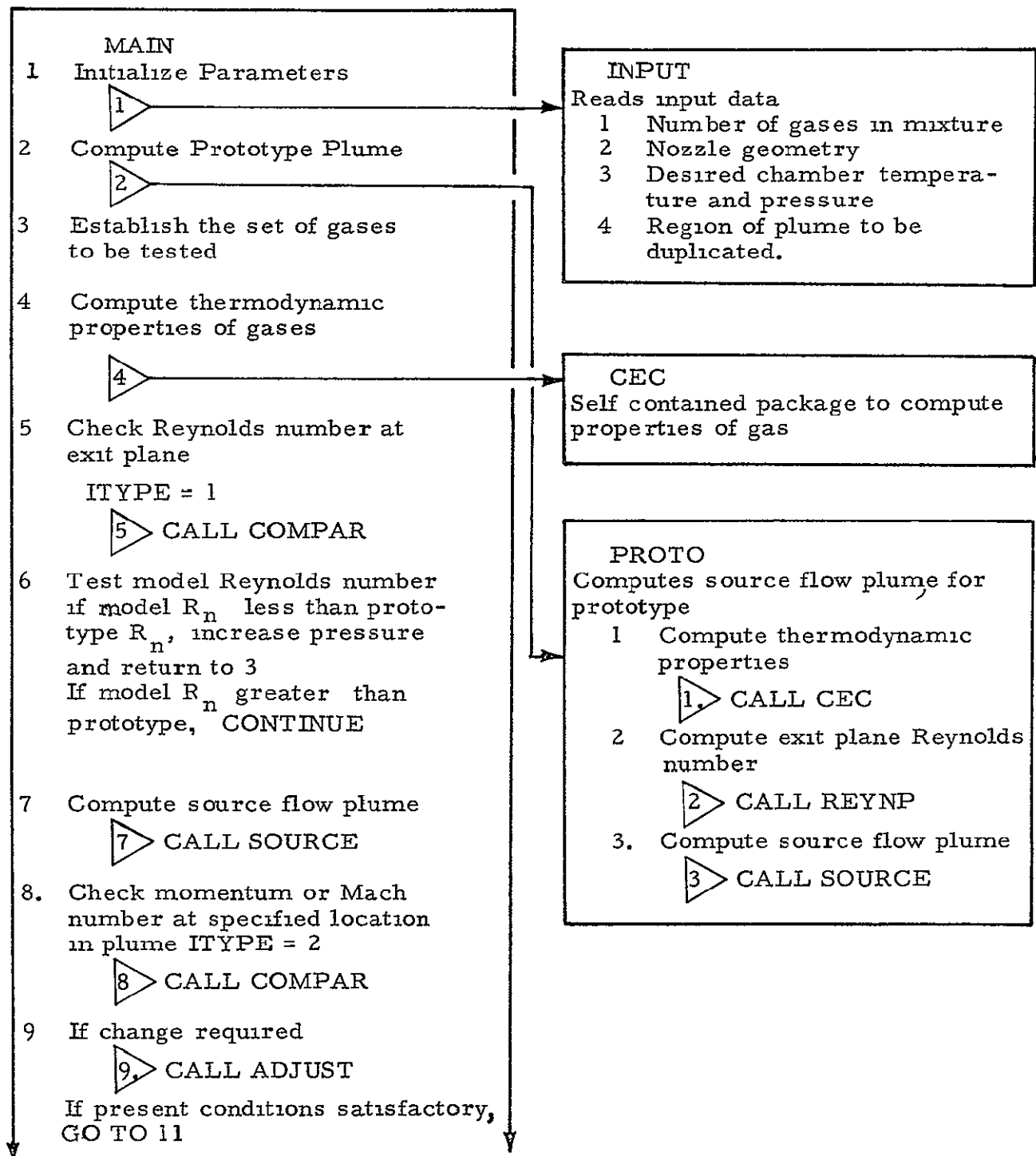


Fig C-1 — General Flow of Program

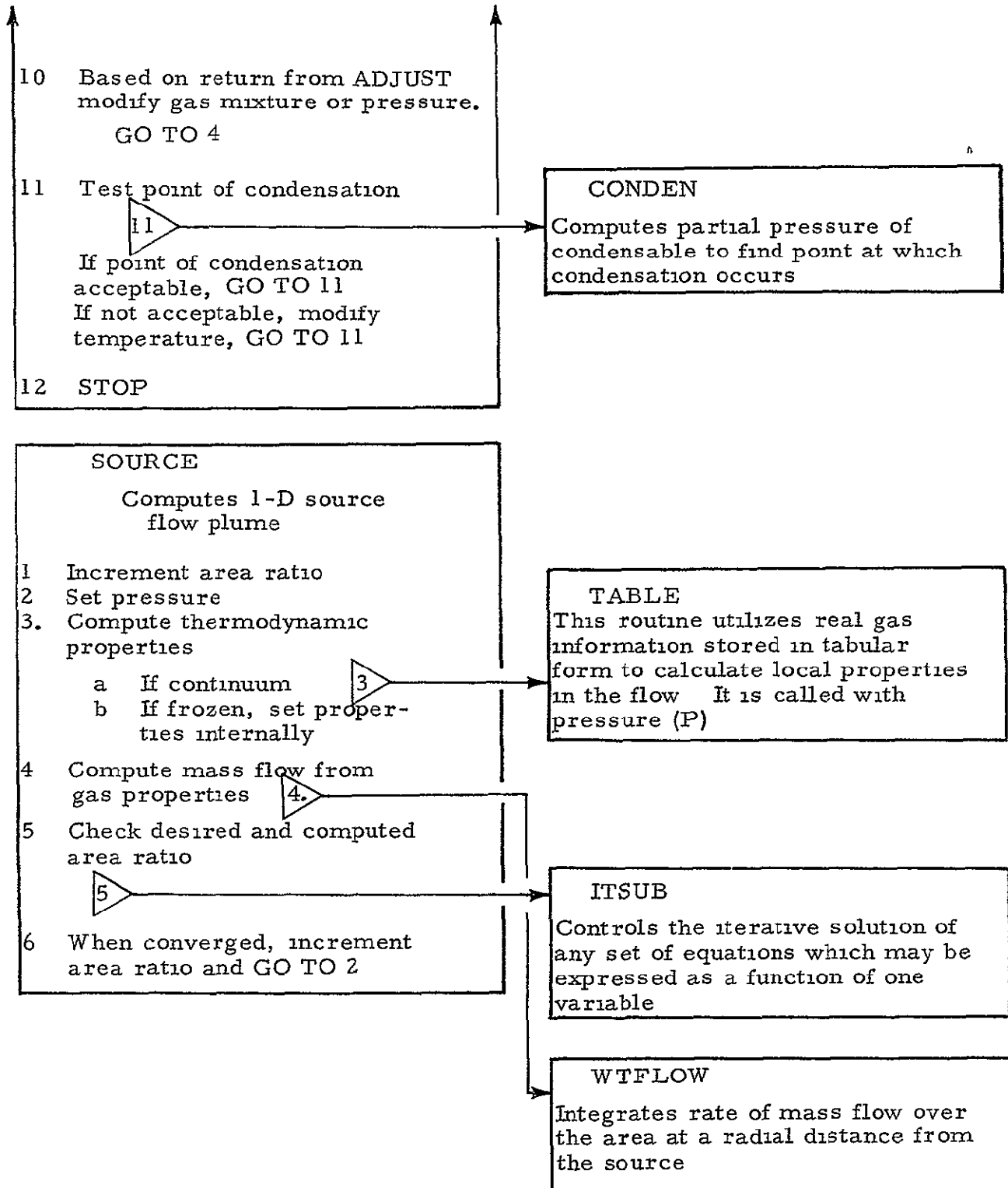


Fig C-1 Contd

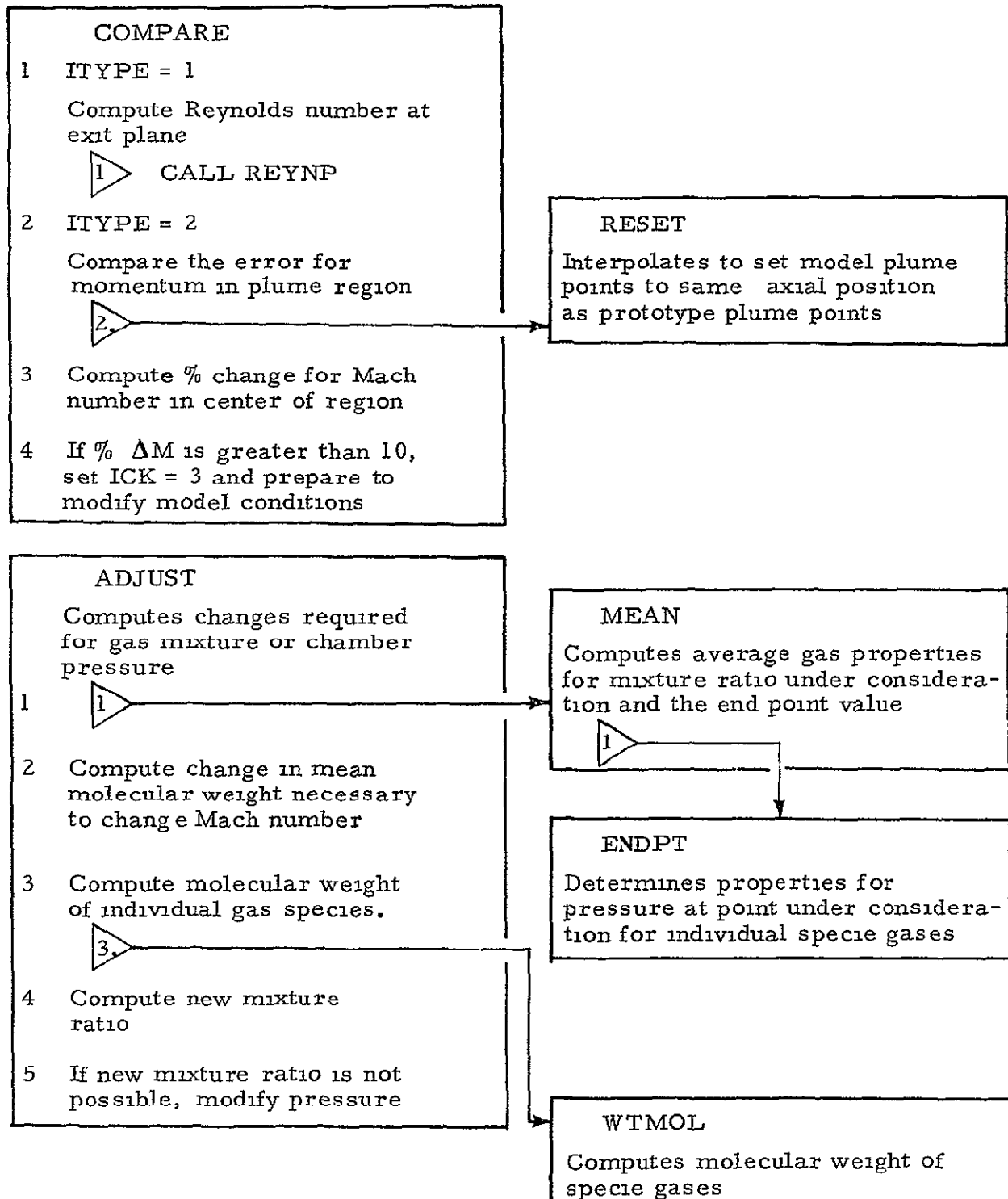


Fig. C-1 Contd

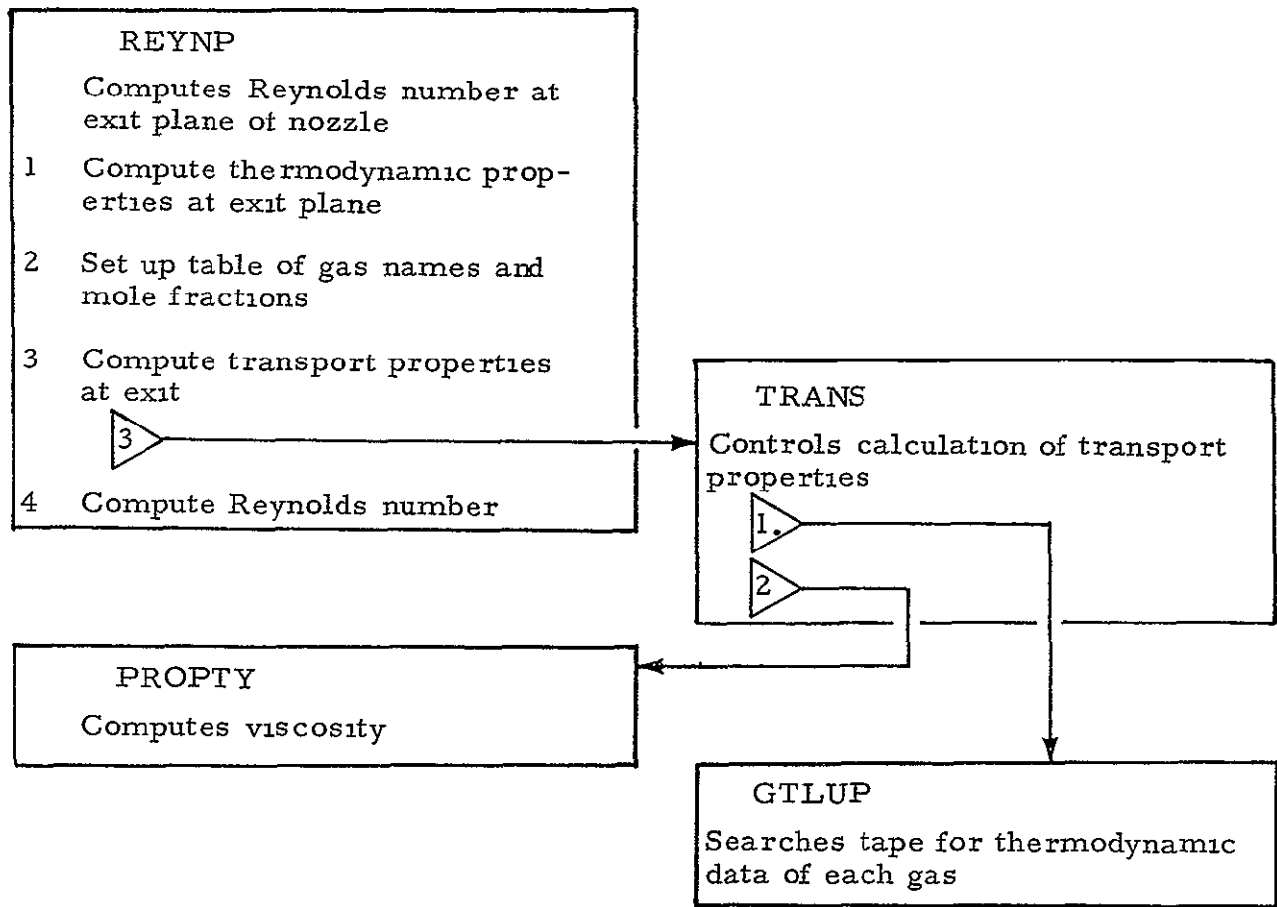


Fig C-1 Contd

C-7

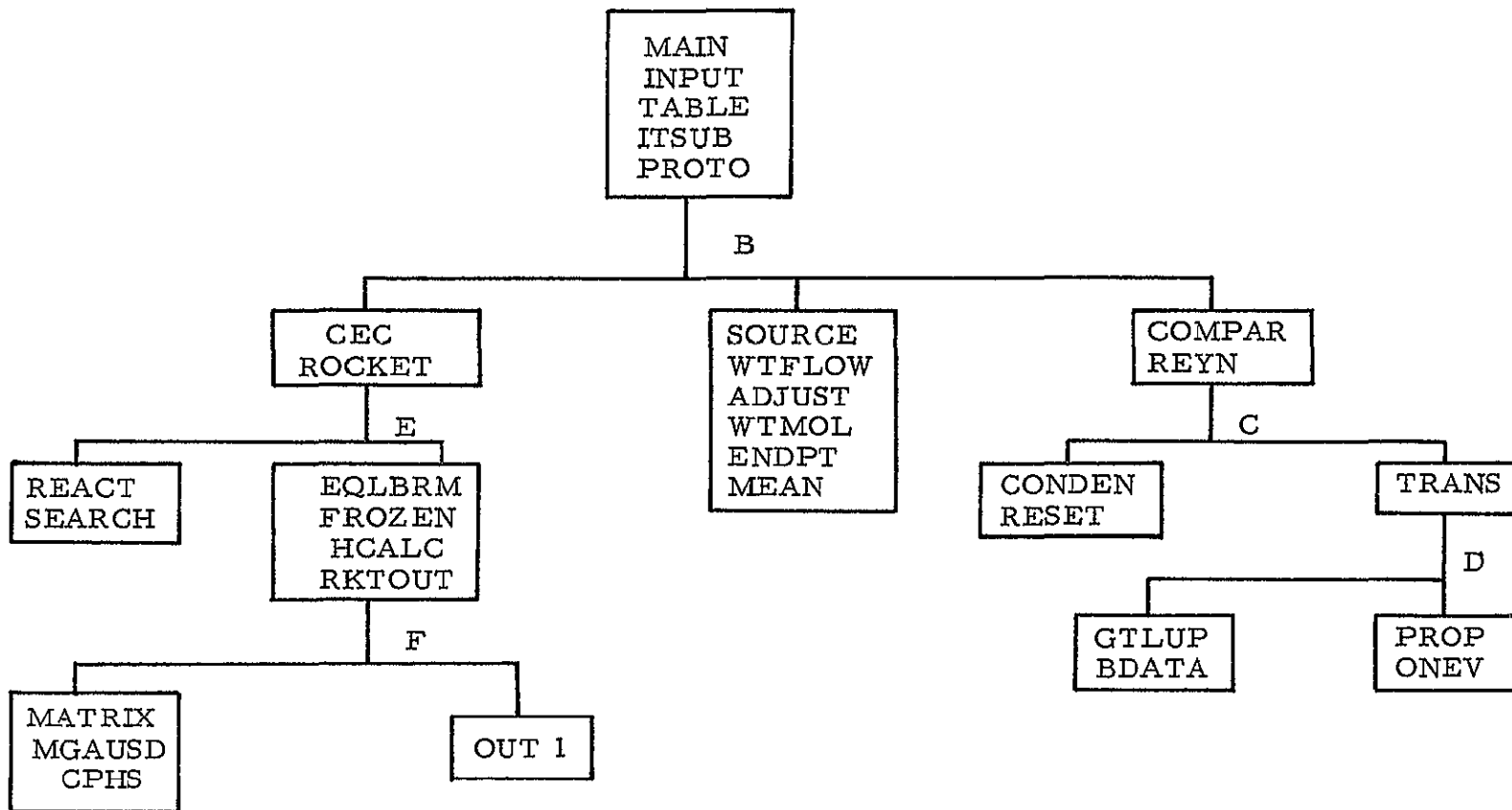


Fig C-2 — Overlay Structure of Simulant Selection Program

C 2 1

INPUT GUIDE

CARD NO 1		Problem Title or Identification
FORMAT	12A6	
Cols 1 - 72	HOL	Comment card or header information
CARD NO 2	Control	Card
FORMAT	8I5	
Cols 1 - 5	NMIX	Number of gases to be used in simulant mixture
Cols 6 - 10	NPTS	Number of points in plume to be matched Must be 3
Col 11 - 15	IP	0 Set initial chamber pressure in program 1 Read in initial chamber pressure
Col 16 - 20	IT	0 Set initial chamber temperature in program 1 Read in initial chamber temperature
Col 21 - 25	IG	0 Gases to be selected by program 1 Specific gas mixture to be read in
Col. 26 - 30	IFLAG	0 Regular output 1 Intermediate output for debugging model information
Col 31 - 35	ITYPE	1 Calculation of simulation ability to be based on momentum flux comparison 2 Calculation of simulation ability to be based on Mach number comparison 3 Calculation of simulation ability to be based on Reynolds number comparison
CARD NO 3		
FORMAT	7E10 6	

Col 1 - 10	ATM	Nossle throat area of model
Col 11 - 20	RADTHM	Throat radius of model (ft)
Col 21 - 30	AEOATM	Ratio of exit plane area to throat area of model
Col 31 - 40	ANGLPM	Angle at nozzle lip of model (deg)
CARD NO 4	(Included if either chamber pressure or temperature is to be specified)	
FORMAT	7E10 6	
Col 1 - 10	PCHAMI	Model chamber pressure to be initially used Blank if not applicable (PSI)
Col 11 - 20	TCHAMI	Model chamber temperature to be initially used Blank if not applicable (deg R)
CARD NO 5	Prototype	Information
FORMAT	7E10 6	
Col 1 - 10	RADP	Throat radius of prototype nozzle
Col 11 - 20	AETP	Ratio of exit plane area to throat area for prototype
Col 21 - 30	ANGP	Angle at exit plane of prototype nozzle (deg)
Col 31 - 40	PREP	Chamber pressure of prototype (PSI)
CARDS No 6	Prototype Fuel and Oxidizer Information	
FORMAT	5(A2, F7 0), 1X, A1, 1X, A1, 1X, 3E10 3	
Col 1 - 45	PNAME	Fuel or oxidizer name (Products must be on CEC products tape)
Col 47	LOF	F In col 48 denotes fuel O In col. 48 denotes oxidizer
Col 49	PHAZ	Phase of propellant L - Liquid G - Gas
Col 51 - 60	WTFRAC	Weight fraction of fuel or oxidizer
Col 61 - 70	HENTH	Heat of formation (in cal) of fuel or oxidizer

Col. 71 - 80	HTEMP	Temperature (°K) associated with heat of formation
CARD NO 7	Region of Simulation	
FORMAT	7E10 6	
Col 1 - 10	XP11	Axial location of point nearest nozzle in region of plume to be simulated (X/D from nozzle)
Col 11 - 20	XP12	Axial location of central point in simulated region (X/D from nozzle)
Col 21 - 30	XP13	Axial location of rear point in simulated region (X/D from nozzle) (XP11, XP12, XP13)
Col 31 - 40	ERRMAX	Multiplication factor which may be input to modify the allowable percentage error used in the program. This allowable error is 10% and thus ERRMAX may be used to tighten or loosen this criteria ($0 < \text{ERRMAX}$)

C 2.2 Description of Program Output

The simulant selection program output is organized into several basic groups which are easily recognizable. The initial output consists of input data. Thermodynamic data from the CEC portion of the program is then printed out. The next area contains data from calculations for the Reynolds number. Finally, a source flow plume is printed out. If this plume does not satisfy the required conditions a message is written out and further calculations are performed with output similar to that above. Detailed explanations are listed below. Numbered flags on the example output correspond to the numbered comments. Only pertinent output pages are shown.

Group I - Identification

(1) Title Identifies particular run.

Group II - Run Control

(2) Run Control Parameters These five parameters control program execution according to options selected. (See input guide for explanation of individual parameters.)

Group III - Model Nozzle Information

- (3) Model Nozzle Geometry These parameters are input and are explained in the input guide
- (4) Chamber Conditions Chamber temperature and pressure are either input or set by program as determined by Group I parameters

Group IV - Prototype Nozzle Information

- (5) Prototype Nozzle Geometry These parameters are input and are explained in the input guide

Group V - Plume Region Information

- (6) Plume Region These parameters define a region of the plume to be duplicated They are explained in the input guide
- (7) ERRMAX Described in input guide

Group VI - Prototype Gas Thermodynamic Information

This data is generated by the CEC portion of the program and contains data for an equilibrium combustion of the reactants and a frozen expansion of the products

- (8) Gas Data This page contains the thermodynamic data for the prototype engine The tables are self-explanatory (Units are on output)
- (9) This table contains gas parameters pertinent to the calculations of a source flow plume. This is the TAB array of the program

Group VIII - Prototype Reynolds Number Calculation

- (10) Prototype Reynolds Number

Group IX - Prototype Plume

- (11) Origin of source flow with respect to exit plane of nozzle - (ft)
- (12) Expansion angle of flow at nozzle lip - (radians)
- (13) Radial distance from source - (ft)
- (14) Mach number - Local Mach number
- (15) Reynolds number - Local Reynolds number
- (16) Gamma - specific heat ratio
- (17) Knudsen Number
- (18) Stagnation temperature - ($^{\circ}\text{R}$)
- (19) Static temperature - ($^{\circ}\text{R}$)
- (20) Stagnation pressure - (psf)
- (21) Static pressure - (psf)
- (22) Condensation point of H_2O in prototype plume - (ft), ternary system only

Group X - Model Gas Mixture

- (23) This data is computed by CEC portion of program. The tables are self-explanatory
- (24) This table contains gas parameters used in the calculation of a source flow plume This is the TAB array
- (25)} Gas data for individual species of gases in the simulant mixture Used
- (26)} in subsequent calculations (appear only when new gases or new chamber stagnation conditions are tried)

Group XI - Model Reynolds Number

This section contains exit plane properties and Reynolds number for model nozzle See Group VIII for explanation

Group XII Model Plume

Source flow plume for model nozzle See Group IX for explanation

C 3 SAMPLE IBM 7094 INSTRUCTION CARD

This sample card is included in the program direction to aid the user in running the program. Naturally this format will vary from machine to machine. The important data to note however, are the tape numbers and logic. These contain the data necessary for the calculation of thermodynamic and transport properties of many gases. See Refs 16 and 17.

- (1) Programmer name
- (2) Operation code - 11-production
- (3) Bin number - assigned by computer services
- (4) Location - Return completed job to this area
- (5) Job number - assigned by computer services
- (6) Simulation gases products tape
- (7) Transport property products tape
- (8) Complete products tape for CEC
(Used in prototype calculations)
- (9) Time assigned by programmer
(Usually 30 minutes of 7094 will suffice)
- (10) Number of lines assigned by programmer
(Usually 15,000 will suffice)

7094 - INSTRUCTIONS									
NAME (1)				OP CODE (2)		STACK #			
BIN # (3)		LOC (4)		JOB # (5)					
IF EXCEEDS MAX (15)				FAST TAPES A B C D					
<input type="checkbox"/> STR <input type="checkbox"/> STE <input type="checkbox"/> DMP <input checked="" type="checkbox"/> RETSY				INPUT TAPES				WORK LOGIC	
(12-13)				LOGIC		REEL NO		DEN	
<input checked="" type="checkbox"/> 1BSYS (11) <input checked="" type="checkbox"/> COMPL / ASSEMBL (6)				A5		28141			
<input type="checkbox"/> SPOOK <input checked="" type="checkbox"/> EXECUTE				A7		4640			
<input type="checkbox"/> OTHER <input type="checkbox"/> PUNCH (BCD BIN)				A8		4451			
<input checked="" type="checkbox"/> 4 FTRN (14) <input type="checkbox"/> MAP									
<input type="checkbox"/> 2 FTRN <input type="checkbox"/> FAP									
<input type="checkbox"/> APT <input type="checkbox"/> SCAT									
<input type="checkbox"/> PERT <input type="checkbox"/> OTHER									
LINES OF OUTPUT (1000S) (10)				MAXIMUM TIME (9)					
<input type="checkbox"/> 0-5 <input type="checkbox"/> 5-15 <input type="checkbox"/> 15-30 <input type="checkbox"/> OVER				HOURS		MINUTES			
PROGRAMMER COMMENTS				NUMBER OF CASES					
OVER									
OPERATOR COMMENTS								<input type="checkbox"/> SEE ON LINE <input type="checkbox"/> SEE TECHNIQUE <input type="checkbox"/> MAX EXCEEDED <input type="checkbox"/> RETURN TO SYS <input type="checkbox"/> LINE MAX	
OPER INIT OVER									
OUTPUT TAPES ONLY									4020
REEL NO	LOGIC	DEN	UNIT	NO OF CPYS	SAVE	TAPE			
	B-1	8							
NO FILES	NO FRAMES	COPIES	DENSITY	COPY FLO	KALVAR				
		P F	5 8	P F					

MSFC - Form 533 (Rev February 1966)

- (11) Job will be executed under IBM 7094
IBSYS system
- (12) Computer is to compile and assemble
the subroutines in binary form suitable for execution
- (13) After compilation and loading of the
binary form of the subroutines the
program is to be executed
- (14) The program coding is in FORTRAN
IV language
- (15) If either maximum time or maximum
pages exceeded, the program control
is to be returned to the IBSYS system
and the job terminated

If the dump is checked and either of the
above occurs, the computer operator
will initiate a dump of the program and
the variables stored in the core

Appendix D

PROGRAM LISTING AND PRINTOUT

```

$JOB          H029-LMSC L5207      ,911000,00,12,140CEP
*            DATE    MAY 70      SEQ= G602
$EXECUTE      IBJOB
$IBJOB        MAP,LOGIC,GO,FIOCS,SOURCE,FLOW
$IBFTC MAIN
C      CONTROLLING PROGRAM
C      SETS INPUT ANDS CALLS CEC
C      TO LESSEN THE NO. OF CHANGES THAT MUST BE MADE, THE THERMODYNAMIC
C      DATA FOR THE TRANSPORT PROPERTIES WILL BE READ FROM TAPE 12, THE
C      OLD NASA/LEWIS DATA TAPE.
C      THE THERMODYNAMIC DATA FOR THE CEC PORTION WILL BE READ FROM TAPE
C      4, THE NEW DATA TAPE GENERATED BY MCDERMIT.
C      TO MAKE THESE COMPATABLE THE CEC IS MODIFIED TO READ THE GAS NAME
C      UNDER A 2A6 FORMAT.
COMMON/PLUNMU/XC(5),PC(5),EMC(5),GMC(5),TC(5),QC(5),EMWC(5)
COMMON/PLUMF1/PRPR(10,4),REYPLM
COMMON/CHANGE/PC11,PC21,PC22,PC31,PC32,PC33,PNW,TNW,DEL,DELMN,
$DELREY
COMMON/PLUMF2/PROP(10,200),IPT
COMMON/GASES/TAB(3,12,13),NMIX
COMMON/GASFO/GASNAM(10,5,4),GNUM(10,5,4),NML(10,4),
1FZG (10,4),FXG(10,4),ENTHG(10,4),RTEMPG(10,4)
COMMON/SUNUP/SUN(3,40,2)
COMMON/CHAMB/PCHAM1,TCHAM1,PMAX,TMAX
COMMON/NUMG/IG1,IG2,IG3,IG4,PCMAX,IG
INTEGER GASNAM
COMMON/GEOM/AT,RADTHT,AEOAT,ANGLP,REYNP
COMMON/LIP/THET,PIO2
COMMON/EXCON/PEX,EMU
COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),BO(15),BOP(15,2)
1,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AC(2),AM(2)
2,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
3,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4,RHOP,RMW(15),TLN
COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
1,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)
2,TOTN(13)
COMMON/COUNT/IKLUG

```

```

COMMON/WRIT/IFLG1
COMMON/TAPE/IPROT
COMMON/MOLFRC/ZFRAC(40),KFR
COMMON/PNT/KPT(4)
DATA LANK/1H /
COMMON/MGEOM/ATM,RADTHM,AEOATM,ANGLPM
COMMON/MOLWT/SA,SB,SC
DIMENSION PSI(10,4)
LOGICAL KAZE
C   IRNK IS COUNTER IF MIXTURE CHANGES FOR REYNOLDS NO. CALC
    IRNK=0
    IKLUG=0
C   READ INPUT INFO AND SET GAS DATA
    CALL INPUT
    PCMAX=.5
    P1=3.14159
    P02=P1/2.0
C
C   CALL PROTO
C   RESET GEOMETRY VALUES TO THOSE OF MODEL
    RADTHT=RADTHM
    AEOAT= AEOATM
    ANGLP= ANGLPM
    AT=ATM
C   USE CEMDAT TO SET UP POSSIBLE SIMULANT GAS NAMES
C   SET UP A STANDARD ARRAY TO CONTAIN POSSIBLE SIMULANT GAS DATA
C   LAST DIGIT DESIGNATES THE CATAGORY TO WHICH THE GAS BELONG
C   1 IS LOW-GAMMA GAS,2 IS HI-GAMMA GAS
C   3 IS CONDENSABLE
C   FIRST DITIT COUNTS NO. OF GASES IN CATAGORY
C   SECOND DIGIT INDICATES ELEMENT IN GAS TYPE
C   NEED TO LOAD IN REF. TEMP. AND ENTHALPY
    RTEMPG(1,2)=298.15
    ENTHG(1,2) =0.0
    RTEMPG(2,2)=298.15
    ENTHG(2,2) =0.0
    RTEMPG(3,2)=298.15
    ENTHG(3,2) =0.0

```

```

RTEMPG(4,2)=298.15
ENTHG(4,2) =19490.0
RTEMPG(1,1)=298.15
ENTHG(1,1) --217200.0
PTEMPG(2,1)= 298.15
ENTHG(2,1) =-162600.0
RTEMPG(1,3)=298.15
ENTHG(1,3) =-94051.8
RTEMPG(2,3)=298.15
ENTHG(2,3) =-171900.0
PSI(1,1)=88.
PSI(2,1)=71.
PSI(1,2)=28.
PSI(2,2)=39.9
PSI(3,2)=2.
PSI(4,2)=44.
PSI(1,3)=44.
PSI(2,3)=106.4
C   INITIALIZE GUESS OF MIXTURE RATIO
PC11=1.0
PC21=0.5
PC22=0.5
PC31=0.4
PC32=0.4
PC33=0.2
DP3=.05
PHOLD=PCHAMI
THOLD=TCHAMI
C   THIS SECTION INTIALIZES THE  GAS SELECTION PROCEDURE
C   L IS COUNTER ON CONDENSABLE
L=1
C   KAZE IS SET FALSE IF MIXTURE IS CHANGED
KAZE =.TRUE.
KASE=0
IRNT=0
  IF(IG.EQ.1)GO TO 400
K=1
C   EVENTUALLY A SYSTEM WILL BE SET UP TO SELECT SINGLE GAS

```

```

C      THAT APPROXIMATES A PT IN THE FIELD
      IF(NMIX.EQ.3)GO TO 200
      IF(NMIX.GT.1)GO TO 100
15  I=0
20  I=I+1
31  CONTINUE
      DO 11 J=1,5
        NAME(1,J)=GASNAM(I,J,K)
11  ANUM(1,J)=GNUM(I,J,K)
      ENTH(1)=ENTHG(I,K)
      RTEMP(1)=RTEMPG(I,K)
      FAZ(1)=FZG(I,K)
      FOX(1)=FXG(I,K)
      PECWT(1)=PC11
      P=PHOLD
      T=THOLD
      NAME(2,1)=LANK
C
C      GO TO 400 ,CALL CEC FOR 1 GAS
      GO TO 400
100 CONTINUE
      IT1=0
21  IT1=IT1+1
33  CONTINUE
      DO 12 J=1,5
        NAME(1,J)=GASNAM(IT1,J,1)
12  ANUM(1,J)=GNUM(IT1,J,1)
      ENTH(1)=ENTHG(IT1,1)
      RTEMP(1)=RTEMPG(IT1,1)
      FAZ(1)=FZG(IT1,1)
      FOX(1)=FXG(IT1,1)
      SA = PSI(IT1,1)
      PECWT(1)=PC21
C
      IF(1RNK.EQ.1)GO TO 34
      IT2=0
22  IT2=IT2+1
34  CONTINUE

```



```

      DO 13 J=1,5
      SB = PSI(IT2,2)
      NAME(2,J)=GASNAM(IT2,J,2)
13  ANUM(2,J)=GNUM(IT2,J,2)
      ENTH(2)=ENTHG(IT2,2)
      RTEMP(2)=RTEMPG(IT2,2)
      FAZ(2)=FZG(IT2,2)
      FOX(2)=FXG(IT2,2)
      PECWT(2)=PC22
      P=PHOLD
      T=THOLD
C
      NAME(3,1)=LANK
C      GO TO 400,CALL CEC FOR 2 GASES
      GO TO 400
200 CONTINUE
C      INITIALIZE FOR TERNARY, USE CO2 FOR CONDENSABLE
      IT1=0
23  IT1=IT1+1
35  CONTINUE
      DO 14 J=1,5
      NAME(1,J)=GASNAM(IT1,J,1)
14  ANUM(1,J)=GNUM(IT1,J,1)
      ENTH(1)=ENTHG(IT1,1)
      RTEMP(1)=RTEMPG(IT1,1)
      FAZ(1)=FZG(IT1,1)
      FOX(1)=FXG(IT1,1)
      SA = PSI(IT1,1)
      PECWT(1)=PC31
C
      IF(IRNK.EQ.1)GO TO 36
      IT2=0
24  IT2=IT2+1
36  CONTINUE
      DO 85 J=1,5
      NAME(2,J)=GASNAM(IT2,J,2)
85  ANUM(2,J)=GNUM(IT2,J,2)
      ENTH(2)=ENTHG(IT2,2)

```

```

      RTEMP(2)=RTEMPG(IT2,2)
      FAZ(2)=FZG(IT2,2)
      FOX(2)=FXG(IT2,2)
      SB = PSI(IT2,2)
      PECWT(2)=PC32
C     SET CONDENSABLE CO2
      DO 16 J=1,5
      NAME(3,J)=GASNAM(L,J,3)
16  ANUM(3,J)=GNUM(L,J,3)
      ENTH(3)=ENTHG(L,3)
      RTEMP(3)=RTEMPG(L,3)
      FAZ(3)=FZG(L,3)
      FOX(3)=FXG(L,3)
      SC = PSI(L,3)
      PECWT(3)=PC33
      P=PHOLD
      T=THOLD
      NAME(4,1)=LANK
400  CONTINUE
      KASE=KASE+1
      WRITE(6,41)
41  FORMAT(30X,31H GAS MIXTURE UNDER CONSIDERATION//35X,4HNAME,15X,
113HMIXTURE RATIO)
      DO 42 MC=1,NMIX
      WRITE(6,44)(NAME(MC,IC),ANUM(MC,IC),IC=1,5),PECWT(MC)
44  FORMAT(15X,5(A2,1X,F7.4,2X),5X,F7.4)
42  CONTINUE
      CALL CEC(1,KASE)
      WRITE(6,310)
310  FORMAT(1H1)
      WRITE(6,51)
51  FORMAT(40X,45HTABLE OF THERMODYNAMIC PROPERTIES FOR MIXTURE)
      WRITE(6,52)
52  FORMAT(15X,8HH FT2/S2,5X,4HA/A*,7X,5HGAMMA,6X,5HM NO.,10X,5HP PSF,
16X,7HT DEG R,5X,6HMOL WT)
      NP1=KPT(1)
      WRITE(6,53)(( TAB(1,I,J),I=1,7),J=1,NPT)
53  FORMAT(13X,E10.3,2X,E10.3,2X,E10.3,2X,E10.3,2X,E10.3,2X,E10.3,2X,

```

```

      $E10.3)
C      TEST IF MIXTURE GASES HAVE CHANGED
      IF(.NOT.FAZE)GO TO 801
C      NOW DETERMINE ENDPTS. OF MIXTURE
      IF(NMIX.EQ.1)GO TO 500
      IF(NMIX.EQ.2)GO TO 550
      IF(NMIX.EQ.3)GO TO 600
500  IF(I.GE.IG1)GO TO 510
      GO TO 20
510  IF(K.EQ.4)GO TO 1000
      K=K+1
      GO TO 15
550  CONTINUE
      PECWT(1)=1.0
      NAME(2,1)=LANK
      P=PHOLD
      T=THOLD
      CALL CEC(2,KASE)
      DO 551 J=1,5
      NAME(1,J)=GASNAM(IT2,J,2)
551  ANUM(1,J)=GNUM(IT2,J,2)
      RTEMP(1)=RTEMPG(IT2,2)
      ENTH(1)= ENTHG(IT2,2)
      FAZ(1) = FZG(IT2,2)
      FOX(1) = FXG(IT2,2)
      P=PHOLD
      T=THOLD
      CALL CEC(3,KASE)
C      AFTER CEC COMPUTES ENDPTS.,THE GAS NAMES MUST BE RESET
580  DO 552 J=1,5
      NAME(1,J)=GASNAM(IT1,J,1)
552  ANUM(1,J)=GNUM(IT1,J,1)
      ENTH(1) = ENTHG(IT1,1)
      RTEMP(1) =RTEMPG(IT1,1)
      FAZ(1)   =FZG(IT1,1)
      FOX(1)   =FXG(IT1,1)
      DO 553 J=1,5
      NAME(2,J)=GASNAM(IT2,J,2)

```

```

553 ANUM(2,J)=GNUM(IT2,J,2)
    ENTH(2) =ENTHG(IT2,2)
    RTEMP(2) =RTEMPG(IT2,2)
    FAZ(2)   =FZG(IT2,2)
    FOX(2)   =FXG(IT2,2)
    PECWT(1)=PC21
    PECWT(2)=PC22
    NAME(3,1)=LANK
C    GAS PROPERTIES LOADED INTO TAB ARRAY,1-MIXTURE,2-ENDPT,3-ENDPT
    GO TO 800
600 CONTINUE
C    NOW TO SET ENDPTS FOR TERNARY MIXTURE
    DO 554 J=1,5
    NAME(2,J)=GASNAM(L,J,3)
554 ANUM(2,J)=GNUM(L,J,3)
    ENTH(2) =ENTHG(L,3)
    RTEMP(2) =RTEMPG(L,3)
    FAZ(2)   =FZG(L,3)
    FOX(2)   =FXG(L,3)
    NAME(3,1)=LANK
    PECWT(1) =PC31+PC32
    PECWT(2) =PC33
    P=PHOLD
    T=THOLD
    CALL CEC(2,KASE)
    DO 555 J=1,5
    NAME(1,J)=GASNAM(IT2,J,2)
555 ANUM(1,J)=GNUM(IT2,J,2)
    ENTH(1) =ENTHG(IT2,2)
    RTEMP(1) =RTEMPG(IT2,2)
    FAZ(1)   =FZG(IT2,2)
    FOX(1)   =FXG(IT2,2)
    P=PHOLD
    T=THOLD
    CALL CEC(3,KASE)
C    AFTER TERNARY ENDPTS COMPUTED, RESET GASES
    PECWT(1)=PC31
    PECWT(2)=PC32

```

```

      DO 557 J=1,5
      NAME(1,J)=GASNAM(IT1,J,1)
557  ANUM(1,J)=GNUM(IT1,J,1)
      ENTH(1) =ENTHG(IT1,1)
      RTEMP(1) =RTEMPG(IT1,1)
      FAZ(1)   =FZG(IT1,1)
      FOX(1)   =FXG(IT1,1)
      DO 558 J=1,5
      NAME(2,J)=GASNAM(IT2,J,2)
558  ANUM(2,J)=GNUM(IT2,J,2)
      ENTH(2) =ENTHG(IT2,2)
      RTEMP(2) =RTEMPG(IT2,2)
      FAZ(2)   =FZG(IT2,2)
      FOX(2)   =FXG(IT2,2)
      DO 559 J=1,5
      NAME(3,J)=GASNAM(L,J,3)
559  ANUM(3,J)=GNUM(L,J,3)
      ENTH(3) =ENTHG(L,3)
      RTEMP(3) =RTEMPG(L,3)
      FAZ(3)   =FZG(L,3)
      FOX(3)   =FXG(L,3)
      NAME(4,1)=LANK
C
800  CONTINUE
      WRITE(6,310)
      WRITE(6,61)
61  FORMAT(40X,49HTABLE OF THERMODYNAMIC PROPERTIES FOR COMPONENT 1)
      WRITE(6,52)
      NPT=KPT(2)
      WRITE(6,53)(( TAB(2,I,J),I=1,7),J=1,NPT)
      WRITE(6,310)
      WRITE(6,71)
71  FORMAT(40X,49HTABLE OF THERMODYNAMIC PROPERTIES FOR COMPONENT 2)
      WRITE(6,52)
      NPT=KPT(3)
      WRITE(6,53)(( TAB(3,I,J),I=1,7),J=1,NPT)
801  CONTINUE
C

```

```

C      COMPARE RN AT EXIT PLANE
      CALL COMPAR (1,IOK,IRCON,KASE)
      IRNK=0
      IF (IRNT.GE.1) GO TO 802
      IF (IRCON.EQ.1) GOTO 1100
      IF (IOK.GT.1) GO TO 900
C      COMPUTE SOURCE FLOW PLUME
802    CONTINUE
      IDZ=0
      CALL SOURCE (IDZ,ISCON)
      IF (ISCON.EQ.1) GO TO 1100
C      COMPARE PLUME REGION
      CALL COMPAR (2,IOK,IDUM,KASE)
      IF (IG.EQ.1) GO TO 1100
      IF (IOK.EQ.0) GO TO 1000
      CALL ADJUST (      NOK,KAZE)
      IF (NMIX.EQ.1.AND.NOK.EQ.0) GO TO 855
      IF (NMIX.EQ.1.AND.NOK.GT.0) GO TO 850
      IF (NMIX.EQ.2.AND.NOK.EQ.0) GO TO 865
      IF (NMIX.EQ.2.AND.NOK.GT.0) GO TO 860
      IF (NMIX.EQ.3.AND.NOK.EQ.0) GO TO 875
      IF (NMIX.EQ.3.AND.NOK.GT.0) GO TO 870
C      MODIFY GASES ACCORDING TO INPUT FROM ADJUST
850    THOLD=TNW
      PHOLD=PNW
      IRNK=0
      IF (I.LT.IG1) GO TO 20
      IF (I.GE.IG1) I=0
      K=2
      IF (I.GT.IG2) GO TO 1020
      GO TO 20
855    T=TNW
      P=PNW
      THOLD=TNW
      PHOLD=PNW
      GO TO 400
860    THOLD=TNW
      PHOLD=PNW

```

```

      IRNK=0
      PC21=.5
      PC22=.5
      IF(IT2.LT.IG2)GO TO 22
      IF(IT1.LT.IG1)GO TO 21
      GO TO 980
865  T=TNW
      P=PNW
      PHOLD=PNW
      THOLD=TNW
      PECWT(1)=PC21
      PECWT(2)=PC22
      GO TO 400
870  THOLD=TNW
      PHOLD=PNW
      IRNK=0
      PC31 =.4
      PC32=.4
      PC33=.2
      IF(IT2.LT.IG2)GO TO 24
      IF(IT1.LT.IG1)GO TO 23
      GO TO 985
875  T=TNW
      P=PNW
      THOLD=TNW
      PHOLD=PNW
      PECWT(1)=PC31
      PECWT(2)=PC32
      PECWT(3)=PC33
      GO TO 400
980  WRITE(6,981)
981  FORMAT(5X,33HNO DESIRABLE BINARY MIXTURE FOUND)
      WRITE(6,706)
706  FORMAT(20X,43HOTO ACHIEVE CONVERGENCE,INCREASE ERROR BAND)
      GO TO 1100
985  WRITE(6,986)
986  FORMAT(5X,72HNO DESIRABLE TERNARY MIXTURE FOUND FOR PRESENT CONDEN
      ISABLE RATIO, MODIFY)

```

```

        WRITE(6,706)
        PC33=PC33+DP3
        PH=(1.0-PC33)/2.0
        PC31=PH
        PC21=PH
        IF(PC33.LE.PCMAX)GO TO 200
        WRITE(6,701)
701  FORMAT(5X,73HNO DESIRABLE TERNARY MIXTURE FOUND  FOR PRESENT CONDE
      2NSABLE, USE NEXT GAS)
        PC33=.2
        PC31=.4
        PC32=.4
        L=L+1
        IF(L.LE.IG3)GO TO 200
        WRITE(6,705)
705  FORMAT(41HNO MIXTURES FOUND FOR PRESENT CONDITIONS)
      GO TO 1100
900  CONTINUE
C    THIS SECTION  INCREASES CHAMBER TEMPERATURE TO COMPENSATE FOR
C    LOW REYNOLDS NO.
      T =TCHAM1 + 300.
      WRITE(6,967)
967  FORMAT(20X, 56HINCREASING CHAMBER TEMPERATURE TO RAISE  REYNOLDS N
      $UMBER)
      P= PCHAM1
      IRNT = IRNT+1
      PHOLD=P
      THOLD=T
      IRNK=1
      IF(NMIX.EQ.1)GO TO 31
      IF(NMIX.EQ.2)GO TO 33
      IF(NMIX.EQ.3)GO TO 35
1000 CONTINUE
      IF(NMIX.EQ.2) GO TO 1100
      WRITE(6,1001)
1001 FORMAT(73HOLAST COMPUTED MIXTURE ACCEPTABLE POINT OF CONDENSATION
      *NOW BEING CHECKED)
      ICON=L

```



```

      CALL CONDEN(ICON,ISW,IACP,TONEW)
      IF(ISW.EQ.0)GO TO 1010
      IF(IACP.EQ.0)GO TO 1050
C     TEMPERATURE CALCULATED IS UNACCEPTABLE, MODIFY GASES
      NOK=1
      PNW=PCHAMI
      TNW=TCHAMI
      GO TO 870
1050 NOK=0
      PNW=P
      TNW=TONEW
      GO TO 875
1020 WRITE(6,1021)
1021 FORMAT(31H0NO ACCEPTABLE SINGLE GAS FOUND)
1010 CONTINUE
1100 CONTINUE
      STOP
      END

```

```

$IBFTC INPUT  DECK
  SUBROUTINE INPUT
    COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),BO(15),BOP(15,2)
    1, TM, TLOW, TMID, THIGH, PP, CPSUM, OF, EQRAT, FPCT, R, RR, HSUBO, AC(2), AM(2)
    2, HPP(2), RHO(2), VMIN(2), VPLS(2), WP(2), DATA(22), NAME(15,5)
    3, ANUM(15,5), PECWT(15), ENTH(15), FAZ(15), RTEMP(15), FOX(15), DENS(15)
    4, RHOP, RMW(15), TLN
    COMMON/GASFO/GASNAM(10,5,4), GNUM(10,5,4), NML(10,4),
    1FZG (10,4), FXG(10,4), ENTHG(10,4), RTEMPG(10,4)
    COMMON/WRIT/IFLG1
    COMMON/GEOM/AT,RADTHT,AEOAT,ANGLP,REYNP
    COMMON/GASES/TAB(3,12,13),NMIX
    COMMON/CHAMB/PCHAMI,TCHAMI,PMAX,TMAX
    COMMON/NUMG/IG1,IG2,IG3,IG4,PCMAX,IG
    COMMON/PROTG/PNAME(4,5),AOF(4),WTFRAC(2),PNUM(4,5),HENTH(4),
    1HTEMP(4),PHAZ(4)
    COMMON/REGION/XPI1,XPI2,XPI3,ERRMAX,ITYPE
    COMMON/PROTN/RADP,AETP,ANGP,PREP
    COMMON/MGEOM/ATM,RADTHM,AEOATM,ANGLPM
    DIMENSION HEADER(12)
  C    READ NO. OF GASES DESIRED IN MIXTURE AND NO. OF AXIAL PTS IN PLUME
    IG=0
    READ(5,1)(HEADER(I),I=1,12)
    1  FORMAT(12A6)
  C    HEADER IDENTIFIES PARTICULAR RUN
    WRITE(6,100)
    100 FORMAT(1H1)
    WRITE(6,2)HEADER
    2  FORMAT(30X,12A6)
    READ(5,5)NMIX,NPTS,IP,IT,IG,IFLG1,ITYPE
    5  FORMAT(8I5)
    WRITE(6,7)NMIX,NPTS,IP,IT,IG,IFLG1,ITYPE
    7  FORMAT(15X,5HNMX=,15,5X,5HNPTS=,15,5X, 3HIP=,15,5X,3HIT=,15,5X,
    13HIG=,15,5X,6HIFLG1=,15,5X,6HITYPE=15)
    TMAX=2000.
    PMAX=1500.
    IF(IP.EQ.0.AND.IT.EQ.0)GO TO 20
    IF(IP.EQ.1.AND.IT.EQ.0)GO TO 10

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      IF(IP.EQ.0.AND.IT.FQ.1)GO TO 15
C     READ BOTH INTIAL CHAMBER T AND P
      READ(5,6)PCHAMI,TCHAMI
      6 FORMAT(7E10.6)
      GO TO 30
      10 READ(5,6)PCHAMI
      GO TO 29
      15 READ(5,6)PDUM,TCHAMI
      20 PCHAMI=200.
      29 CONTINUE
      IF(IT.EQ.1)GO TO 30
      TCHAMI=1800.
      30 CONTINUE
C     READ GEOMETRY OF THROAT
      READ(5,6)ATM,RADTHM,AFOATM,ANGLPM
      WRITE(6,31)
      31 FORMAT(1H0///,40X,23HNOZZLE GEOMETRY FOLLOWS)
      WRITE(6,37)
      37 FORMAT(1H0,29X,11HTHROAT AREA,5X,13HTHROAT RADIUS,5X,10HAREA RATIO,
      $,5X,9HLIP ANGLE)
      WRITE(6,33)ATM,RADTHM,AEOATM,ANGLPM
      33 FORMAT(30X,6(E10.3,5X))
      TCHAMI=TCHAMI/1.8
      WRITE(6,91)TCHAMI,PCHAMI
      91 FORMAT(1H0//,30X,21HINITIAL CHAMBER TEMP=E10.3,5X,9HPRESSURE=E10.3
      1)
      READ(5,6)RADP,AETP,ANGP,PREP
      WRITE(6,110)
      110 FORMAT(1H0//,40X,21HPROTOTYPE INFORMATION)
      WRITE(6,120)RADP,AETP,ANGP,PREP
      120 FORMAT(30X,5HRADP=E10.3,5HAETP=E10.3,5HANGP=E10.3,5HPREP=E10.3)
      DO 140 I=1,2
      READ(5,130)(PNAME(I,J),PNUM(I,J),J=1,5),AOF(I),PHAZ(I),WTFRAC(I),
      $HENTH(I),HTEMP(I)
      140 CONTINUE
      130 FORMAT(5(A2,F7.0),1X,A1,1X,A1,1X,3E10.3)
C     ARE INITIAL GASES INPUT OR SELECTED BY PROGRAM
      IF(IG.EQ.0)GO TO 60

```

```

      L=0
      L=L+1
      DO 50 N=1,NMIX
        READ(5,40)(NAME(N,I),ANUM(N,I),I=1,5),PECWT(N),NML(N,L),ENTH(N),
1FAZ(N),RTEMP(N),FOX(N),DENS(N)
40  FORMAT(5(A2,F7.5),F7.5,A1,F9.5,A1,F8.5,A1,F8.5)
50  CONTINUE
      WRITE(6,84)
84  FORMAT(40X,24HINPUT GAS FOR SINGLE RUN)
      DO 83 J=1,NMIX
        WRITE(6,81)(NAME(J,I),ANUM(N,I),I=1,5),PECWT(J),NML(J,L),ENTH(J),
1FAZ(J),RTEMP(J),FOX(N),DENS(N)
81  FORMAT(1X,5(A2,1X,F7.4,2X),F8.4,2X,A1,F11.2,2X,F8.3,2X,
1A1,3X,F8.5)
83  CONTINUE
60  CONTINUE
      READ(5,6)XPI1,XPI2,XPI3,ERRMAX
C      XPI1 AN XPI3 ARE AXIAL PTS. DEFINING REGION OF INTEREST
      WRITE(6,150)
150  FORMAT(1H0//,45X,32HREGION OF PLUME TO BE DUPLICATED)
      WRITE(6,160)XPI1,XPI2,XPI3
160  FORMAT(35X,4HXP1=E10.3,2X,4HXP2=E10.3,2X,4HXP3=E10.3)
      WRITE(6,170)ERRMAX
170  FORMAT(1H0///,30X,30HERROR MULTIPLICATION FACTOR = E10.3)
      RETURN
      END

```

```

$IBFTC TABL1 DECK
      SUBROUTINE TABLE (P,I1)
      COMMON/GASES/TAB(3,12,13),NMIX
      COMMON/PNT/KPT(4)
      COMMON/GASCON/GAMA,R,T0,P0,EM,RHO,T,WM ,Q
      COMMON/EI TH/H
C      IL IS THE NO. OF PRESSURE CUTS
      IL=KPT(11)
      EQUIVALENCE(NPT ,IL)
      UGC=1545.
      I=11
      RGC=UGC/TAB(I,7,IL)*32.174
      PP=P
      IF(PP.LT.TAB(I,5,IL))PP=TAB(I,5,IL)
      IF(PP.GT.TAB(I,5,1))PP=TAB(I,5,1)
      IF(P.LT.TAB(I,5,IL).OR.P.GT.TAB(I,5,1))GO TO 50
      IT=0
5      IT=IT+1
      IF(PP.LE.TAB(I,5,IT))GO TO 5
      IT=IT-1
      HP=(PP-TAB(I,5,IT))/(TAB(I,5,IT+1)-TAB(I,5,IT))
      GAMA= TAB(1,3,IT) +HP*(TAB(1,3,IT+1)-TAB(1,3,IT))
      XSIP=ALOG(TAB(I,5,IT)/TAB(I,5,IT+1))/ALOG(TAB(I,6,IT)/TAB(I,6,IT+
1))
      ONOX=1./XSIP
      T=(PP/TAB(I,5,IT))*ONOX*TAB(I,6,IT)
C      COMPUTE CP
      XSIH=(TAB(1,1,IT+1)-TAB(1,1,IT))/(TAB(1,6,IT+1)-TAB(1,6,IT))
      H=TAB(1,1,IT)+XSIH*(T-TAB(1,6,IT))
      H0=TAB(1,1,1)
      Q=SQRT(2.*ABS(H0-H))*(H0-H)/ABS(H0-H)
      QSQ=Q**2
      R=RGC
      A=SQRT(GAMA*R*T)
      EM=Q/A
      T0= T+ (GAMA-1.)*QSQ/(2.*GAMA*RGC)
      P0= PP*(T0/T)**(GAMA/(GAMA-1.))
      WM= TAB(I,7,IT)

```

```

      RHO= PP/(RGC*T) *32.174
      GO TO 100
50  CONTINUE
C    COMPUTATION IF P OUTSIDE TABLE
      IF(P.GT.TAB(I,5,1))GO TO 70
      IF(P.LT.TAB(I,5,1L))GO TO 80
70  T1=TAB(I,6,1)
      GAMA=TAB(I,3,1)
      H1=TAB(I,1,1)
      GO TO 90
80  T1=TAB(I,6,1L)
      GAMA=TAB(I,3,1L)
      H1=TAB(I,1,1L)
90  CONTINUE
      T=T1*(P/PP)**((GAMA-1.)/GAMA)
      A=SQRT(GAMA*RGC*T)
C    TAB(I,1,1P) WILL CONTAIN ENTHALPY
C    XSIH IS CP
      XSIH=GAMA*RGC/(GAMA-1.)
      H=H1+XSIH*(T-T1)
      H0=TAB(I,1,1)
      Q=SQRT(2.*(H0-H))
      RHO= P/(T*RGC)*32.174
      EM = Q/A
      WM=TAB(I,7,1)
      R=RGC
      T0=T+(GAMA-1.)/(2.*GAMA*R)*Q**2
      P0=P*(T0/T)**(GAMA/(GAMA-1.))
100 RETURN
      END

```

\$IBFTC CEMDAT DECK

BLOCK DATA

```
COMMON/GASFO/GASNAM(10,5,4),GNUM(10,5,4),NML(10,4),
1FZG(10,4),FXG(10,4),ENTHG(10,4),RTEMPG(10,4)
COMMON/NUMG/IG1,IG2,IG3,IG4,PCMAX,IG
DATA IG1/3/,IG2/4/,IG3/1/,IG4/1/
DATA(GASNAM(1,1,1),I=1,5)/2HS ,2HF ,2H ,2H ,2H /
DATA(GNUM(1,1,1),I=1,5)/1.0,6.0,0.0,0.0,0.0/
DATA NML(1,1)/1HM/,FZG(1,1)/1HG/,FXG(1,1)/1HF/
DATA(GASNAM(2,1,1),I=1,5)/2HC ,2HF ,2H ,2H ,2H /
DATA (GNUM(2,1,1),I=1,5)/1.0, 4.0,0.0,0.0, 0.0, 0.0/
DATA NML(2,1)/1HM/,FZG(2,1)/1HG/,FXG(2,1)/1HF/
DATA(GASNAM(3,1,1),I=1,5)/2HC ,2HH ,2HF ,2H ,2H /
DATA (GNUM(3,1,1),I=1,5)/1.0, 1.0, 3.0,0.0,0.0/
DATA NML(3,1)/1HM/,FZG(3,1)/1HG/,FXG(3,1)/1HF/
DATA (GASNAM(1,1,2),I=1,5)/2HN ,2H ,2H ,2H ,2H /
DATA (GNUM(1,1,2),I=1,5)/2.0,0.0,0.0,0.0,0.0/
DATA NML(1,2)/1HM/,FZG(1,2)/1HG/,FXG(1,2)/1HF/
DATA (GASNAM(2,1,2),I=1,5)/2HAR,2H ,2H ,2H ,2H /
DATA (GNUM(2,1,2),I=1,5)/1.0,0.0,0.0,0.0,0.0/
DATA NML(2,2)/1HM/,FZG(2,2)/1HG/,FXG(2,2)/1HF/
DATA (GASNAM(3,1,2),I=1,5)/2HH ,2H ,2H ,2H ,2H /
DATA (GNUM(3,1,2),I=1,5)/2.0,0.0,0.0,0.0,0.0/
DATA NML(3,2)/1HM/,FZG(3,2)/1HG/,FXG(3,2)/1HF/
DATA (GASNAM(4,1,2),I=1,5)/2HN ,2HO ,2H ,2H ,2H /
DATA (GNUM(4,1,2),I=1,5)/2.0, 1.0,0.0,0.0,0.0/
DATA NML(4,2)/1HM/,FZG(4,2)/1HG/,FXG(4,2)/1HF/
DATA (GASNAM(1,1,3),I=1,5)/2HC ,2HO ,2H ,2H ,2H /
DATA (GNUM(1,1,3),I=1,5)/1.0, 2.0, 0.0, 0.0, 0.0/
DATA NML(1,3)/1HM/,FZG(1,3)/1HG/,FXG(1,3)/1HF/
DATA (GASNAM(2,1,3),I=1,5)/2HC ,2HCL, 2HF ,2H ,2H /
DATA (GNUM(2,1,3),I=1,5)/1.0, 1.0, 3.0,0.0,0.0/
DATA NML(2,3)/1HM/,FZG(2,3)/1HG/,FXG(2,3)/1HF/
END
```

```

$IBFTC ITSUB1 DECK
      SUBROUTINE ITSUB (FOFY,Y,SAVE,CONV,NTIMES)
C      REVISED MARCH 5, 1969
C      THIS SUBROUTINE PROVIDES ITERATION CONTROL FOR ANY FUNCTION      0010
C      OF ONE VARIABLE                                                  *20
C      (FOFX)-FUNCTION WHICH IS DRIVEN TO ZERO                          0030
C      (X)-VARIABLE WHICH IS ITERATIVELY SOLVED FOR                     0040
C      (SAVE)-PROGRAM CONTROL                                           050
C      SAVE(1)=ITIME                                                    060
C      SAVE(2)=X INCREMENT                                              0070
C      SAVE(3)=COUNTER DENOTING NTH ITERATION                           0080
C      SAVE(4-7)=STORAGE LOCATIONS FOR X AND FOFX                       0090
C      SAVE( 9-12) = STORAGE LOCATIONS FOR SUCCESSIVE X VALUES
C      SAVE(13-14) = STORAGE LOCATIONS FOR MX AND NXX
C      SAVE(15) = ITERATION TIME SUBTOTAL
C      SAVE(16) = FOFY
C      (CONV)-CONVERGENCE CRITERIA                                     0100
C      (NTIMES)-MAX NUMBER OF ITERATIONS                               0110
      DIMENSION SAVE(16)
      MX = SAVE(13)
      NXX = SAVE(14)
      N1=SAVE(3) +.1
      N2=SAVE(15)+1.0
      SAVE(16) = FOFY
      IF(N2.NE.1) GO TO 5
      NXX=0
      MX = 8
5 CONTINUE
      NX=N2/4 - NXX
      FOFXCK=SAVE(8)
C      FOFY AND Y ARE DUMMY INPUT ARGUMENTS                             0150
      FOFX=FOFY                                                         0160
      X=Y                                                                0170
C      CHECK FOR CONVERGENCE                                           0180
      IF(ABS (FOFX)-CONV.LE.0.)GOTO110                                  0190
      ITIME=SAVE(1)+.1                                                  0200
C      ITIME CONTROLS THE TYPE CALCULATION TO BE PERFORMED           0210
C      ITIME=1,FIRST TIME THROUGH                                     0220
                                                                0230

```


C	ITIME=2, POS FIRST TIME THROUGH	0240
C	ITIME=3, NEG FIRST TIME THROUGH	0250
C	ITIME=4, SOLUTION IS BRACKETED	0260
C	ITIME=5, SOLUTION HAS CONVERGED	0270
C	ITIME=6, SOLUTION WILL NOT CONVERGE	0280
C	AJUMP=0.0	
	GOTO(10,30,50,70),ITIME	0290
C	INITIALIZE	0300
10	N1=1	0310
	ITIME=2	0320
	FOFXCK=FOFX	0330
	SAVE(8)=FOFXCK	0340
	IF(FOFX.LT.0.)GOTO50	0350
30	IF(FOFX.LT.0.)GOTO70	0360
	IF(FOFXCK.GE.FOFX)GOTO35	0370
	SAVE(2)=-1.*SAVE(2)	0380
	X=X-2.*SAVE(2)	0390
	GOTO90	0400
35	IF(N1.EQ.1) GO TO 40	
C	ACHECK=(SAVE(5)-FOFX)/SAVE(5)	
C	IF(ACHECK.LT.0.3) AJUMP=+1.0	
C	IF(ACHECK.LT.0.2) AJUMP=+2.0	
40	SAVE(4)=X	
	SAVE(5)=FOFX	0420
	X=X-SAVE(2)	0430
	GOTO90	0440
50	ITIME=3	0450
	IF(FOFX.GT.0.)GOTO70	0460
	IF(FOFXCK.LE.FOFX)GOTO55	0470
	SAVE(2)=-1.*SAVE(2)	0480
	X=X+2.*SAVE(2)	0490
	GOTO90	0500
55	IF(N1.EQ.1) GO TO 60	
C		
C	IF(ACHECK.LT.0.3) AJUMP=-1.0	
C	IF(ACHECK.LT.0.2) AJUMP=-2.0	
60	SAVE(6)=X	
	SAVE(7)=FOFX	0520

	X=X+SAVE(2)	0530
	GOTO90	0540
70	ITIME=4	0550
	N1=SAVE(3)	0560
	N2=0	
	IF(FOFX.LT.0.)GOTO75	0570
	SAVE(4)=X	0580
	SAVE(5)=FOFX	0590
	GOTO80	0600
75	SAVF(6)=X	0610
	SAVE(7)=FOFX	0620
C	PICK NEW GUESS FOR X ACCORDING TO TYPE CALCULATION	0630
80	X=SAVE(4)-SAVE(5)*((SAVE(6)-SAVE(4))/(SAVE(7)-SAVE(5)))	0640
90	IF(N1.GE.NTIMES)GOTO100	0650
C	X=X-AJUMP*SAVE(2)	
	MX=MX+1	
	SAVE(MX) = X	
	IF(NX.EQ.0) GO TO 92	
	MX = 8	
	NXX=NXX+1	
92	CONTINUE	
C	TEN ITERATION WILL BE ALLOWED BEFORE MAKING THE TEST OF X VALUE	
	IF(N1.LT.10) GO TO 95	
	IF((SAVE(12)-SAVE(10)).NE.0..OR.(SAVE(11)-SAVE(9)).NE.0.) GO TO 95	
C	X VALUE HAS BEEN REPEATING, SET ITIME=4 -- SO THAT THE VALUE OF	
C	SAVE(2) CAN BE ADJUSTED IN THE CALLING ROUTINE	
	ITIME=4	
	N2=0	
95	CONTINUE	
	N1=N1+1	*660
	SAVE(3)=N1	0670
	GOTO120	0680
100	ITIME=6	0690
	GOTO120	0700
110	ITIME=5	0710
	SAVE(4)=X	0720
	SAVE(5)=FOFX	0730
	SAVE(6)=X	0740

SAVE(7)=FOFX	0750
120 SAVE(1)=FLOAT(ETIME)+.1	0760
SAVE(13) = MX	
SAVE(14) = NXX	
SAVE(15)=N2	
Y=X	0770
RETURN	0780
END	0790

```

$IBFTC PROTO1 DECK
SUBROUTINE PROTO
C   PRODUCES PROTOTYPE PLUME
COMMON/GASES/TAB(3,12,13),NMIX
COMMON/REGION/XC11,XC12,XC13,ERRMAX,ITYPE
COMMON/PLUMF1/PRPR(10,4),REYPLM
COMMON/PLUMF2/PROP(10,200),IPT
COMMON/GEOM/AT,RADTHT,AEOAT,ANGLP,REYNP
COMMON/PNT/KPT(4)
COMMON/EXCON/PEX,EMU
DIMENSION H2O(10)
COMMON/MOLFRC/ZFRAC(40),KFR
COMMON /PROSAT/XSAT
INTEGER PNAME
COMMON/PROTG/PNAME(4,5),AOF(4),WTFRAC(2),PNUM(4,5),HENTH(4),
1HTEMP(4),PHAZ(4)
COMMON/SUNUP/SUN(3,40,2)
COMMON/PROTN/RADP,AETP,ANGP,PREP
COMMON/TAPE/IPROT
DATA LLK/1H /
COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),BO(15),BOP(15,2)
1  ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)
2  ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
3  ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4  ,RHOP,RMW(15),TLN
COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
1,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)
2,TOTN(13)
DATA(H2O(1),I=1,7)/-.111333E+03,-.816633E+02,+.273088E+02,+.110650E
$E+01,-.560044E+00,-.191904E-01,+.546921E-02/
DATAWATER,CARBO2/6HH2O  ,6HCO2  /
DIMENSION CO2(10),ARG(10),CON(10)
DATA(CO2(1),I=1,4)/-0.11763432E+03,-0.15185070E+02,+0.15828812E+0
$2,-0.16524522E+01/
C   LOAD GASES INTO CEC ARRAY
DO 20 I=1,5
NAME(1,I)=PNAME(I,I)
20 ANUM(1,I)=PNUM(I,I)

```

```

      PECWT(1)=WTFRAC(1)
      ENTH(1)=HENTH(1)
      RTEMP(1)=HTEMP(1)
      FOX(1)=AOF(1)
      FAZ(1)=PHAZ(1)
      DO 30 I=1,5
      NAME(2,I)=PNAME(2,I)
30  ANUM(2,I)=PNUM(2,I)
      PECWT(2)=WTFRAC(2)
      ENTH(2)=HENTH(2)
      RTEMP(2)=HTEMP(2)
      FOX(2)=AOF(2)
      FAZ(2)=PHAZ(2)
      NAME(3,1)=LLK
      P=PREP
C      IPROT CONTROL WHICH PRODUCTS TAPE WILL BE READ IN CEC
      IPROT=1
      CALL CEC(1,KASE)
      WRITE(6,52)
52  FORMAT(15X,8HH FT2/S2,5X,4HA/A*,7X,5HGAMMA,6X,5HM NO.,10X,5HP PSF,
      16X,7HT DEG R,5X,6HMOLE WT)
      NPT=KPT(1)
      WRITE(6,53)(( TAB(1,I,J),I=1,7),J=1,NPT)
53  FORMAT(13X,E10.3,2X,E10.3,2X,E10.3,2X,E10.3,2X,E10.3,2X,E10.3,
      $2X,E10.3)
C      COMPUTE REYNOLDS NO.
      RADTHT=RADP
      AEOAT=AETP
      ANGLP=ANGP
      AT = 3.174*RADP**2
      DEP = 2.*RADTHT*SQRT(AEOAT)
      CALL REYN(1,REY,IRCON)
      WRITE(6,4242) REY
4242 FORMAT(1H0,20X,37HPROTOTYPE EXIT PLANE REYNOLDS NO. IS E10.3)
C      PRODUCE SOURCE FLOW PLUME
      CALL SOURCE(IDUM,ISCON)
C      RESET PROTOTYPE PLUME POINTS TO THOSE AXIAL POSITIONS INPUT
      CALL RESET

```

```

C      COMPUTE APPROXIMATE REYNOLDS NUMBER FOR PROTOTYPE
      IF(IATYPE.EQ.3) CALL REYN(2,REYPL,IRCON)
      IPROT=0
C      RE-INITIALIZE TAB ARRAY TO ZERO
      DO 40 I=1,13
      DO 40 J=1,12
40     TAB(I,J,1)=0.
      REYNP=REY
      REYPLM=REYPL
C      TMAX=647.0
      TMAX = ALOG(300.)
      WRITE(6,778)KFR
      WRITE(6,779)(ZFRAC(IZ),IZ=1,KFR)
778    FORMAT(17H0ZFRAC ARRAY,KFR=15)
779    FORMAT(5X,8E10.3)
C      SEARCH SUN ARRAY FOR C02
      IH=0
      DO 10 I=1,10
10     CON(I)=C02(I)
50     IH=IH+1
      WRITE(6,777)SUN(1,IH,1)
777    FORMAT(10X,10HSUN ARRAY ,A6)
      IF(SUN(1,IH,1).EQ. WATER) GO TO 60
      IF(SUN(1,IH,1).EQ.CARB02) GO TO 60
      IF(IH.EQ.KFR)GO TO 55
      GO TO 50
55     XSAT=1000.
      GO TO 150
60     HMOL=ZFRAC(IH)
      WRITE(6,1881) HMOL
1881   FORMAT(17HOHMOLE IN PROTO =E10.3)
      IF(HMOL.LE.1.E-06) GO TO 55
C      SEARCH PLUME FOR SAT. POINT
      IT=0
70     IT=IT+1
C      CHANGE P AND T TO LOG VALUES BECAUSE VAPOR PRES. CURVE FIT
C      IS FOR LOG COOR.
      PL = ALOG(PROP(5,IT)/(14.7*144.)*HMOL)

```

```

      TL= ALOG(PROP(6,IT)/1.8)
      IF(TL.GE.TMAX) GO TO 70
C     PVAP= H2O(1)+H2O(2)*TL +H2O(3)*TL**2+ H2O(4)*TL**3+H2O(5)*TL**4
C     A+H2O(6)*TL**5+ H2O(7)*TL**6
      PVAP = CON(1)+CON(2)*TL+CON(3)*TL**2 +CON(4)*TL**3
      IF(PL.LE.PVAP) GO TO 80
C     FOR BRACKETED POINT
      DT=TH-TL
      DP1=PLH-FL
      DP2= PVAPH-PVAP
      SLP1=DP1/DT
      SLP2=DP2/DT
      GO TO 90
80    CONTINUE
      IF(IT.EQ.1) GO TO 120
      PLH=PL
      PVAPH=PVAP
      TH=TL
      GO TO 70
90    CONTINUE
      TINSCT = EXP((PVAP-PL + TL*(SLP1-SLP2))/(SLP1-SLP2))
      TLI = ALOG(TINSCT)
      PINSCT = EXP(SLP1*(TLI-TL)+PL)
      PTINS = PINSCT/HMOL
C     COMPUTE AXIAL LOCATION OF CONDENSATION
      SLPX = ALOG(PROP(5,IT)/PROP(5,IT-1))/ALOG(PROP(1,IT)/PROP(1,IT-1))
      ONOS= 1./SLPX
      XINSCT= PROP(1,IT-1)*EXP(ONOS*ALOG(PTINS/PROP(5,IT-1)))
      WRITE(6,100) XINSCT
100   FORMAT(10X,38HPROTOTYPE CONDENSATION OCCURS AT .....E10.3)
      GO TO 130
120   WRITE(6,121)
121   FORMAT(10X,56HSATURATION OCCURS IN OR NEAR NOZZLE, XINSCT SET TO
      *ZERO)
      XINSCT=0.
130   XSAT = XINSCT
150   CONTINUE
      RETURN
      END

```

```

$X
$ORIGIN      B
$IBFTC COMP
      SUBROUTINE COMPAR(ITYP,ICK,IRCON,KASE)
      COMMON/PLUNMU/XC(5),PC(5),EMC(5),GMC(5),TC(5),QC(5),EMWC(5)
      COMMON/GASES/TAB(3,12,13),NMIX
      COMMON/SUNUP/SUN(3,40,2)
      COMMON/WRIT/IFLG1
      COMMON/TAPE/IPROT
      COMMON/NUMG/IG1,IG2,IG3,IG4,PCMAX,IG
      COMMON/CHANGE/PC11,PC21,PC22,PC31,PC32,PC33,PNW,TNW,DELM,DELMN,
$DELREY
      COMMON/GEOM/AT,RADTHT,AEOAT,ANGLP,REYNP
      COMMON/REGION/XC11,XC12,XC13,ERRMAX,ITYPE
      COMMON/PLUMF1/PRPR(10,4),REYPLM
      DIMENSION EP(50),EPS(5)
      ICK=0
      KACE = KASE
      IF(ITYP.GT.1)GO TO 100
      CALL REYN(1,REY,IRCON)
      WRITE(6,5)REY
5  FORMAT(20X,21HSIMULANT RN AT EXIT =,E10.3)
      IF(REY.LT.REYNP)ICK=2
      GO TO 300
100 CONTINUE
      CALL RESET
      GO TO (120,130,140),ITYPE
120 CONTINUE
C  COMPARE PLUME REGION FOR MOMENTUM FLUX
      EPSUM=0
      DO 50 J=1,3
      G1=GMC(J)
      P1=PC(J)
      EM1=EMC(J)
      G2=PRPR(3,J)
      P2=PRPR(5,J)
      EM2=PRPR(4,J)
C  COMPUTE ERROR

```



```

      EPS(J)=FMOM(G1,P1,FM1)-FMOM(G2,P2,EM2)
      EPSUM=EPSUM+EPS(J)
50  CONTINUE
      EP(KACE)=EPSUM
      WRITE(6,60)EPSUM,KACE
60  FORMAT(2CX,23HSUMMATION OF MOM ERROR=,E10.3,2X,10HFOR CASE  ,15)

C
C      ALSO COMPARE CENTER PT.
      DELM=EPS(2)
      PCM=DELM/FMOM(PRPR(3,2),PRPR(5,2),PRPR(4,2))
      WRITE(6,70)DELM,PCM
70  FORMAT(1H2,5HDELM=,E10.3,5X,4HPCM=,E10.3)
      IF(ABS(PCM).GT..1*ERRMAX) ICK=3
      GO TO 300
130  CONTINUE
C      COMPARE PLUME REGION FOR MACH NO.
      DELMN=EMC(4)-PRPR(4,2)
      PCMN = DELMN/PRPR(4,2)
      WRITE(6,132) DELMN,PCMN
132  FORMAT(20X,17HOMACH NO. ERROR= E10.3,2X,18HPERCENTAGE ERROR= E10.3)
      $)
      IF(ABS(PCMN).GT..1*ERRMAX) ICK=3
      GO TO 300
140  CONTINUE
C      COMPARE PLUME REGION FOR REYNOLDS NJMBER
      CALL REYN(2,REYM,IRCON)
      DELREY=REYPLM-REYM
      PCREY= DELREY/REYNP
      WRITE(6,142) DELREY,PCREY
142  FORMAT(20X, 21HOREYNOLDS NO. ERROR= E10.3,2X,18HPEPCENTAGE ERROR =,
      1E10.3)
      IF(ABS(PCREY).GT..1*ERRMAX) ICK=3
300  CONTINUE
      RETURN
      END

```

```
$IBFTC FMOM1 DECK  
      FUNCTION FMOM(G,P,EM)  
      FMOM=G*P*EM**2  
      RETURN  
      END
```

```

$IBFTC REYN1
      SUBROUTINE REYN(LTYPE,REY,IRCON)
C      SUBROUTINE REYN COMPUTES REYN. NO. AT EXIT PLANE
C      USING PROPERTIES FROM THE TAB ARRAY
C
      COMMON/GASES/TAB(3,12,13),NMIX
      COMMON/SUNUP/SUN(3,40,2)
      COMMON/SPNAME/SPNAM1(90),SPNAM2(90),TEMP( 5, 90),IDATA,KK,KT
      COMMON/NUMG/IG1,IG2,IG3,IG4,PCMAX,IG
      COMMON/GASCON/GAMA,R,T0,P0,EM,RHO,T,WM ,Q
      COMMON/GEOM/AT,RADTHT,AEOAT,ANGLP,REYNP
      COMMON/EXCON/PEX,EMU
      COMMON/PLUMF1/PRPR(10,4),REYPLM
      COMMON/TAPE/IPROT
      COMMON/PLUNMU/XC(5),PC(5),EMC(5),GMC(5),TC(5),QC(5),EMWC(5)
      COMMON/MOLFRC/ZFRAC(40),KFR
      COMMON/WRIT/IFLG1
      COMMON/COUNT/IKLUG
      DIMENSION SAVEA(16)
      DATA (SAVEA(K),K=1,16) /16*0./
      EQUIVALENCE (GAMA,GAMA)
      IRCON=0
C      REYN COMPUTES REYNOLDS NO. AT AT PT. KNOWING THE THERMO
C      PROPERTIES..... EXIT CONDITIONS ARE GENERALLY CALLED
C      FIRST GUESS FOR EXIT PRESSURE
      P=.005*TAB(1,5,1)
      SSQR=AEOAT
      TOL=.005*SSQR
      SAVEA(1)=1.0
      PINC=-.09*P
      SAVEA(2)=PINC
      PSTAR=TAB(1,5,2)
      CALL TABLE(PSTAR,1)
      RSTAR=RHO
      QSTAR=Q
C      BYPASS EXIT PLANE CALC IF PLUME RN IS DESIRED
      IF(LTYPE.EQ.2)GO TO 200
18 CONTINUE

```

```

        IF(P.GT.0.)GO TO 30
        P=P-.95*PINC
        PINC=.1*PINC
        SAVEA(2)=PINC
30  CONTINUE
        CALL TABLE(P,1)
        ARAT=RSTAR*QSTAR/(RHO*Q)
        FP= SSQR-ARAT
        GO TO 198
        WRITE(6,39)
39  FORMAT(20H0TABLE CHECK--GASCON)
        WRITE(6,40)GAMA,R,T0,P0,EM,RHO,T,WM,Q
40  FORMAT(10X,9E10.3)
        WRITE(6,4000)RHO,Q,GAMA,GAMMA
4000 FORMAT(1H0,4HRHO=E10.3,2HQ=E10.3,5HGAMA=E10.3,6HGAMMA=E10.3)
        WRITE(6,100)SSQR,ARAT,FP,P,SAVEA(2)
100  FORMAT(6H0SSQR=,E10.3,5HARAT=,E10.3,3HFP=,E10.3,5HPRES=,E10.3,
15HPINC=,E10.3)
198  CONTINUE
        CALL ITSUB(FP,P,SAVEA,TOL,199)
        II=SAVEA(1)+.1
        NI=SAVEA(3)+.1
        GO TO (18,18,18,18,22,23),II
23  WRITE(6,600)FP,P
600  FORMAT(36H0ITSUB WILL NOT CONVERGE IN REYN,FP=,E10.3,5X,2HP=,E10.3
1)
        IRCON=1
        RETURN
22  CONTINUE
        PEX = P
        GO TO 300
200  CONTINUE
C    LOAD PLUME PROPERTIES INTO P AND T
        IF(IPROT.EQ.1) GO TO 210
        P=PC(2)
        T=TC(2)
        GO TO 300
210  P=PRPR(5,2)

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```

      T=PRPR(6,2)
300 CONTINUE
      GO TO 400
      IF(IPROT.EQ.1) GO TO 400
      TR=T
C     THE FIRST DIGIT IN TAB AND SUN INDICATES IF GAS IS MIXTURE
C     OR COMPONENT
C     3RD DIGIT OF SUN INDICATES PART OF GAS NAME
C     FIRST LOAD THE NAME INTO TEMP
      K=NMIX+8
      DO 5 KM=1,NMIX
        TEMP(1,KM+7)=SUN( 1,KM,1)
      5 TEMP(2,KM+7)=SUN(1,KM,2)
C     LOAD MOLE FRACTION INTO TEMP
C     IF PROTOTYPE CALC.. USE MOLE FRAC. FROM ZFRAC
      IF(IPROT.EQ.1)GO TO 70
      DO 10 KM=9,K
      10 TEMP(3,KM-1)=TAB(1 ,KM,1)
      GO TO 80
      70 CONTINUE
      DO 75 KL=1,KFR
      75 TEMP(3,KL+7)=ZFRAC(KL)
      80 CONTINUE
      IWRT=1
      WRITE(6,16)
      16 FORMAT(51HORE WRITING GAS NAME AND MOLE FRACTION USED IN REYN)
      DO 17 N=1,NMIX
      17 WRITE(6,28) TEMP(1,N+7),TEMP(2,N+7),TEMP(3,N+7)
      28 FORMAT(1H0,5X,2A6,E10,3)
      15 CONTINUE
      CALL TRANS(TR,1,EMU)
C     COMPUTATION OF REYNOLDS NO.
      REX =RADTHT*SQRT(AEOAT)
      EMU=EMU*.0671983
      REY= RHO*Q*2.0*REX/EMU
      GO TO 500
      400 ROUSTR=RSTAR*QSTAR
      VIS = .1335E-4*(T/1.8)**.95
      EL= RADTHT*SQRT(AEOAT)
      REY=ROUSTR*2.*EL/VIS
      500 CONTINUE
      RETURN
      END

```

```

$ORIGIN      C
$IBFTC CONDNS
      SUBROUTINE CONDEN(ICON,ISWTCH,IACP,TONEW)
      COMMON/GASES/TAB(3,12,13),NMIX
C      COEFFICIENTS FOR VAPOR PRESSURE CURVES ARE COMPUTED FOR LOG
      COMMON/PLUMF2/PROP(10,200),IPT
      COMMON/PROSAT/XSAT
      COMMON/SUNUP/SUN(3,40,2)
      COMMON/MOLFRC/ZFRAC(40),KFR
      COMMON/REGION/XC11,XC12,XC13,ERRMAX,ITYPE
      COMMON/MGEOM/ATM,RADTHM,AE0ATM,ANGLPM
      DATA CARB02/6HC02 /
C      COMPARE PROPERTY ALONG EXPANSION--PROP--WITH VAPOR PRESSURE
C      CURVE
C      TYPE FIT. THUS THE CONVERSION OF THE PLUME DATA.
C
      DIMENSION CO2(10),ARG(10),CON(10)
      DATA(CO2(I),I=1,4)/-0.11763432E+03,-0.15185070E+02,+0.15828812E+0
$2,-0.16524522E+01/
C      TEST GAS TYPE
      IF(ICON.EQ.2)GO TO 20
      DO 10 I=1,10
10    CON(I)=CO2(I)
      TMAX=ALOG(300.)
      GO TO 40
20    DO 30 I=1,10
30    CON(I)=ARG(I)
      TMAX=ALOG(300.)
40    CONTINUE
      IH =0
150   IH=IH+1
      WRITE(6,777)SUN(1,IH,1)
777   FORMAT(10X,10HSUN ARRAY ,A6)
      IF(SUN(1,IH,1).EQ.CARB02) GO TO160
      GO TO150
160   XCON=ZFRAC(IH)
      WRITE(6,500)XCON
500   FORMAT(20X,5HXCON=E10.3)

```

```

      I=0
50  I=I+1
      P1= ALOG (PROP(5,I)*XCON/(14.7*144.))
      T1=ALOG (PROP(6,I)/1.8)
      IF(T1.GE.TMAX)GO TO 50
      ISWTC=0
      P2=CON(1)+CON(2)*T1+CON(3)*T1**2+CON(4)*T1**3
C    TEST IF LINES CROSS
      IF(P1.LE.P2)GO TO 60
C    NOW HAVE INTERSECTION BRACKETED
      DT=TH-T1
      DP1=P1H-P1
      DP2=P2H-P2
      SLP1=DP1/DT
      SLP2=DP2/DT
      GO TO 80
60  P1H=P1
      P2H=P2
      TH=T1
      GO TO 50
80  TINRST=(P2-P1+T1*(SLP1-SLP2))/(SLP1-SLP2)
      PINRST= SLP1*(TINRST-T1)+P1
      WRITE(6,501)P1,T1,P2,DT,SLP1,SLP2,TINRST,PINRST
501  FORMAT(10X,8E10.3)
C
C    OBTAIN MOLE FRACTION OF CONDENSANT
C    NOW INTERPOLATE FOR AXIAL POSITION OF CONDENSATION
C    FIRST CALC. ACTUAL PRESSURE AND TEMP
      TI=EXP(TINRST)
      PIT = EXP(PINRST)
      PI = PIT*14.7*144./XCON
      WRITE(6,90)
90  FORMAT(20X,31HOCONDENSATION PROPERTIES FOLLOW)
      WRITE(6,91)TI,PI
91  FORMAT(1H0,19X,3HT2=,E10.3,2X,3HPI=,E10.3)
      X1H=PROP(1,I-1)
      SLPX=ALOG(PROP(5,I)/PROP(5,I-1))/ALOG(PROP(1,I)/PROP(1,I-1))
      ONOM=1./SLPX

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```

      XI=XIH*EXP(ONOM*ALOG(PI/PROP(5,I-1)))
      WRITE(6,100)XI
100  FORMAT(1H0,14X,28HSIMULANT CONDENSATION PT. IS,E10.3)
C    COMPUTE PERCENT DIFFERENCE
      DX=XSAT-XI
      DEPM = 2.*RADTHM*SQRT(AEOAT)
      DIFF = 20.*DEPM
C    DETERMINE IF ERROR ACCEPTABLE
      IF(XI.GT.XC13.AND.XSAT.GT.XC13)GO TO 200
      IF(DX.LE.DIFF) GO TO 200
      ISWTCH=1
C    IF NOT COMPUTE A DESIRED CHANGE IN TO TO ADJUST THE PT.
      GOGM1=(PROP(3,I)-1.)/PROP(3,I)
C
C    KNOWING DESIRED SATURATION POSITION A NEW PRESSURE IS COMPUTED
      PNEW= PI*EXP(SLPX*ALOG(XSAT/XI))
      DELP= PNEW-PI
      IACP=1
      TONEW= (DELP/TAB(1,5,1))*GOGM1*TAB(1,6,1)*DELP**(.1/SLP1)
C    IS TONEW ACCEPTABLE
      IF(TONEW.LT.2000.)IACP=0
      WRITE(6,105)TONEW
105  FORMAT(1H0,20X,18HNEW TO COMPUTED IS,E10.3)
200  RETURN
      END

```



```

$IBFTC REST1  DECK
SUBROUTINE RESET
COMMON/TAPE/IPROT
COMMON/PLUNMU/XC(5),PC(5),EMC(5),GMC(5),TC(5),QC(5),EMWC(5)
COMMON/PLUMF1/PRPR(10,4),REYPLM
COMMON/PLUMF2/PROP(10,200),IPT
COMMON/REGION/XC11,XC12,XC13,ERRMAX,ITYPE
C   RESETS SIMULANT PLUMF PTS. TO THOSE STATIONS
C   COMPUTED FOR PROTOTYPE CASE
      IF(IPROT.EQ.1) GO TO 40
      I=0
      J=0
      5  J=J+1
      10 I=I+1
      IF(PRPR(1,J).GT.PROP(1,I))GO TO 10
      XQ=PRPR(1,J)
      XC(J)=XQ
      SLP1=ALOG(PROP(5,I)/PROP(5,I-1))/ALOG(PROP(1,I)/PROP(1,I-1))
      PC(J)= PROP(5,I-1)*EXP(SLP1*ALOG(XQ/PROP(1,I-1)))
C
      SLP2=(PROP(4,I)-PROP(4,I-1))/(PROP(1,I)-PROP(1,I-1))
      EMC(J)= SLP2*(XQ-PROP(1,I-1))+PROP(4,I-1)
C
      SLP3=(PRPR(3,I)-PRPR(3,I-1))/(PROP(1,I)-PROP(1,I-1))
      GMC(J)=SLP3*(XQ-PROP(3,I-1))+PROP(3,I-1)
      XSIP=ALOG(PROP(5,I-1)/PROP(5,I))/ALOG(PROP(6,I-1)/PROP(6,I))
      ONOX=1.0/XSIP
      TC(J)= PROP(6,I-1)*(PC(J)/PROP(5,I-1))*ONOX
      RGC=1545./PROP(7,I-1)*32.174
      A=GMC(J)*RGC*TC(J)
      QC(J)= EMC(J)*SQRT(A)
      EMWC(J)=PROP(7,I-1)
      NPTS=3
      IF(J.EQ.NPTS)GO TO 20
      GO TO 5
      20 CONTINUE
      WRITE(6,25)
      25 FORMAT(1H0,10X,35H SIMULANT PLUME PROPERTIES AT X-CUTS)

```

```

        WRITE(6,27)
27  FORMAT(1H0,20X,1HX,10X,2HPC,10X,1HM,10X,1HG,10X,1HT,10X,2HMW,
        110X,1HQ)
        WRITE(6,26) ( XC(J),PC(J),EMC(J),GMC(J),TC(J),EMWC(J),QC(J) ,J=1,3)
26  FORMAT(25X,7E10,3)
        GO TO 100
40  CONTINUE
C    THE FOLLOWING SECTION PICKS OUT PROTOTYPE PTS IN REGION
        XC(1)=XC11
        XC(2)=XC12
        XC(3)=XC13
        I=0
        J=0
45  I=I+1
50  J=J+1
        IF(XC(I).GT.PROP(1,J))GO TO 50
        FAC1=ALOG(PROP(5,J)/PROP(5,J-1))/ALOG(PROP(1,J)/PROP(1,J-1))
        PRPR(5,I)= PROP(5,J)*EXP(FAC1*ALOG(XC(I)/PROP(1,J-1)))
        FAC2= (PROP(4,J)-PROP(4,J-1))/(PROP(1,J)-PROP(1,J-1))
        PRPR(4,I)= PROP(4,J-1)+ FAC2*(XC(I)-PROP(1,J-1))
        FAC3= (PROP(3,J)-PROP(3,J-1))/(PROP(1,J)-PROP(1,J-1))
        PRPR(3,I)= PROP(3,J-1)+ FAC3*(XC(I)-PROP(1,J-1))
        ONOX=1./( ALOG(PROP(5,J-1)/PROP(5,J))/ ALOG(PROP(6,J-1)/PROP(6,J))
        1)
        PRPR(6,I)=PROP(6,J-1)*(PRPR(5,I)/PROP(5,J-1))*ONOX
        PRPR(7,I)=PROP(7,J-1)
        PRPR(1,I)=XC(I)
        IF(I.EQ.3) GO TO 70
        GO TO 45
70  CONTINUE
        WRITE(6,75)
75  FORMAT(20X,33HPROTOTYPE PLUME POINTS FOR REGION)
        WRITE(6,80)
80  FORMAT(15X,1HX,10X,5HM NO.,10X,5HGAMMA,10X,1HP,10X,1HT,10X,2HMW)
        DO 90 IP=1,3
        WRITE(6,85)PRPR(1,IP),PRPR(4,IP),PRPR(3,IP),PRPR(5,IP),PRPR(6,IP),
        1PRPR(7,IP)
85  FORMAT(10X,6(E10,3,4X))
90  CONTINUE
100 CONTINUE
        RETURN
        END

```

```

$*
$ORIGIN      C

```

```

$IBFTC TRAN    DECK
      SUBROUTINE TRANS(TE,JDUM,VIS)
C
C**    PROGRAM WHICH CALCULATES TABLE OF VISCOSITY, CP AND THERMAL
C      CONDUCTIVITY FROM THE NASA-LEWIS EQUILIBRIUM CHEMISTRY DATA
C
C      TO LESSEN THE NO. OF CHANGES THAT MUST BE MADE, THE THERMODYNAMIC
C      DATA FOR THE TRANSPORT PROPERTIES WILL BE READ FROM TAPE 12, THE
C      OLD NASA/LEWIS DATA TAPE.
C      THE THERMODYNAMIC DATA FOR THE CEC PORTION WILL BE READ FROM TAPE
C      4, THE NEW DATA TAPE GENERATED BY MCDERMIT.
C      TO MAKE THESE COMPATABLE THE CEC IS MODIFIED TO READ THE GAS NAME
C      UNDER A 2A6 FORMAT.
      DIMENSION ZETA(4),BETA(4),BETEND(4)
      COMMON/SPDATA/AA(90,5),XMF(90),XMW(90),SIGMA(90),OMEGA(90),TR,N
      COMMON/SPNAME/SPNAM1(90),SPNAM2(90),TEMP( 5, 90),IDATA,KK,KT
      COMMON/THRMTR/A(90,15)
      COMMON/MO/NUM(90)
      COMMON/GASES/TAB(3,12,13),NMIX
      DATA (BETEND(I),I=1,4)/4*6HEND
      COMMON/WRIT/IFLG1
      COMMON/COUNT/IKLUG
      IDATA=NMIX+7
      TR=TE
      REWIND 13
      IV=3
C**    LOOP WHICH CALCULATES FLOW PROPERTIES
      DO 54 J=3,IV
1030  FORMAT(1H , (7E18.7))
      IF(TR.LT. 1.0) GO TO 9000
      KT = 0
      DO 55 K=8,IDATA
      IF(TEMP(J,K).LT..000005)GO TO 55
      IF(TEMP(J,K).GT.1.0   ) GO TO 55
      KT = KT + 1
C
C**    GAS SPECIE NAMES
C

```

```

        SPNAM1(KT) = TEMP(1,K)
        SPNAM2(KT) = TEMP(2,K)
55  CONTINUE
    IF(KT.EQ.0) GO TO 999
C
C**  LOCAL TEMPERATURE
    IERR = 0
    CALL GTLUP(J,IERR,IFIRST)
    IF(IERR.LQ.1) GO TO 99
C
C**  CALCULATE VISCOSITY,CP,CONDUCTIVITY
C
    CALL PROPTY(    VIS,COND,CP)
    TEMP(J,IDATA+1) = VIS
    TEMP(J,IDATA+2) = COND
    TEMP(J,IDATA+3) = CP
    GO TO 54
999  WRITE(6,1000)I,J
1000  FORMAT(1H0,33HNO SPECIE DATA FOR ENTROPY CUT = ,I2, 17H  VELOCITY
        CUT = ,I2)
    TEMP(J,IDATA+1) = 0.
    TEMP(J,IDATA+2) = 0.
    TEMP(J,IDATA+3) = 0.
    GO TO 54
9000  WRITE(6,9001)
9001  FORMAT(1H , 20HNegative TEMPERATURE )
    TEMP(J,IDATA+1) = 0.
    TEMP(J,IDATA+2) = 0.
    TEMP(J,IDATA+3) = 0.
54  CONTINUE
99  CONTINUE
C
    RETURN
    END

```

\$ORIGIN D
\$IBFTC PROP DECK
C

SUBROUTINE PROPTY(VISCOS,COND, CP)
C** THIS SUBROUTINE CALCULATES THE GAS VISCOSITY, THERMAL CONDUCTIVITY
C AND CP AS A FUNCTION OF TEMPERATURE
C DIMENSION TABLJP(131)
C DIMENSION CPR(90), XP(4,90), F(4),XA(90),D(90,90)
C COMMON/WRIT/IFLG1

COMMON/SPDATA/AA(90,5),XMF(90),XMW(90),SIGMA(90),OMEGA(90),TR,N
C** THIS TABLE IS THE REDUCED COLLISION INTEGRAL FROM HIRSHFELDER
COMMON/SPNAME/SPNAM1(90),SPNAM2(90),TEMP(5, 90),IDATA,KK,KT

C 1 THE HIRSHFELDER SYMBOL EQUALS OMEGA***2.2

DATA TABLJP /65..	.3 ,	.4 ,	.5 ,	.6 ,	.7 ,	.8 ,		01150
* .9 ,	1. ,	1.1 ,	1.2 ,	1.3 ,	1.4 ,	1.5 ,	1.6 ,	01160
* 1.7 ,	1.8 ,	1.9 ,	2.0 ,	2.1 ,	2.2 ,	2.3 ,	2.4 ,	01170
* 2.5 ,	2.6 ,	2.7 ,	2.8 ,	2.9 ,	3.0 ,	3.1 ,	3.2 ,	01180
* 3.3 ,	3.4 ,	3.5 ,	3.6 ,	3.7 ,	3.8 ,	3.9 ,	4.0 ,	01190
* 4.1 ,	4.2 ,	4.3 ,	4.4 ,	4.5 ,	4.6 ,	4.7 ,	4.8 ,	01200
* 4.9 ,	5. ,	6. ,	7. ,	8. ,	9. ,	10. ,	20. ,	01210
* 30. ,	40. ,	50. ,	60. ,	70. ,	80. ,	90. ,	100. ,	01220
* 200. ,	300. ,	400. ,						01230
\$	2.785 ,	2.492 ,	2.257 ,	2.065 ,	1.908 ,	1.780 ,		01240
\$ 1.675 ,	1.587 ,	1.514 ,	1.452 ,	1.399 ,	1.353 ,	1.314 ,	1.279 ,	01250
\$ 1.248 ,	1.221 ,	1.197 ,	1.175 ,	1.156 ,	1.138 ,	1.122 ,	1.107 ,	01260
\$ 1.093 ,	1.081 ,	1.069 ,	1.058 ,	1.048 ,	1.039 ,	1.030 ,	1.022 ,	01270
\$ 1.014 ,	1.007 ,	.9999 ,	.9932 ,	.9870 ,	.9811 ,	.9755 ,	.9700 ,	01280
\$.9649 ,	.9600 ,	.9553 ,	.9507 ,	.9464 ,	.9422 ,	.9382 ,	.9343 ,	01290
\$.9305 ,	.9269 ,	.8963 ,	.8727 ,	.8538 ,	.8379 ,	.8242 ,	.7432 ,	01300
\$.7005 ,	.6718 ,	.6504 ,	.6335 ,	.6194 ,	.6076 ,	.5973 ,	.5882 ,	01310
\$.5320 ,	.5016 ,	.4811 /						01320

C
C THE AA ARRAY IS DEFINED AS THE FOLLOWING
C ** THIS DATA TAKEN FROM NASA LEWIS THERMOCHEMISTRY DATA DECK **
C
C 1 THE FIRST FIVE NUMBERS OF EACH TWO CARD SET
C 2 ARE POLYNOMIAL COEFFICIENTS OF A CURVE FIT
C 3 OF CP/R FOR A TEMPERATURE RANGE DEPENDING ON TK

```

C      XMF=MASS FRACTION
C      XMW=MOLECULAR WEIGHT
C      CPR=CPAR
C      RU=UNIVERSAL GAS CONSTANT
C      VISCOS=VISCOSITY
C      COND=THERMAL CONDUCTIVITY
C      CP=SPECIFIC HEAT AT CONSTANT PRESSURE
      TK = TR/ 1.8
      RU = 1.98726
      DO 840 I = 1, N
      XP(4, I) = XMW(I)
      CPR(I) = AA(I,1)
      DO 830 J = 2, 5
      AT = AA(I,J)
      DO 820 JJ= 2,J
      820 AT = AT * TK
      830 CPR(I) = CPR(I) + AT
      XP(3,I) = CPR(I)
      840 CONTINUE
      DO 850 I = 1, N
      TRED = TK / OMEGA(I)
      CALL ONEVAR( TRED, 2, TABLJP, 1, 131, OMERED)
      IF(IFLG1.EQ.0)GO TO 191
      WRITE(6,1032)TRED,OMERED,I
1032 FORMAT(1H0, 6HTRED =,E15.7,5X, 8HOMERED =, E15.7, 5X, 3H I=,I3)
      191 CONTINUE
      XP(1, I)=266.93 *10.**(-7)*SQRT(XMW(I)*TK )/(SIGMA(I)**2*OMERED)
      850 XP(2, I) =(RU/XMW(I))*(3.75 +1.32*(CPR(I)- 2.5))*XP(1, I)
      IF(IFLG1.EQ.0)GO TO 192
      WRITE(6,1035)
1035 FORMAT(1H , 35HRESULTS OF TRANSPORT PROPERTY CALCS,/, 6HSPECIE,7X
      1, 6HVISCOS,8X, 4HCOND,10X, 2HCP, 12X, 7HMOL, WT,7X, 9HMOL FRACT,
      2 5X, 5HOMEGA, 9X, 5HSIGMA, 9X,11HTEMP(DEG K),/)
      192 CONTINUE
      DO 600 I=1,N
      IF(IFLG1.EQ.0)GO TO 193
      600 WRITE(6,1040) SPNAM1(I),SPNAM2(I),(XP(K,I),K=1,4),XMF(I),OMEGA(I),
      1 SIGMA(I),TK

```

1040	FORMAT(1H0, 2A6, 1X, (8(E12.5, 2X)))	
193	CONTINUE	
900	CONTINUE	01730
	DO 500 K = 1,4	01740
C		01750
C	FOR K = 1 VISCOSITY OF MIXTURE CALCULATED	01760
C	K = 2 CONDUCTIVITY OF MIXTURE CALCULATED	01770
C	K = 3 CP OF MIXTURE CALCULATED	01780
C	K = 4 MOLE WEIGHT OF MIXTURE CALCULATED	01790
C		01800
	VISCOS = 0.	01810
	COND = 0.	01820
	CP = 0.	01830
	OLWT = 0.	01840
	F(K) = 0.	01850
	DO 400 I=1,N	01860
	XA(I) = 0.0	01870
	IF (K.EQ.4) GO TO 320	
	DO 300 J=1,N	01880
	IF (J.EQ. 1) GO TO 300	01890
	D(I,J) = .376*(1. + SQRT(XP(K,I) / XP(K,J)) * (XMW(J)/XMW(I))	01900
	1 ** .25)**2*SQRT(XMW(J)/(XMW(I)+XMW(J)))	01910
	XA(I) = XA(I) + XMF(J) * D(I,J)	
300	CONTINUE	01930
	IF(XMF(I).LT..000001) GO TO 400	01940
310	F(K) = F(K) + (XMF(I) * XP(K,I)) / (XMF(I) + XA(I))	01950
	GO TO 400	
320	F(K) = F(K) + XP(K,I)*XMF(I)	
400	CONTINUE	01960
500	CONTINUE	01970
C	UNITS-POISES	
	VISCOS=F(1)	
C	UNITS-ENGLISH	
	COND = F(2)	
C	UNITS-BTU/LBM/DEG-R	
	CP = F(3) * RU / F(4)	02000
	OLWT = F(4)	02010
	RETURN	02020
	END	02030

\$1BFTC ONEV	DECK		02050
	SUBROUTINE ONEVAR (ARGUMT,NXDIR, TABLE, NOTAB, NX, OUTPUT)		2060
C			02070
C	ONEVAR IS AN INTERPOLATION ROUTINE - ONE FUNCTION OF ONE		02080
C	ARGUMENTS OF THE SUBROUTINE ARE AS FOLLOWS		02090
C	ARGUMT = INPUT INTERPOLATION ARGUMENT (X)		02100
C	NXDIR = TYPE OF INTERP. 1 FOR LINEAR, 2 FOR QUAD.		02110
C	TABLE = SET OF X VALUES FOLLOWED BY THE Y VALUES		02120
C	OUTPUT = INTERPOLATED VALUE OF Y = F(X)		02130
C	NER = ERROR CODE		02140
C	1 = OK, INTERPOLATION SUCCESSFUL.		02150
C	2 = OFF CHART LOW END. MIN. VAL. SUBSTITUTED		02160
C	3 = OFF CHART HIGH END. MAX. VAL. SUBSTITUTED		02170
C	4 = NO. OF X ENTRIES IS NOT 2 TO 15 (IF NXDIR		02180
C	IS 1). OR, IT IS NOT 3 TO 15 (IF NXDIR		02190
C	IS 2).		02200
C	5 = X ENTRIES NOT IN ASCENDING ORDER.		02210
C			02220
C	TABLE IS LOADED AS	LOC. VALUE	02230
C		TABLE(1) NO. OF X VALUES	02240
C		TABLE(2) X(1)	02250
C			02260
C		ETC	02270
C		TABLE(N+1) X(N)	02280
C		TABLE(N+2) Y(1) WHERE Y = F(X)	02290
C			02300
C		ETC	02310
C		TABLE(N+1+N) Y(N)	02320
C			02330
	DIMENSION TABLE(NX)		02340
	NOENTR = INT(TABLE(1))		02350
	N = NOENTR		02360
	NER = 1		02370
	IF (NXDIR-1) 1,1,2		02380
1	IF (NOENTR-2) 4,3,3		02390
2	IF (NOENTR-3) 4,3,3		02400
3	IF (NXDIR + 1 - NOENTR) 5, 9, 4		02410
4	NER = 4		

GO TO 701	02420
5 IF (ARGUMT-TABLE(2)) 6,7,10	02430
6 NER = 2	02440
GO TO (23, 32), NXDIR	02450
7 NER = 1	02460
8 IOUT = 2	02470
GO TO 700	02480
9 GO TO (23, 32), NXDIR	02490
10 IF (TABLE(NOENTR+1)-ARGUMT) 11,13,16	02500
11 NER = 3	02510
I = N - 1	02520
GO TO (25, 31), NXDIR	02530
13 NER = 1	02540
14 IOUT = NOENTR+1	02550
15 GO TO 700	02560
C AT THIS STAGE OF THE GAME, ERROR CONDITIONS 2,3,4 HAVE	02570
C BEEN TESTED FOR AND HAVE BEEN PASSED.	02580
16 DO 100 JK=1, NOENTR	02590
I = JK	02600
IF (I-1) 20,20,17	02610
17 IF (TABLE(I+1)-TABLE(I)) 18,18,20	02620
18 NER = 5	02630
GO TO 701	02640
20 IF (TABLE(I+1)- ARGUMT) 99,21,24	02650
99 IF (I .GE. N) GO TO 11	02660
100 CONTINUE	02670
21 NER = 1	02680
IOUT = I+1	02690
GO TO 700	02700
23 I = 2	02710
24 IF (NXDIR-1) 25,25,29	02720
25 ION = I + N	02730
OUTPUT = TABLE(ION)+ (ARGUMT - TABLE(I)) * (TABLE	02740
I(ION+1)- TABLE(ION))/(TABLE(I+1)-TABLE(I))	02750
GO TO 701	02760
29 IF (NOENTR - I) 31, 30, 33	02770
30 I = I-1	02780
GO TO 31	02790

32	I = 2	02800
33	IF (I .EQ. 1) I = 2	02810
31	ION = I + N	02820
	CA=(TABLE(ION)*(ARGUMENT-TABLE(I+1))*(ARGUMENT-TABLE(I+2)))	
	CB=(TABLE(I)-TABLE(I+1))	
	CD=(TABLE(I)-TABLE(I+2))	
	CE=((TABLE(ION+1)*(ARGUMENT - TABLE(I)))*(ARGUMENT-TABLE(I+2)))	
	CF=((TABLE(I+1)-TABLE(I))*(TABLE(I+1)-TABLE(I+2)))	
	OUTPUT= (CA)/(CB * CD)+(CE)/(CF) + (TABLE(ION+2)*(ARGUMENT -	
	TABLE(I)) * (ARGUMENT - TABLE(I+1)))/((TABLE(I+2)-	02880
	TABLE(I)) *(TABLE(I+2) - TABLE(I+1)))	02890
	GO TO 701	02900
700	IOUT = IOUT + N	02910
	OUTPUT = TABLE(IOUT)	02920
701	IF (NER - 2) 800, 707, 706	02930
706	IF (NER - 4) 707, 711, 714	02940
707	GO TO 800	02950
711	WRITE(6,712) NOTAB	02960
712	FORMAT(1H ,28HTOO FEW ENTRIES IN TABLE NO., I4)	02970
	GO TO 800	02980
714	WRITE (6, 715) NOTAB	02990
715	FORMAT(1H ,57HENTRIES ARE NOT IN MONOTOMIC ASCENDING ORDER IN TABL	03000
	1E NO.,I4)	03010
800	RETURN	03020
	END	03030
\$ORIGIN	D	

```

$IBFTC GTLU      DECK
      SUBROUTINE GTLUP(J,IERR,IFIRST)
C
C**  THIS SUBROUTINE DOES A TAPE LOOK UP TO OBTAIN DATA REQUIRED FOR
C    COMPUTATION CP,MU AND K
      DIMENSION DDD(90,5)
      COMMON/WRIT/IFLG1
      COMMON/DRAY/B(5,100),KD
      DIMENSION TITLT(4),D(5),DD(15,4),TITLE(4),TEND(4)
      COMMON/SPDATA/AA(90,5),XMF(90),XMW(90),SIGMA(90),OMEGA(90),TR,N
      COMMON/SPNAME/SPNAM1(90),SPNAM2(90),TEMP( 5, 90),IDATA,KK,KT
      COMMON/THRMTR/A(90,15)
      COMMON/MO/NUM(90)
      COMMON/COUNT/IKLUG
      DATA(TEND(I),I=1,4)/4*6HEND      /
      DATA(TITLE(I),I=1,4)/6HSPECIE,6HDATA F,6HOR TRA,6HNSPROP/
      IF(IFIRST.EQ.0.AND.J.EQ.3) GO TO 6
      IF(J.GT.3) GO TO 90
      IF(IFIRST.EQ.1)GO TO 10
      IF(IKLUG.GT.0)GO TO 6
      IKLUG=1
      IF(IFLG1.EQ.0)GO TO 191
      WRITE(6,3)
3     FORMAT(39HOB ARRAY CONTAINING SOME DATA FOR TRANS)
      WRITE(6,4)((B(I,JD),I=1,5),JD=1,KD)
4     FORMAT(5X,2A6,3E10.3)
191  CONTINUE
6     CONTINUE
      IFIRST = 1
      DO 9 KRD=1,KD
      DO 15 I=1,5
15    DDD(KRD,I)=B(I,KRD)
9     CONTINUE
10    CONTINUE
      KK=0
      KRD=KD
      DO 25 I=1,KRD
      DO 17 I1I=1,5

```

```

17 D(III) = DDD(1,III)
DO 20 JJ =8,1DATA
IF ( D(1).EQ.TEMP(1,JJ))GO TO 11
GO TO 20
11 IF (D(2).EQ.TEMP(2,JJ))GO TO 21
20 CONTINUE
GO TO 25
21 KK=KK+1
NUM(KK) = JJ
DO 22 L=1,5
22 A(KK,L)= D(L)
IF(,IFLG1.EQ.0)GO TO 192
WRITE(6,200)
200 FORMAT(39HOA ARRAY CONTAINING GAS DATA TO BE USED)
WRITE(6,201)KK,(A(KK,L),L=1,5)
201 FORMAT(4X,I2,2X,2A6,3F10.3)
192 CONTINUE
IF(KK+7.EQ.IDATA) GO TO 50
25 CONTINUE
50 NUMFND = 0

```

C
C
C

```

FIND AND FILL IN THERMO DATA

51 READ(13) (D(I),I=1,5),((DD(I,IJ),I=1,9),IJ=1,2)
IF(IFLG1.EQ.0)GO TO 193
WRITE(6,500)(D(I),I=1,5)
500 FORMAT(23HOD ARRAY READ FROM TAPE,5E10.3)
193 CONTINUE
DO 70 JJ=1,KK
IF(D(1).EQ.TEND(1)) GO TO 80
IF(D(1).NE.A(JJ,1)) GO TO 70
IF(D(2).EQ.A(JJ,2)) GO TO 72
70 CONTINUE
GO TO 51
72 LI =5
DO 78 NN=1,2
DO 77 LL=3,7
LI=LI+1

```

```

77 A(JJ,LI) = DD(LL,NN)
78 CONTINUE
   IF(IFLG1.EQ.0)GO TO 194
   WRITE(6,202)D(1),D(2)
202 FORMAT(5X,2A6)
   WRITE( 6,203)((A(JJ,LI)*LI=6*15))
203 FORMAT(1H0,      10E10.3)
194 CONTINUE
   NUMFND = NUMFND+1
   IF(NUMFND.EQ.KK) GO TO 90
   GO TO 51
80 IF(NUMFND.EQ.KK) GO TO 90
   WRITE(6,81)
81 FORMAT(1H0,50HNOT ALL SPECIES FOUND ON THERMO-CHEM PRODUCT TAPE )
90 N=0
   M = 1
   REWIND 13
91 DO 96 NN=1,KK
   IF(SPNAM1(M).NE.A(NN,1)) GO TO 96
   IF(SPNAM2(M).EQ.A(NN,2)) GO TO 98
   GO TO 96
98 TK = TR/1.8
   N = N + 1

```

```

C
C**  SET ARRAY CONTAINING CONSTANTS FOR GAS CALCULATIONS
C

```

```

   JJ=0
   IF(TK.GT.999.) GO TO 110
   DO 105 LL = 11,15
   JJ= JJ+1
105 AA(N,JJ) = A(NN,LL)
   GO TO 120
110 DO 115 LL = 6,10
   JJ=JJ+1
115 AA(N,JJ) = A(NN,LL)
120 NN8 = NUM(NN)

```

```

C
C**  MOLE FRACTIONS

```

```

      XMF(N) = TEMP(J,NN8)
      SPNAM1(N) = A(NN,1)
      SPNAM2(N) = A(NN,2)
C**  SPECIES MOLECULAR WEIGHT
      XMW(N) = A(NN,3)
      SIGMA(N)=A(NN,4)
      OMEGA(N)=A(NN,5)
      IF(IFLG1.EQ.0)GO TO 195
      WRITE(6,300)J,NN,NN8,TEMP(J,NN8)
300  FORMAT(10HONUM CHECK,2X,3I5,2X,E10.3)
195  CONTINUE
      GO TO 97
96  CONTINUE
97  IF (M .EQ. KK) GO TO 9999
      M = M + 1
      GO TO 91
9999 RETURN
      END

```

\$IBFTC BDATA DECK

BLOCK DATA

COMMON/DRAY/B(5,100),KD

DATA KD/45/

DATA ((B(I,J),I=1,5),J=1,19)/

16HAL	,	6H	,	26.98	,	2.655	,	2750.0	,
26HALCL	,	6H	,	62.444	,	3.578	,	972.0	,
36HALCL3	,	6H	,	133.55	,	5.127	,	472.0	,
46HALF	,	6H	,	45.98	,	3.148	,	556.0	,
56HALF3	,	6H	,	83.98	,	4.198	,	1846.0	,
66HALN	,	6H	,	40.99	,	3.369	,	2682.0	,
76HALO	,	6H	,	42.98	,	3.204	,	542.0	,
86HALS	,	6H	,	59.05	,	3.73	,	1526.0	,
96HAL2	,	6H	,	53.96	,	2.94	,	2750.0	,
A6HAR	,	6H	,	39.944	,	3.542	,	93.3	,
B6HAS1H3	,	6H	,	77.94	,	4.145	,	259.8	,
C6HB	,	6H	,	10.82	,	2.265	,	3331.0	,
D6HBBR3	,	6H	,	250.57	,	5.439	,	430.0	,
E6HBCL	,	6H	,	46.28	,	3.318	,	1026.0	,
F6HBCL2	,	6H	,	81.73	,	4.222	,	682.0	,
G6HBCL3	,	6H	,	117.19	,	5.127	,	337.7	,
\$6HCCLF3	,	6H	,	104.47	,	4.96	,	188.0	,
\$6HCF4	,	6H	,	88.01	,	4.662	,	121.0	,
\$6HCHF3	,	6H	,	70.02	,	4.33	,	240.0/	,

DATA ((B(I,J),I=1,5),J=20,38)/

H6HCH4	,	6H	,	16.04	,	3.758	,	148.6	,
I6HCO	,	6H	,	28.01	,	3.690	,	91.7	,
J6HCOS	,	6H	,	60.08	,	4.13	,	336.0	,
K6HC02	,	6H	,	44.01	,	3.941	,	195.2	,
L6HCS	,	6H	,	44.08	,	4.216	,	199.4	,
M6HCL	,	6H	,	35.457	,	3.613	,	130.8	,
N6HCL2	,	6H	,	70.91	,	4.217	,	316.0	,
O6HH	,	6H	,	1.008	,	2.708	,	37.0	,
P6HH2	,	6H	,	2.016	,	2.827	,	59.7	,
Q6HHCL	,	6H	,	36.47	,	3.339	,	344.7	,
R6HH20	,	6H	,	18.02	,	2.641	,	809.1	,
S6HHS	,	6H	,	33.07	,	3.673	,	86.4	,
T6HH2S	,	6H	,	34.08	,	3.623	,	301.1	,

U6HN2	,	6H	,	28.02	,	3.798	,	71.4	,
V6HNNH3	,	6H	,	17.03	,	2.90	,	558.3	,
W6HNO	,	6H	,	30.01	,	3.492	,	16.7	,
\$6HN2O	,	6H	,	44.02	,	3.828	,	232.4	,
*6HNE	,	6H	,	20.183	,	2.82	,	32.8	,
X6HO	,	6H	,	16.0	,	3.05	,	106.7	/
DATA((B(1,J),I=1,5),J=39,45)/									
Y6HO2	,	6H	,	39.0	,	3.467	,	106.7	,
Z6HOH	,	6H	,	17.01	,	3.147	,	79.8	,
*6HS	,	6H	,	32.066	,	3.839	,	847.0	,
\$6HSF6	,	6H	,	146.07	,	5.128	,	222.1	,
*6HSO	,	6H	,	48.07	,	3.993	,	301.0	,
*6HSO2	,	6H	,	64.07	,	4.112	,	335.4	,
*6HS2	,	6H	,	64.13	,	4.519	,	847.0/	
END									
\$*									
\$ORIGIN		B							


```

$IBFTC SOUR      DECK
      SUBROUTINE SOURCE(IDUM,ISCON)
      COMMON/WRIT/IFLG1
      DIMENSION SAVEA(16)
      DATA (SAVEA(K),K=1,16) /16*0./
      99 FORMAT(1H1)
      100 FORMAT(4X2HS2,7X7HMACH N05X5HRE N05X7H GAMMA 2X10HKNUDSEN N05X,3H
      1T05X1HT9X2HP010X1HP)
      200 FORMAT(1H0,10E11.4,2X,13)
      300 FORMAT(1H020X,32HVIBRATIONAL      ENERGY MODE FROZEN)
      400 FORMAT(1H052X,32HR0TATIONAL      ENERGY MODE FROZEN)
      500 FORMAT(1H084X,32HTRANSLATIONAL ENERGY MODE FROZEN)
      COMMON/PLUMF2/PROP(10,200),IPT
      COMMON/GASES/TAB(3,12,13),NMIX
      COMMON/GASCON/GAMA,R,T0,P0,EM,RHO,T,WM ,Q
      COMMON/GEOM/AT,RADTHT,AEOAT,ANGLP,REYNP
      COMMON/LIP/THET,PI02
      COMMON/EXCON/PEX,EMU
      COMMON/TAPE/IPROT
      EQUIVALENCE(GAMA,GAMMA)
      IPT=0
      IFREZ=0
      ITC1=0
      ITC2=0
      LPAGE=1
      POWER=.95
      CNLOCL=0.
      GMT=1.4
      ISCON=0
      PI=3.1415926536
      PI02=PI/2.
      REXT=RADTHT*SQRT(AEOAT)
      C FIRST COMPUTE LIP EXPANSION ANGLE
      RE=RADTHT*SQRT(AEOAT)
      ANGLP=ANGLP/57.29578
      P=PEX
      CALL TABLE(P,1)
      QE=Q

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      RHOEX=RHO
      WRITE(6,1022)P ,EM,GAMA,RHOEX,QE
1022 FORMAT(10HOEXIT PROP,5E10.3)
      EM1=EM
      VNU=PI02*(SQRT((GAMA+1.)/(GAMA-1.))-1.)
      VN1= SQRT((GAMA+1.)/(GAMA-1.))*ATAN(SQRT((GAMA-1.)/(GAMA+1.))
      $*(EM*EM-1.))-ATAN(SQRT(EM*EM-1.))
      DELTHT=VNU-VN1
      THET=DELTHT+ANGLP
      WRITE(6,9000)GAMA,VNU,THET
9000 FORMAT(6HOGAMA=E10.3,4HVNU=E10.3,5HTHET=E10.3)
C      TEST IF THET GT 90.
      IF(THET.GE.PI02)GO TO 5
      X=-RE/TAN(THET)
      GO TO 15
5      CONTINUE
      IF(THET.EQ.0.)GO TO 10
      THT=THET-PI02
      WRITE(6,9001)THT
9001 FORMAT(5H0THT=E10.3)
      X=RE*TAN(THT)
      GO TO 15
10     X=0.
15     CONTINUE
      WRITE(6,904)X,THET
904    FORMAT(1H027HORIGIN OF SOURCE FLOW AT X=.E10.3,5X,11HWITH THETA=.E
110.3)
      P1=P
      P2=P
      P01=TAB(1,5,1)
      T01=TAB(1,6,1)
      FUG=2.*THET
      FUG =2.*PI*(1.-COS(THET))
      PSTAR=TAB(1,5,2)
      CALL TABLE(PSTAR,1)
      RSTAR=RHO
      QSTAR=Q
      WFSTAR=RSTAR*QSTAR*AT

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```

      WRITE(6,1023)WFSTAR,RSTAR,QSTAR
1023  FORMAT(1H0,11HTHROAT PROP,3E10.3)
      WRITE(6,99)
      WRITE(6,100)
      SREF =2.*RE
      SST = .25
      IF(IPROT.EQ.1)SST=1.0
      S1=X
      S2 =0.
      AEXT = AT*AEOAT
585  S2 = S2 + SST
      SSQR = FUG*S2*S2
      IF(SSQR.LE.AEXT)GO TO 585
      S2 = S2 +SREF
      PINC=-.09*P
17  CONTINUE
      SAVEA(2)=PINC
      SAVEA(1)=1.0
      TOL=.05*WFSTAR
C    THIS SECTION COMPUTES GAS PROPERTIES UNTIL FREEZING DETECTED
C
18  CONTINUE
      IF(P2.LE.0.)GO TO 32
      GO TO 37
32  CONTINUE
      P2=P2-.95*PINC
      PINC=.1*PINC
      SAVEA(2)=PINC
37  CONTINUE
      IF(CNLOCL.GT.1./500.)GO TO 19
C    USE P TO CALL TABLE
      CALL TABLE(P2,1)
      GO TO 89
19  POP=P2/P0
      RGK=1545.*32.174/TAB(1,7,1)
      T=T0*(P2/P0)**((GAMA-1.)/GAMA)
      TOVT=T0/T
      SOS=SQRT(GAMA*RGK*T)

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      FM=SQRT((TOVT-1.)/((GAMA-1.)/2.))
      Q=EM*SOS
      RHO=P2*32.174/(T*RGK)
89  CONTINUE
      WF2=WFDOT(P2,RHO,Q,THFT,S2)
      FP=WFSTAR-WF2
      GO TO 1776
      WRITE(6,91)WF2,P2,RHO,Q,S2,GAMA,EM,T
91  FORMAT(1H0,4HWF2=E10.3,3HP2=E10.3,4HRHO=E10.3,2HQ=E10.3,3HS2=E10.3
      $,5HGAMA=E10.3,3HEM=E10.3,2HT=E10.3)
      WRITE(6,92)SAVEA(2),PINC
92  FORMAT(1H0,5HSAVE=E10.3,5HPINC=E10.3)
      WRITE(6,50)TOL
50  FORMAT(5X,4HTOL=,E10.3)
1776 CONTINUE
      CALL ITSUB(FP,P2,SAVEA,TOL,199)
      II=SAVEA(1)+.1
      NI=SAVEA(3)+.1
      GO TO (18,18,18,18,22,23),II
23  WRITE(6,600)S2 ,P2,FP
600  FORMAT(24H0ITSUB WILL NOT CONVERGE,1X,5HS2  =,E12.5,1X,2HP=,E12.5,
      $1X,3HFP=,E12.5)
      I$CON=1
      GO TO 40
22  CONTINUE
      PINC=.09*P2
4500 FORMAT(8H0CNLOCL=E10.3)
      DS=S2-S1
C    EM1 SAVED FROM PREVIOUS POINT CALCULATION
70  CONTINUE
      EM2=EM
80  CONTINUE
      GP102=(GAMA+1.)/2.
      ONOGM1=1./((GAMA-1.))
      ROUSTR=P0/(R*T0)*((GP102**(-ONOGM1)))*SQRT (2.0*GAMMA*R*T0/(GAMMA+
      $1.0))
      T02=T0
      SBAR=(S2+S1)/2.

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EMBAR=(EM1+EM2)/2.
VIS=1.36E-9*(T/1.8)**POWER
RE=ROUSTR/(VIS*SBAR**2)
DLOGT=ALOG(T02/T01*(2.+(GAMMA-1.)*EM1**2)/(2.+(GAMMA-1.)*EM2**2))
DLTDS=ABS(DLOGT/DS)
CNLOCL=(2.51*3.14*GAMMA)*((EMBAR*EMBAR)/RE)*DLTDS
IF(LPAGE.LT.55)GO TO 55
LPAGE=1
WRITE(6,99)
WRITE(6,100)
55 CONTINUE
WRITE(6,200) S2,EM2,RE,GAMMA,CNLOCL,T0,T,P0,P2
LPAGE=LPAGE+2
IPT=IPT+1
C THE FOLLOWING STATEMENTS STORE PLUME PROPERTIES IN PROP ARRAY
PROP(1,IPT)=S2/(2.*REXT)
PROP(2,IPT)=SSQR
PROP(3,IPT)=GAMA
PROP(4,IPT)=EM2
PROP(5,IPT)=P2
PROP(6,IPT)=T
PROP(7,IPT)=WM
GO TO 30
IF(CNLOCL.LT.1./500.)GO TO 30
IFREZ=1
C CALCULATION WITH VIBRATIONAL ENERGY MODE FROZEN
GAMMA=1.4
GM102=(GAMMA-1.)/2.
ONOGM1=1./(GAMMA-1.)
GOGM1=GAMMA*ONOGM1
ITC1=ITC1+1
IF(ITC1.EQ.1)T0=T*(1.+GM102*EM2*EM2)
P0=P2*(T0/T)**GOGM1
WRITE(6,300)
IF(CNLOCL.LT.1./5. )GO TO 30
C CALCULATION WITH VIBRATIONAL AND ROTATIONAL ENERGY MODE FROZEN
PINC=.07*P2
CK=CNLOCL

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      GAMMA= -.000567*CK**3 +.00868*CK**2 -.003404*CK +1.4003
      IF(CNLOCL.GE.10.)GAMMA=1.667
      ONOGM1=1./(GAMMA-1.)
      GOGM1=GAMMA*ONOGM1
      GM1O2=(GAMMA-1.)/2.
      IF(GAMMA.LE.1.667)T0=T*(1.+GM1O2*EM2*EM2)
      P0=P2*(T0/T)**GOGM1
      WRITE(6,400)
      IF(CNLOCL.LT..8)GO TO 30
C     CALCULATION WITH VIBRATIONAL,ROTATIONAL AND TRANSLATIONAL ENERGY
C     MODE FROZEN
      WRITE(6,500)
30    EM1=EM2
      T01=T02
      S1=S2
      STRECH=1.0
      DELTS=SREF
      S2=S2+DELTS
      IF(EM2.GE.100.)GO TO 40
      IF(IPT.GE. 75)GO TO 40
      GO TO 17
40    CONTINUE
      RETURN
      END

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$IBFTC WDOT1  DECK
      FUNCTION WFDOT(P0,R0,Q0,THTM,R)
      PI=3.14159265
      TWOPI=2.*PI
      PIO2=PI/2.
C
      DELTHT=THTM/20.
      THETA=0.
      AREA=0.
      DO 20 J=1,20
      I1=J
      I2=J+1
      THETA=THETA
      CR=(COS(PIO2*THETA/THTM))*7
      CV=1.
      SA=SIN(THETA)
      F1 =CR*CV*SA
      THETA=THETA+DELTHT
      CR=(COS(PIO2*THETA/THTM))*7
      CV=1.
      SA=SIN(THETA)
      F2 =CR*CV*SA
      A=.5*DELTHT*(F1+F2)
20  AREA=AREA+A
      WFDOT=TWOPI*R0*Q0*R**2*AREA
      RETURN
      END

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$IBFTC ADJUST1
  SUBROUTINE ADJUST(      NOK,KAZE)
  COMMON/CHANGE/PC11,PC21,PC22,PC31,PC32,PC33,PNW,TNW,DELM,DELMN,
$DELREY
  COMMON/AVE/EMM,EMWM,HM,HOM,GM,SLP1,SLP2
  COMMON/GASES/TAB(3,12,13),NMIX
  COMMON/CHAMB/PCHAMI,TCHAMI,PMAX,TMAX
  COMMON/PLUNMU/XC(5),PC(5),EMC(5),GMC(5),TC(5),QC(5),EMWC(5)
  COMMON/PLUMF1/PRPR(10,4),REYPLM
  COMMON/MOLWT/SA,SB,SC
  COMMON/REGION/XC11,XC12,XC13,ERRMAX,ITYPE
  COMMON/EXCON/PEX,EMU
  COMMON/GEOM/AT,RADTHT,AEOAT,ANGLP,REYNP
  LOGICAL KAZE
  PIO2=3.1415927/2.0
  NOK=0
  GO TO(300,310,320),ITYPE
300 CONTINUE
C  COMPUTE MACH NO. CHANGE FOR MOMENTUM FLUX ERROR
  P=PC(2)
  G=GMC(2)
  DEM = SQRT(ABS(DELM)/(P*G))
  IF(DELM.LT.0.) SIGN = -1.0
  IF(DELM.GT.0.) SIGN = +1.0
  DEM = SIGN*DEM
  GO TO 340
310 CONTINUE
  DEM=DELM
  GO TO 340
320 CONTINUE
C  COMPUTE MACH NO. CHANGE FOR REYNOLDS NO. ERROR
  GO2= (GMC(2)-1.)/2.
  EMF= (1.+GO2*EMC(2)*EMC(2))
  EGX=-1.*(3.*GMC(2)-1.)/(2.*(GMC(2)-1.))
  R=1545.*32.174/EMWC(2)
  D= 2.*RADTHT*SQRT(AEOAT)
  VISCOS=1.36E-09*(T/1.8)**.95
  PTL= PCHAMI*SQRT(GMC(2)/(R*TCHAMI))*D/VISCOS

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      DEM=DELRL Y/(PTL*(EMF)**EGX+EMC(2)*EMC(2)*EGX*EMF**((EGX-1.)*(GMC(2)-1.))
      $-1.))
340 CONTINUE
      KAZE=.FALSE.
C      COMPUTE MEAN PROPERTIES FOR GAS MIXTURE UNDERGOING TESTING
      CALL MEAN(DEM,P)
C      COMPUTE CHANGE FOR MOLECULAR WT.
      HOH=HM/HOM
      SH=SLP1/HM
      GM2 =(GM-1.)/2.
      ONOM =1./EMWM
      GF1= SQRT((GM-1.)/(GM+1.))
      GF2 = 1./((GM-1.))**2
      AG =P102*GF1*GF2/THET
      DELMW=(2.* DEM/EMM)/(ONOM+2.*HOH*(-SH+GM2*EMM**2*(SH-ONOM) +SLP2*
1AG) +2.*SH-2.*ONOM-2.*SLP2*AG -SLP2/GM-SLP1/HM)
      DELMW = -1.0*DELMW
      WRITE(6,5)DELMW
      5 FORMAT(33H0COMPUTED CHANGE IN MOLECULAR WT=,E10.3)
      WMN=TAB(1,7,1)+DELMW
      CHCK = TAB(2,7,1)/TAB(3,7,1)
      IF(CHCK.GT.1.) GO TO 150
      WM1 =TAB(2,7,1)
      WM2 = TAB(3,7,1)
150 WM1 = TAB(3,7,1)
      WM2 = TAB(2,7,1)
160 CONTINUE
C      TEST IF DELMW POSSIBLE
      IF(1.05*WM1.GT.WMN)GO TO 50
      IF(.95*WM2.LT.WMN)GO TO 70
      IF(NM1X.EQ.3) GO TO 20
      X1P = SA*(SB/WMN-1.)/(SB-SA)
      X2P= 1.-X1P
      WRITE(6,10)X1P,X2P
      10 FORMAT(30H0NEW MIXTURE RATIOS ARE,  X1P=,E10.3,2X,4HX2P=,E10.3)
C      BINARY MIXTURE
      PC21=X1P
      PC22=X2P

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        IF(X1P.LE.0..OR.X2P.LE.0.)GO TO 30
        TNW=TAB(1,6,1)/1.8
        PNW=TAB(1,5,1)/144.
        GO TO 200
C      IF NEW MIXTURE PHYSICALLY IMPOSSIBLE • COME HERE
30    CONTINUE
        WRITE(6,31)X1P,X2P
31    FORMAT(5X,4HX1P=,E10.3,5X,4HX2P=,E10.3,5X,19HCHANGE BINARY GASES)
        KAZE=.TRUE.
        NOK=1
        GO TO 110
20    CONTINUE
C      TERNARY MIXTURES
        FC=PC33
        FA=(1.-FC*WMN/SC-(1.-FC)*WMN/SB)/(WMN/SA-WMN/SB)
        FB= 1.-FC-FA
        X1=FA
        X2=FB
        WRITE(6,15)X1,X2,PC33
15    FORMAT( 28HNEW MIXTURE RATIOS ARE, X1=,E10.3,2X,3HX2=,E10.3,
12X,3HX3=,E10.3)
C      TEST IF PHYSICALLY POSSIBLE
        IF(X1.LT.0.)GO TO 80
        IF(X2.LT.0.)GO TO 80
        PC31=X1
        PC32=X2
        PNW=TAB(1,5,1)/144.
        TNW=TAB(1,6,1)/1.8
        GO TO 200
50    CONTINUE
        WRITE(6,51)WMN
51    FORMAT(5X,4HWMN=E10.3,38HNEW MW LT MIN.,ADJUST PRESSURE      DOWN)
        RATIO = PRPR(5,2)/PC(2)
        PNW= TAB(1,5,1)*RATIO/144.
        TNW =  TAB(1,6,1)/1.8
        IF(PNW.LT.0.)GO TO 100
        GO TO 200
70    CONTINUE

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      WRITE(6,71)WMN
71  FORMAT(5X,4HWMN=E10.3,36HNEW MW GT MAX.,ADJUST PRESSURE      UP)
      RATIO = PRPR(5,2)/PC(2)
      PNW= TAB(1,5,1)*RATIO/144.
      TNW = TAB(1,6,1)/1.8
      IF(PNW.GT.PMAX)GO TO 105
      GO TO 200
80  CONTINUE
      WRITE(6,81)X1,X2
81  FORMAT(5X,3HX1=,E10.3,5X,3HX2=,E10.3,5X,12HCHANGE GASES)
      GO TO 110
C    FLAGS SET IN THIS SECTION TO CHANGE GASES
100  CONTINUE
      WRITE(6,101)
101  FORMAT(13H0FLOW REACHED)
      KAZE=,TRUE.
      PNW=PCHAMI
      TNW=TCHAMI
      NOK=1
      GO TO 200
105  CONTINUE
      WRITE(6,106)
106  FORMAT(13H0P HI REACHED)
      KAZE=,TRUE.
      PNW=PCHAMI
      TNW=TCHAMI
      NOK=1
      GO TO 200
110  CONTINUE
      PNW=PCHAMI
      TNW=TCHAMI
      NOK=1
      KAZE=,TRUE.
200  RETURN
      END
$IBFTC WTMOL
      SUBROUTINE WTMOL(SA,SR,SC)
      COMMON/CHANGE/PC11,PC21,PC22,PC31,PC32,PC33,PNW,TNW,DELM,DELMN,

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$DELREY
COMMON/GASES/TAB(3,12,13),NMIX
DIMENSION A(20,3),B(3),C(3)
C   LOAD QUANTITIES INTO ARRAYS
C   COMPUTE MOLECULAR WTS OF INDIVIDUAL GASES
A(1,1)=PC31+PC32
A(1,2)=0.
A(1,3)=PC33
A(2,1)=0.
A(2,2)=PC31+PC32
A(2,3)=PC33
A(3,1)=PC31
A(3,2)=PC32
A(3,3)=PC33
CALL GASINV(A,3,DET)
B(1)= 1./TAB(2,7,1)
B(2)= 1./TAB(3,7,1)
B(3)= 1./TAB(1,7,1)
CALL MATMPY(A,B,C,3,3,1)
SA=1./C(1)
SB=1./C(2)
SC=1./C(3)
RETURN
END

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$IBFTC MEAL    DECK
  SUBROUTINE MEAN(DEM,P)
    COMMON/AVE/EMM,EMWM,HM,HOM,GM,SLP1,SLP2
    COMMON/ENDS/TE(2),G(2),HOE(2),HE(2),EME(2)
    COMMON/PLUNMU/XC(5),PC(5),EMC(5),GMC(5),TC(5),QC(5),EMWC(5)
    COMMON/GASES/TAB(3,12,13),NMIX
    CALL ENDPT(P)
C      C
C      COMPUTE EXTRA PROPERTIES AT PLUME PT
      UGC=1545.
      RGC=UGC/EMWC(2)
      CP= GMC(2)*RGC/(GMC(2)-1.)
      H = CP*TC(2)
      HO= H+.5*QC(2)**2
C      TEST ON DIRECTION OF CHANGE
C      AND SET END POINT VALUES
      IF(DEM.GT.0.)GO TO 100
C      NEGATIVE MACH NO. AND THUS MW CHANGE
      G1=G(1)
      HO1=HOE(1)
      H1=HE(1)
      EMW1=TAB(2,7,1)
      SLP1=(H-H1)/(EMWC(2)-EMW1)
      SLP2=(GMC(2)-G1)/(EMWC(2)-EMW1)
      EMM=(EME(1)+EMC(2))/2.0
      GM=(GMC(2)+G1)/2.0
      EMWM=(EMW1+EMWC(2))/2.0
      HM= (H1+H)/2.0
      HOM=(HO+HO1)/2.0
      GO TO 200
100 CONTINUE
      G1=G(2)
      HO1=HOE(2)
      H1=HE(2)
      EMW1= TAB(3,7,1)
      SLP1= (H-H1)/(EMWC(2)-EMW1)
      SLP2= (GMC(2)-G1)/(EMWC(2)-EMW1)
      EMM = (EME(1)+EMC(2))/2.0

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      EMWM= (EMW1+EMWC(2))/2.0
      HM=(H1+H)/2.0
      HOM=(H0+H01)/2.0
      GM= (GMC(2)+G1)/2.0
200 CONTINUE
      IWRT=1
      IF(IWRT .EQ.0)GO TO 20
      WRITE(6,5)
      5  FORMAT(25H0MEAN PROPERTIES OF GASES)
      WRITE(6,10)
      10 FORMAT(10X,3HEMM,8X,4HEMWM,8X,2HHM,9X,3HHOM,8X,2HGM)
      WRITE(6,15)EMM,EMWM,HM,HOM,GM
      15 FORMAT(6X,5E10.3)
      20 CONTINUE
      RETURN
      END

```

```

$IBFTC ENDP1   DECK
      SUBROUTINE ENDPT(P)
      COMMON/ENDS/TE(2),G(2),HOE(2),HE(2),EME(2)
      COMMON/GASCON/GAMA,R,T0,P0,EM,RHO,T,WM,Q
      COMMON/ENTH/H
C     SUBROUTINE COMPUTES GAS PROPERTIES OF INDIVIDUAL SPECIE GASES
C     AT PRESSURE SPECIFIED
      P1=P
      DO 200 J=2,3
      L=J-1
      CALL TABLE(P1,J)
      TE(L)=T
      G(L)=GAMA
      HE(L)=H
      HOE(L)=H+.5*Q**2
      EME(L)=EM
      WRITE(6,10) P
10    FORMAT(48HOEND POINT PROPERTIES OF COMPOSITE AT PRESSURE= ,E10.3)
      WRITE(6,11)
11    FORMAT(20X,3HGAS,6X,1HT,10X,1HH,10X,5HGAMMA,5X,1HM,10X,2HHO)
      WRITE(6,12)L,T,H,GAMA,EM,HOE(L)
12    FORMAT(21X,I2,2X,6E10.3)
200  CONTINUE
100  RETURN
      END

$*
$ORIGIN      B

```

```

$IBFTC CECS1  DECK
      SUBROUTINE CEC (LSD,KACE)
C
C      TO LESSEN THE NO. OF CHANGES THAT MUST BE MADE, THE THERMODYNAMIC
C      DATA FOR THE TRANSPORT PROPERTIES WILL BE READ FROM TAPE 12, THE
C      OLD NASA/LEWIS DATA TAPE.
C      THE THERMODYNAMIC DATA FOR THE CEC PORTION WILL BE READ FROM TAPE
C      8, THE NEW DATA TAPE GENERATED BY MCDERMIT.
C      TO MAKE THESE COMPATABLE THE CEC IS MODIFIED TO READ THE GAS NAME
C      UNDER A ZAG6 FORMAT.
C
C      DOUBLE PRECISION G,X
C      INTEGER DATA, OMIT, ENSERT, REAC, BLANK, THRM, END, SUB
C      LOGICAL HP, SP, TP, IDEBUG, NEWR, IONS, MOLES, FROZ, EQL, PSIA, RKT
C      LOGICAL SHOCK, MMHG, PASCAL, EV, IC, DETN, CPCVFR, CPCVEQ, SIUNIT, EUNITS
C
C      INTEGER DATDUM
C      DIMENSION DATDUM(5)
C      COMMON/TAPE/IPROT
C      COMMON/WRIT/IFLG1
C      COMMON/GASES/TAB(3,12,13),NMIX
C      COMMON/MOLFRC/ZFRAC(40),KFR
C      DIMENSION OMIT(3,3),NCD(4),ENSERT(3,3),LH(2),LVP(2),LVM(2)
C      1  ,WPSAVE(2)
C      COMMON/SUNUP/SUN(3,40,2)
C      COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
C      1  ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)
C      2  ,TOTN(13)
C      COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)
C      1  ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)
C      COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),B0P(15,2)
C      1  ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)
C      2  ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
C      3  ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
C      4  ,RHOP,RMW(15),TLN
C      COMMON /DOUBLE/ G(20,21), X(20)
C      COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM
C      1  ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEWR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ

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	2 , IONS, NC, NSERT, JSOL, JLIQ, KASE, NREAC, IC, JS1	240
	COMMON/PERF/PCP(26), VMOC(13), SPIM(13), VACI(13), SUBAR(13), SUPAR(13)	250
	1 , CPRF(13), AEAT(13), CSTR, EQL, FROZ, SS0	260
	COMMON/CASENO/LST	
	COMMON/PNT/KPT(4)	
C		270
	EQUIVALENCE (OMIT, ENLN), (ENERT, EN(1,3)), (NLM, L)	280
C		290
	DATA MIT/4HOMIT/, BLANK/1H /, PSIA/4HPSIA/, REAC/4HREAC/, IZ/2H00/	300
	1 , INPUT/4HINPU/, IE/1HE/, INSERT/4HINSE/, THRM/4HTHER/, END/3HEND/	310
	DATA LH/4HH, CA, 4HL/G /, LVP/2HV+, 1H /, LVM/2HV-, 1H /, NMLT/4HNAME/	320
	DATA (DATDUM(I), I=1,5)/6HREAC , 6HNAME , 6H , 6H ,	
	16H /	
C		330
	NAMELIST/INPT2/KASE, P, T, EQRAT, OF, FPCT, FA, TP, HP, SP, RKT	340
	1, PSIA, MMHG, SHOCK, IONS, EV, V, DETN, CPCVFR, CPCVEQ, IDEBUG	350
	2, SIUNIT, EUNITS	360
C		370
	LST=LSD	
	KASE=KACE	
	TLOW = 0.	380
	NEWR = .FALSE.	390
C		400
	1 WRITE(6,400)	410
	400 FORMAT(1H1)	420
	DATA(1)=DATDUM(1)	
	203 CONTINUE	
	204 FORMAT(5(3A4,3X))	440
	WRITE (6,2045)(DATA(I), I=1,15)	450
	2045 FORMAT(1X,5(3A4,3X))	460
	IF(DATA(1).EQ.REAC) GO TO 11	480
	IF(DATA(1).EQ.INPUT.OR.DATA(1).EQ.NMLT) GO TO 210	510
	IF(DATA(1).EQ.BLANK) GO TO 203	520
	1023 WRITE(6,1024)	530
	1024 FORMAT(40H0ERROR IN ABOVE CARD. IGNORE CONTENTS.)	540
	GO TO 203	550
	11 CONTINUE	
	NOMIT=0	

	NSERT = 0	570
	MOLES = .FALSE.	580
	CALL REACT	590
	DATA(1)=DATDUM(2)	
	WPSAVE(1) = WP(1)	600
	WPSAVE(2) = WP(2)	610
	IF(L.EQ.() WRITE(6,52)	620
	52 FORMAT(24HOERROR IN REACTANT CARDS)	630
	GO TO 203	640
C		650
C		890
C		1120
C	BEGIN NAMELIST INPT2	1130
C		1140
	210 DO 300 I=1,26	1150
	V(I) = 0.	1190
	300 CONTINUE	1200
	DO 307 I=2,26	
	P(I)=0.0	
	307 T(I)=0.0	
C	SET PRESSURE RATIO ARRAY	
	PCP(1)=1.0	
	PCP(2)=25.0	
	PCP(3)=300.0	
	PCP(4)=1000.0	
	PCP(5)=2000.0	
	PCP(6)=3000.0	
	PCP(7)=4000.0	
	PCP(8)=5000.0	
	PCP(9)=7000.0	
	PCP(10)=10000.	
	PCP(11)=30000.	
	PCP(12)=60000.	
	PCP(13)=100000.	
C		
	DO 308 I=14,26	
	308 PCP(I)=0.0	
	V1 = 0.	1210

V2 = 0.	1220
RHOP = 0.	1230
RKT=.TRUE.	
HP=.FALSE.	1260
SP=.FALSE.	1270
TP=.TRUE.	
IF(IPROT.EQ.1)TP=.FALSE.	
CPCVFR = .FALSE.	1290
CPCVEQ = .FALSE.	1300
SHOCK = .FALSE.	1310
DETN = .FALSE.	1320
EV = .FALSE.	1330
PASCAL = .FALSE.	1340
MMHG = .FALSE.	1350
PSIA=.TRUE.	
R = 1.987165	1370
RR = 4184.*R	1380
SIUNIT = .FALSE.	1390
EUNITS = .FALSE.	1400
IONS = .FALSE.	1410
IDBUG=.FALSE.	
IF(IFLG1.EQ.1)IDBUG=.TRUE.	
FA = 0.	1430
OF = 0.	1440
EQRAT= 0.	1450
FPCT= 0.	1460
EQL = .TRUE.	1470
DO 305 I=1,26	1490
IF(P(I).EQ.0.) GO TO 322	1500
NP = I	1510
IF (MMHG) P(NP) = P(NP)/760.	1520
IF (PASCAL) P(NP) = P(NP)/101325.	1530
IF(PSIA) P(NP)=P(NP)/14.696006	1540
305 CONTINUE	1550
322 IF (FA.NE.0.) OF = 1./FA	1560
IF(EQRAT.EQ.0.) GO TO 725	1570
OF= (-EQRAT*VMIN(2)-VPLS(2))/(VPLS(1)+EQRAT*VMIN(1))	1580
GO TO 727	1590

725 IF(OF.NE.0.) GO TO 727	1600
IF(FPCT.EQ.0.) GO TO 9051	1610
OF= (100.-FPCT)/FPCT	1620
GO TO 727	1630
9051 WRITE(6,724)	1640
724 FORMAT(48H0NO INPT2 VALUE GIVEN FOR OF, EQRAT, FA, OR FPCT)	1650
IF(WP(2).NE.0.) OF=WPSAVE(1)/WPSAVE(2)	1660
727 WP(1) = OF	1670
WP(2) = 1.	1680
SUM = WP(1)+WP(2)	1690
FPCT = 100.*WP(2)/SUM	1700
IF (EQRAT.NE.0.) GO TO 746	1710
V2 = (WP(1)*VMIN(1)+WP(2)*VMIN(2))/SUM	1720
V1 = (WP(1)*VPLS(1)+WP(2)*VPLS(2))/SUM	1730
IF(V2.NE.0.) EQRAT=ABS(V1/V2)	1740
746 DO 747 I=1,L	1750
B0(I) = (WP(1)*BOP(I,1)+WP(2)*BOP(I,2))/SUM	1760
747 CONTINUE	1770
IF (EQRAT.EQ.1.) EQRAT= 1.000005	1780
IF(.NOT.IONS.OR.LLMT(L).EQ.IE) GO TO 748	1790
L = L+1	1800
LLMT(L) = IE	1810
B0(L) = 0.	1820
748 HSUB0 = (WP(1)*HPP(1)+WP(2)*HPP(2))/SUM	1830
IF(NEW) CALL SEARCH	1840
DO 755 N=1,NREAC	1850
IF(NAME(N,5).NE.IZ) GO TO 755	1860
TT = RTEMP(N)	1870
CALL HCALC	1880
GO TO 760	1890
755 CONTINUE	1900
IF(IFLG1.EQ.0)GO TO 291	
760 WRITE(6,INPT2)	1910
WRITE (6,770)	1920
770 FORMAT (1H0,17X,4HFUEL ,13X,7HOXIDANT ,12X,7HMIXTURE //)	1930
780 FORMAT (1H 2A4,3E18.8/)	1940
WRITE (6,780) LH,HPP(2),HPP(1),HSUB0,LVP,VPLS(2),VPLS(1),V1,	1950
1LVM,VMIN(2),VMIN(1),V2	1960

291	CONTINUE	1970
	HSUB0 = HSUB0/R	1980
	WRITE (6,785)	1990
785	FORMAT (8H ATOMS/G)	2000
	WRITE(6,780)(LLMT(I),BLANK,BOP(I,2),BOP(I,1),B0(I),I=1,L)	2010
	RHOP = WP(2)*RHO(1)+WP(1)*RHO(2)	2020
	IF(RHOP.NE.0.) RHOP = (WP(1)+WP(2))*RHO(1)*RHO(2)/RHOP	2030
	IQ1= L+1	2040
	IF(NC.EQ.0) GO TO 790	2050
	DO 302 J=1,NS	2060
	IF(IUSE(J).EQ.0) GO TO 302	2070
	IF(IUSE(J).GT.0) IUSE(J) = -IUSE(J)	2080
	IF(NSERT.EQ.0) GO TO 302	2090
	DO 301 I=1,NSERT	2100
	IF(SUB(J,1).NE.ENSERT(1,I)) GO TO 301	2110
	IF(SUB(J,2).NE.ENSERT(2,I)) GO TO 301	2120
	IF(SUB(J,3).NE.ENSERT(3,I)) GO TO 301	2130
	ENSERT(1,I) = 0.	2140
	IQ1= IQ1+1	2150
	IUSE(J) = -IUSE(J)	2160
301	CONTINUE	2170
302	CONTINUE	2180
	NSERT = 0	2190
790	ITN= 35	2200
	IC = .FALSE.	2210
	PP = NS	2220
	NPT = 1	2230
	ENN = .1	2240
	SUMN = ENN	2250
	XI = NS - NC	2260
	XI = FNN/XI	2270
	XLN = ALOG(XI)	2280
	DO 432 J=1,NS	2290
	IF(IUSE(J).EQ.-10000) IUSE(J)=0	2300
	EN(J,1) = 0.	2310
	ENLN(J)=0.	2320
	IF (IUSE(J).NE.0) GO TO 432	2330
	EN(J,1) = XI	

ENLN(J) = XLN	2340
432 CONTINUE	2350
JSOL = 0	2360
JLIQ = 0	2370
IF(RKT) CALL ROCKET	2390
KPT(LST)=NPT	
RETURN	
END	2430

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$IBFTC CECS18  DECK
BLOCK DATA
C
    DIMENSION ATEM(3,50)
C
    COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),B0P(15,2)
    1 ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)
    2 ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
    3 ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
    4 ,RHOP,RMW(15),TLN
C
    EQUIVALENCE (ATOM(1,52),ATEM)
C
C  ATOMIC SYMBOLS, WEIGHTS, AND VALENCES
C
    DATA ATOM/
A  2HH , 1.00797, 1., 2HHE, 4.0026, 0., 2HLI, 6.939 , 1.,
B  2HBE, 9.0122 , 2., 2HB , 10.811 , 3., 2HC , 12.01115, 4.,
C  2HN , 14.0067 , 0., 2HO , 15.9994,-2., 2HF , 18.9984 , -1.,
D  2HNE, 20.183 , 0., 2HNA, 22.9898, 1., 2HMG, 24.312 , 2.,
E  2HAL, 26.9815 , 3., 2HSI, 28.086 , 4., 2HP , 30.9738 , 5.,
F  2HS , 32.064 , 4., 2HCL, 35.453 , -1., 2HAR, 39.948 , 0.,
G  2HK , 39.102 , 1., 2HCA, 40.080 , 2., 2HSC, 44.956 , 3.,
H  2HTI, 47.900 , 4., 2HV , 50.942 , 5., 2HCR, 51.996 , 3.,
I  2HMN, 54.9380 , 2., 2HFE, 55.847 , 3., 2HCO, 58.9332 , 2.,
J  2HNI, 58.710 , 2., 2HCU, 63.540 , 2., 2HZN, 65.370 , 2.,
K  2HGA, 69.720 , 3., 2HGE, 72.590 , 4., 2HAS, 74.9216 , 3.,
L  2HSE, 78.960 , 4., 2HBR, 79.909 , -1., 2HKR, 83.800 , 0.,
M  2HRB, 85.47 , 1., 2HSR, 87.620 , 2., 2HY , 88.905 , 3.,
N  2HZR, 91.220 , 4., 2HNB, 92.906 , 5., 2HMO, 95.94 , 6.,
O  2HTC, 99.000 , 7., 2HRU, 101.070 , 3., 2HRH, 102.905 , 3.,
P  2HPD, 106.400 , 2., 2HAG, 107.870 , 1., 2HCD, 112.400 , 2.,
Q  2HIN, 114.820 , 3., 2HSN, 118.690 , 4., 2HSB, 121.750 , 3. /
    DATA ATEM/
R  2HTE, 127.600 , 4., 2HI , 126.9044, -1., 2HXE, 131.300 , 0.,
S  2HCS, 132.905 , 1., 2HBA, 137.340 , 2., 2HLA, 138.910 , 3.,
T  2HCE, 140.120 , 3., 2HPR, 140.907 , 3., 2HND, 144.240 , 3.,
U  2HPM, 145.000 , 3., 2HSM, 150.350 , 3., 2HEU, 151.960 , 3.,

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V	2HGD,157.250	, 3.,	2HTB,158.924	, 3.,	2HDY,162.500	, 3.,	410
W	2HHO,164.930	, 3.,	2HER,167.260	, 3.,	2HTM,168.934	, 3.,	420
X	2HYB,173.040	, 3.,	2HLU,174.997	, 3.,	2HHF,178.490	, 4.,	430
Y	2HTA,180.948	, 5.,	2HW ,183.850	, 6.,	2HRE,186.200	, 7.,	440
Z	2HOS,190.200	, 4.,	2HIR,192.200	, 4.,	2HPT,195.090	, 4.,	450
A	2HAU,196.967	, 3.,	2HHG,200.590	, 2.,	2HTL,204.370	, 1.,	460
B	2HPB,207.190	, 2.,	2HBI,208.980	, 3.,	2HPO,210.000	, 2.,	470
C	2HAT,210.000	, 0.,	2HRN,222.000	, 0.,	2HFR,223.000	, 1.,	480
D	2HRA,226.000	, 2.,	2HAC,227.000	, 3.,	2HTH,232.038	, 4.,	490
E	2HPA,231.000	, 5.,	2HU ,238.030	, 6.,	2HNP,237.000	, 5.,	500
F	2HPU,242.000	, 4.,	2HAM,243.000	, 3.,	2HCM,247.000	, 3.,	510
G	2HBK,249.000	, 3.,	2HCF,251.000	, 3.,	2HES,254.000	, 0.,	520
H	2HFM,253.000	, 0.,	2HMV,256.000	, 0./			530
	END						740

\$*

\$IBFTC CECS13 DECK	
C	10
SUBROUTINE ROCKET	20
C	30
ROCKET PERFORMANCE	40
EITHER HPSP OR TPSP IS TRUE	50
C	60
LOGICAL HP,SP,TP,IDEBUG,NEWR ,IONS,MOLES,FROZ,EQL,LOGV,HPSP,TPSP	70
C	80
DIMENSION AA(2),BB(2),CC(2)	90
C	100
COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)	110
1 ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)	120
2,TOTN(13)	130
COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)	140
1 ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)	150
COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),B0P(15,2)	160
1 ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)	170
2 ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)	180
3 ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)	190
4 ,RHOP,RMW(15),TLN	200
COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM	210
1 ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEWR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ	220
2 ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1	230
COMMON/PERF/PCP(26),VMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13)	
1,CPRF(13),AEAT(13),CSTR,EQL,FROZ,SS0	
COMMON/CASENO/LST	
COMMON/TAPE/IPROT	
C	260
C	280
NAMelist/RKTINP/EQL,FROZ,SUBAR,SUPAR,PCP	270
ITH = 0	290
210 DO 300 I=1,26	300
SUBAR(I) = 0.	320
300 CONTINUE	330
HPSP = .TRUE.	340
HP = .TRUE.	350
TPSP = .FALSE.	360

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FOL=.FALSE.	380
FROZ = .TRUE.	
IF(IPROT.EQ.1)T(1)=0.	400
IF (T(1).EQ.0.) GO TO 302	410
TPSP = .TRUE.	420
TP = .TRUE.	430
HPSP = .FALSE.	440
GO TO 303	450
302 T(1) = 3800.	460
303 IF(PCP(1).NE.0.) GO TO 308	470
DO 305 I=1,NP	480
K = NP-I+2	490
P(K) = P(K-1)	500
305 CONTINUE	510
GO TO 311	520
308 NP= 2	530
DO 310 I=1,24	540
IF (I.GT.2) GO TO 309	550
IF ((PCP(I).EQ.0.).OR.PCP(I).EQ.1.) GO TO 310	560
309 IF (PCP(I).EQ.0.) GO TO 311	570
NP = NP + 1	580
P(NP) = P(1)/PCP(1)	590
310 CONTINUE	600
311 NSUB=0	610
NSUP = 0	620
DO 320 I=1,13	630
IF(SUBAR(I).NE.0.)NSUB=NSUB+1	640
IF(SUPAR(I).NE.0.)NSUP=NSUP+1	650
320 CONTINUE	
IF(IFLG1.EQ.0)GO TO 294	660
WRITE (6,RKTINP)	
294 CONTINUE	680
ITROT= 3	670
SSO = 0.	690
TT = T(1)	700
C	710
C SET ASSIGNED P	720
C	

DO 902 IP = 1,NP	730
PP = P(IP)	740
CALL EQLBRM	750
C	
IF(IFLG1.EQ.0)GO TO 291	
WRITE(6,5200)TT,NPT	
5200 FORMAT(11H0TT IN RKT=E10.3,2X,4HNPT=15)	
291 CONTINUE	
C	
T(NPT) = TT	760
IF(TT.NE.0.) GO TO 333	770
IF(NPT.EQ.0) GO TO 1000	780
GO TO 900	790
333 PCP(NPT) = P(1)/PP	800
IF(IP.GT.1) GO TO 195	810
C	820
C COMBUSTION CHAMBER	830
C	840
TP = .FALSE.	850
HP = .FALSE.	860
SP = .TRUE.	870
S0 = SSUM(1)	880
PCP(2)=((GAMMAS(1)+1.)/2.)*GAMMAS(1)/(GAMMAS(1)-1.)	890
P(2) = P(1)/PCP(2)	900
TT = 2.*TT/(GAMMAS(1)+1.)	910
GO TO 900	920
195 IF(IP.GT.2) GO TO 900	930
C	940
C THROAT	950
C	960
190 IF(ITH.NE.2) GO TO 191	970
ITH = 0	980
GAMMAS(2) = 0.	990
GO TO 900	1000
191 DH = HSUM(1)-HSUM(2)	1010
DHSTAR = DH-GAMMAS(2)*TT*ENN/2.	1020
IF (IDEBUG) WRITE(6,923)DHSTAR,HSUM(1),HSUM(2),PCP(2)	1030
923 FORMAT(4E25.8)	1040

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      DH = DHSTAR/DH
      IF(DH.LT.0.) DH=-DH
      IF(DH.LE.0.4E-4.OR.ITROT.EQ.0) GO TO 900
      IF(JSOL.NE.0) ITH = 1
      IF (JSOL.EQ.0.AND.ITH.EQ.1) ITH=2
      IF(ITH.EQ.0) GO TO 192
C
C     SPECIAL THROAT INTERPOLATION IF ITH = 2
C
      DLNI = .5*TT*ENN/(HSUM(1)-HSUM(2))
      AA(ITH)=.5*DLNI*(2.*DLNI+(GAMMAS(2)-1.)/GAMMAS(2))
      XX = ALOG(PCP(2))
      BB(ITH) = 1./GAMMAS(2)-DLNI-2.*XX*AA(ITH)
      CC(ITH) = ENN*TT/(PP*(HSUM(1)-HSUM(2))*5)
      CC(ITH) = ALOG(CC(ITH))-XX*(BB(ITH)+AA(ITH)*XX)
      IF(ITH.EQ.1) GO TO 192
      BB(1)=BB(1)-BB(2)
      AA(1)=AA(1)-AA(2)
      PCP(2)=(-BB(1)+(BB(1)*BB(1)-4.*AA(1)*(CC(1)-CC(2)))*5)/(2.*AA(1)
1)
      PCP(2)=EXP(PCP(2))
      GO TO 193
192 PCP(2)= PCP(2)/(1.+2.*DHSTAR/(ENN*TT *(GAMMAS(2)+1.)))
193 P(2) = P(1) / PCP(2)
      PP = P(2)
      ITROT = ITROT-1
      CALL EQLBRM
      IF(TT.EQ.0.) GO TO 1000
      GO TO 190
C
C     900 K = 0
      IF (.NOT.EQL .AND. FROZ) GO TO 990
      IF(IP.EQ.NP.OR.TT.EQ.0.) GO TO 860
      K = NPT
      IF(NPT.NE.13) GO TO 870
860 CALL RKTOUT
      IF(K.EQ.0) GO TO 990
      WRITE(6,865)

```

865	FORMAT(1H1)	1440
	NPT = 2	1450
870	NPT = NPT + 1	1460
C		1470
C	SAVE COMPOSITIONS FOR ESTIMATES OF NEXT POINT	1480
C		1490
	DO 880 I = 1,NS	1500
	EN(I,NPT) = EN(I,K)	1510
880	CONTINUE	1520
902	CONTINUE	1530
990	IF (FROZ) CALL FROZEN	1540
1000	RETURN	1550
	END	1560

```

$ORIGIN      E
$IBFTC CECS4  DECK
C                                                    10
      SUBROUTINE EQLBRM                                20
C  ROUTINE TO CALCULATE EQUILIBRIUM COMPOSITION AND PROPERTIES  30
C                                                    40
      DOUBLE PRECISION X,G                                50
      LOGICAL HP,SP,TP,IDEBUG,CONVG,IONS,MOLES,FROZ,EQL,LOGV,HPSP,TPSP  60
      LOGICAL ISING,IC                                    70
C                                                    80
      DIMENSION PROW(18)                                90
C                                                    100
      COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)  110
1    ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)  120
2    ,TOTN(13)                                           130
      COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)  140
1    ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)  150
      COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),BOP(15,2)  160
1    ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)  170
2    ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)  180
3    ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)  190
4    ,RHOP,RMW(15),TLN                                  200
      COMMON /DOUBLE/ G(20,21), X(20)                    210
      COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM  220
1    ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEW,NSUB,NSUP,ITN,CPCVFR,CPCVEQ  230
2    ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1         240
      COMMON/PERF/PCP(26),VMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13)  250
1    ,CPRF(13),AEAT(13),CSTR,EQL,FROZ,SSO              260
C                                                    270
      COMMON/CASENO/LST
      EQUIVALENCE (NLM,L)                                280
C                                                    290
      DATA ITER/4HITER/,IE/1HE/,SMALNO/1.E-6/,SMNOL/-13.815511/  300
C                                                    310
      SIZE= 18.5                                          320
      ISING = .FALSE.                                    330
      ENNL = ALOG(ENN)                                    340
      LOGV = .FALSE.                                     350

```

PPLN = ALOG(PP)	360
TLN = ALOG(TT)	370
CONVG = .FALSE.	380
ITNUMB = ITN	390
IF(IC) GO TO 966	400
IF (.NOT.IONS.OR.IE.EQ.LLMT(L)) GO TO 33	410
L = L+1	420
IQ1 = IQ1+1	430
DO 499 J = 1,NS	440
IF (A(L,J) .EQ.0.) GO TO 499	450
EN(J,NPT) = SMALNO	460
ENLN(J) = SMNOL	470
IUSF(J) = 0	480
499 CONTINUE	490
33 IF(NPT.EQ.1) WRITE(6,244)(LLMT(I),I=1,L),ITER	500
244 FORMAT (4H0PT ,14(5X,A4))	510
43 TM = ALOG(PP/ENN)	520
JS1 = 1	530
IF(.NOT.TP) CALL CPHS	540
IF(TP.AND.(CONVG.OR.ITNUMB.EQ.ITN)) CALL CPHS	550
IF(IC) GO TO 171	560
IF (.NOT.CONVG.OR.JSOL.EQ.0) GO TO 62	570
ENSOL = EN(JSOL,NPT)	580
EN(JSOL,NPT) = EN(JSOL,NPT)+EN(JLIQ,NPT)	590
IUSE(JLIQ) = -IUSE(JLIQ)	600
IQ1 = IQ1-1	610
DLVTP(NPT) = 0.	620
CPR(NPT) = 0.	630
GAMMAS(NPT) = 0.	640
LOGV = .TRUE.	650
62 CALL MATRIX	660
NUMB = ITN-ITNUMB+1	670
IF(.NOT.CONVG) GO TO 67	680
IF (LOGV.AND.JSOL.EQ.0) GO TO 63	690
DO 182 I=1,L	700
PROW(I) = G(IQ1,I)	710
182 CONTINUE	720
IF (.NOT.LOGV) GO TO 67	730

C		740
C	LOGV = .TRUE.-- SET UP MATRIX TO SOLVE FOR DLVPT	750
C		760
	63 G(IQ1,IQ2) = ENN	770
	IQ = IQ1 - 1	780
	DO 777 I = 1,IQ	790
	G(I,IQ2) = G(I,IQ1)	800
	777 CONTINUE	810
	67 IF (.NOT.IDEBUG) GO TO 72	820
	WRITE(6,772) NUMB	830
	772 FORMAT (11H01 ITERATION ,I3,6X,7HMATRIX //)	840
	DO 911 I=1,IMAT	850
	911 WRITE (6,73) (G(I,K),K=1,KMAT)	860
	72 IF(CONVG) IMAT=IMAT-1	870
	ITST = IMAT	880
	CALL MGAUSD	890
	IF(ITST.NE.IMAT) GO TO 774	900
	IF(.NOT.IDEBUG.OR.CONVG) GO TO 773	910
	WRITE (6,373)(LLMT(I),I=1,L)	920
	373 FORMAT (7H0PI ,9(A4,10X))	930
	WRITE (6,73)(X(I),I=1,IMAT)	940
	73 FORMAT (9E14.6)	950
	773 IF(.NOT.CONVG) GO TO 85	960
	IF(LOGV) GO TO 171	970
	174 SUM = 0.	980
	DO 175 J=1,L	990
	SUM = SUM+PROW(J)*X(J)	1000
	175 CONTINUE	1010
	DLVTP(NPT) = 1.+G(IQ2,IQ1)/ENN-SUM/ENN - X(IQ1)	1020
	CPR(NPT) = G(IQ2,IQ2)	1030
	DO 176 J=1,IQ1	1040
	CPR(NPT) = CPR(NPT)-G(IQ2,J)*X(J)	1050
	176 CONTINUE	1060
	LOGV = .TRUE.	1070
	GO TO 62	1080
C		1090
C	SINGULAR MATRIX	1100
C		1110

774 IF(.NOT.CONVG) GO TO 775	1120
WRITE(6,172)	1130
172 FORMAT(28H0DERIVATIVE MATRIX SINGULAR)	1140
IC = .TRUE.	1150
GO TO 171	1160
775 IF (.NOT.HP.OR.NPT.NE.1.OR.NC.EQ.0.OR.TT.GT.100.) GO TO 871	1170
WRITE(6,874)	1180
874 FORMAT(96H0LOW TEMPERATURE IMPLIES CONDENSED SPECIES SHOULD HAVE	1190
1BEEN INCLUDED ON AN INSERT CARD, RESTART)	1200
GO TO 873	1210
871 WRITE (6,74)	1220
74 FORMAT(16H0SINGULAR MATRIX)	1230
IF(IC) GO TO 873	1240
IF (ISING) GO TO 997	1250
NTZERO = 0	1260
966 DO 970 JJ = 1, NS	1270
IF(IUSE(JJ)) 970,968,967	1280
967 IF(EN(JJ,NPT).EQ.0.) GO TO 873	1290
GO TO 969	1300
968 IF(EN(JJ,NPT).NE.0.) GO TO 969	1310
EN(JJ,NPT) = SMALNO	1320
ENLN(JJ) = SMNOL	1330
GO TO 970	1340
969 NTZERO = NTZERO+1	1350
970 CONTINUE	1360
IF(.NOT.IC) GO TO 971	1370
IC = .FALSE.	1380
GO TO 43	1390
971 ISING = .TRUE.	1400
WRITE (6,776)	1410
776 FORMAT (8H0RESTART)	1420
GO TO 43	1430
997 IF(NTZERO.NE.(L-1)) GO TO 873	1440
IF(EQRAT.GT.1.00001.OR.EQRAT.LT.0.99999) GO TO 873	1450
ENN=0.	1460
NEN = 0	1470
DO 83 I=1,L	1480
JEN=0	1490

DO 80 J=1,NS	1500
IF(EN(J,NPT).EQ.0.) GO TO 80	1510
IF(A(I,J).EQ.0.) GO TO 80	1520
IF(JEN.NE.0) GO TO 83	1530
JEN = J	1540
80 CONTINUE	1550
NEN = NEN+1	1560
EN(JEN,NPT) = B0(I)/A(I,JEN)	1570
83 CONTINUE	1580
IF(NEN.LT.NTZERO) GO TO 873	1590
CONVG = .TRUE.	1600
IC = .TRUE.	1610
HSUM(NPT) = 0.	1620
DO 84 J=1,NS	1630
IF(EN(J,NPT).EQ.0.) GO TO 84	1640
ENN = EN(J,NPT)+ENN	1650
TEM = EN(J,NPT)	1660
ENLN(J) = ALOG(TEM)	1670
HSUM(NPT) = HSUM(NPT) + EN(J,NPT)*H0(J)	1680
84 CONTINUE	1690
TM = ALOG(PP/ENN)	1700
GO TO 43	1710
85 ITNUMB= ITNUMB-1	1720
C	1730
C	1740
C	1750
OBTAIN CORRECTIONS TO THE ESTIMATES	1760
KK = L + 1	1770
DLNT= X(IQ2)	1780
IF (TP) DLNT=0.	1790
DO 101 J=1,NS	1800
IF (IUSE(J)) 101,98,100	1810
98 DELN(J) = H0(J)*DLNT-H0(J)+S(J)-ENLN(J)-TM+X(IQ1)	1820
DO 99 K=1,L	1830
DELN(J)= DELN(J)+A(K,J)*X(K)	1840
99 CONTINUE	1850
GO TO 101	1860
100 DELN(J) = X(KK)	1870
KK = KK + 1	

101	CONTINUE	1880
	AMBDA= 1.	1890
	AMBDA1= 1.	1900
	SUM = X(IQ1)	1910
	IF(SUM.LT.0.) SUM=-SUM	1920
	IF(DLNT.GT.SUM) SUM=DLNT	1930
	IF(-DLNT.GT.SUM) SUM=-DLNT	1940
	DO 917 J=1,NS	1950
	IF (IUSE(J).NE.0) GO TO 917	1960
	IF((EN(J,NPT).GT.0.).AND.DELN(J).GT.SUM) SUM = DELN(J)	1970
	IF((EN(J,NPT).NE.0.) .OR. DELN(J).LE.0.) GO TO 917	1980
	SUM1 = (-9.212-ENLN(J)+ENNL)/(DELN(J)-X(IQ1))	1990
	IF(SUM1.LT.0.) SUM1=-SUM1	2000
	IF (SUM1.LT.AMBDA1) AMBDA1 = SUM1	2010
917	CONTINUE	2020
	IF(SUM.GT.2.)AMBDA=2./SUM	2030
	IF (AMBDA1.LT.AMBDA) AMBDA = AMBDA1	2040
	IF (.NOT.IDEBUG) GO TO 111	2050
	WRITE(6,923) TT,ENN,ENNL,PP,PPLN,AMBDA	2060
923	FORMAT (3H0T=,E15.8,6H ENN=,E15.8,7H ENNL=E15.8,5H PP=,E15.8,	2070
	1 7H PPLN=E15.8,8H AMBDA=E15.8)	2080
	WRITE (6,924)	2090
924	FORMAT(1H0,18X,2HNI,12X,5HLN NI,8X,9HDEL LN NI,10X,4HH/RT,9X,4HS0/	2100
	1R,12X,6H-G0/RT,9X,5H-G/RT)	2110
	DO 926 J=1,NS	2120
	FNEG1 = S(J)-H0(J)	2130
	FNEG2 = FNEG1	2140
	IF(IUSE(J).EQ.0) FNEG2=FNEG2-ENLN(J)-TM	2150
	WRITE (6,925) SUB(J,1),SUB(J,2),	2160
	1SUB(J,3),EN(J,NPT),ENLN(J),DELN(J),H0(J),S(J),FNEG1,FNEG2	2170
925	FORMAT (1X,3A4,7E15.6)	2180
926	CONTINUE	2190
	WRITE (6,110)	2200
110	FORMAT(1H0)	2210
C		2220
C	APPLY CORRECTIONS TO ESTIMATES	2230
C		2240
111	SUM = 0.	2250

DO 113 J=1,NS	2260
IF (IUSE(J)) 113,112,114	2270
112 ENLN(J)=ENLN(J)+AMBDA*DELN(J)	2280
EN(J,NPT) = 0.	2290
IF((ENLN(J)-ENNL+SIZE).LE.0.) GO TO 113	2300
EN(J,NPT) = EXP(ENLN(J))	2310
SUM = SUM+EN(J,NPT)	2320
GO TO 113	2330
114 EN(J,NPT) = EN(J,NPT) + AMBDA * DELN(J)	2340
113 CONTINUE	2350
SUMN = SUM	2360
IF (TP) GO TO 115	2370
TLN= TLN+AMBDA*DLNT	2380
TT = EXP(TLN)	2390
115 ENNL = ENNL+AMBDA*X(IQ1)	2400
ENN = EXP(ENNL)	2410
IF (LLMT(L).NE.1E) GO TO 116	2420
C	2430
C CHECK ON REMOVING IONS	2440
C	2450
DO 1116 J = 1,NS	2460
IF (A(L,J).EQ.0.) GO TO 1116	2470
IF (EN(J,NPT).GT.0.) GO TO 116	2480
1116 CONTINUE	2490
DO 1118 J=1,NS	2500
IF(A(L,J).NE.0.) IUSE(J) = -10000	2510
1118 CONTINUE	2520
L = L-1	2530
IQ1 = IQ1-1	2540
GO TO 43	2550
C	2560
C TEST FOR CONVERGENCE	2570
C	2580
116 IF (ITNUMB.EQ.0) GO TO 13	2590
IF (AMBDA.LT.1.) GO TO 43	2600
SUM = (ENN-SUMN)/ENN	2610
IF (SUM.LT.0.) SUM = -SUM	2620
IF (SUM.GT.0.5E-5) GO TO 43	2630

DO 130 J=1,NS	2640
IF (IUSE(J).LT.0) GO TO 130	2650
AA= DELN(J)/SUMN	2660
IF(AA.LT.0.) AA=-AA	2670
IF (IUSE(J).EQ.0) AA = AA*EN(J,NPT)	2680
129 IF(AA.GT.0.5E-5) GO TO 43	2690
130 CONTINUE	2700
13 CONVG= .TRUE.	2710
IF(TT .LT.TLOW.OR.TT .GT.THIGH)WRITE (6,306)TT ,NPT	2720
306 FORMAT(17H0THE TEMPERATURE=E12.4,26H IS OUT OF RANGE FOR POINT,15)	2730
IF(ITNUMB.NE.0, GO TO 160	2740
WRITE(6,973) ITN,NPT	2750
973 FORMAT(1HL,12.69H ITERATIONS DID NOT SATISFY CONVERGENCE REQUIREME	2760
1NTS FOR THE POINT 15)	2770
IF (.NOT.HP.OR.NPT.NE.1.OR.NC.EQ.0.OR.TT.GT.100.) GO TO 873	2780
WRITE(6,674)	2790
TT = T(1)	2800
RETURN	2810
C	2820
C CONVERGENCE TESTS ARE SATISFIED, TEST CONDENSED SPECIES.	2830
C	2840
160 IF(NC.EQ.0) GO TO 143	2850
SIZEF = 0.	2860
INC = 0	2870
DO 170 J = 1,NS	2880
IF (IUSE(J).EQ.0 .OR. IUSE(J).EQ.-10000) GO TO 170	2890
INC = INC + 1	2900
IF(IDEBUG) WRITE(6,144)(SUB(J,1),1=1,3),TEMP(INC,1),TEMP(INC,2),	2910
1 IUSE(J),EN(J,NPT)	2920
144 FORMAT (1H0,3A4,2F10.3,3X,5HIUSE=,14,E15.7)	2930
IF (EN(J,NPT)) 146,148,169	2940
146 IF (J.NE.JSOL .AND. J .NE.JLIQ) GO TO 147	2950
JSOL = 0	2960
JLIQ = 0	2970
147 IQ1 = IQ1 - 1	2980
EN(J,NPT) = 0.	2990
GO TO 166	3000
148 KG = 1	3010

	IF(IUSE(J).EQ.-IUSE(J+1)) GO TO 154	3020
151	IF(J.EQ.1.OR.IUSE(J).NE.-IUSE(J-1)) GO TO 153	3030
	KG = -1	3040
154	JKG = J + KG	3050
	IF (EN(JKG,NPT).LT.0.) GO TO 170	3060
	TMELT = TEMP(INC,1)	3070
	IMP = INC + KG	3080
	IF(TMELT.EQ.TEMP(IMP,2)) GO TO 158	3090
	TMELT = TEMP(INC,2)	3100
	IF (TMELT.EQ.TEMP(IMP,1)) GO TO 157	3110
	WRITE (6,156)	3120
156	FORMAT (50H03 PHASES OF A CONDENSED SPECIES ARE OUT OF ORDER	3130
C		3140
C	JTH SPECIES A SOLID (EN=0), (J+KG)TH SPECIES A LIQUID (EN IS +)	3150
C		3160
157	IF(TT.GT.TMELT) GO TO 169	3170
	IF (TP.AND.TT.EQ.TMELT) GO TO 169	3180
	IF (TP) GO TO 1165	3190
	IF (TT.LE.TMELT-150.) GO TO 1165	3200
	JSOL = J	3210
	JLIQ = JKG	3220
	GO TO 159	3230
C		3240
C	JTH SPECIES A LIQUID(EN=0), (J+KG)TH SPECIES A SOLID (EN IS +)	3250
C		3260
158	IF (TT.LT.TMELT) GO TO 169	3270
	IF (TP.AND.TT.EQ.TMELT) GO TO 169	3280
	IF (TP) GO TO 1165	3290
	IF (TT.GE.TMELT+150.) GO TO 1165	3300
	JSOL = JKG	3310
	JLIQ = J	3320
159	TLN = ALOG (TMELT)	3330
	TT = TMELT	3340
	EN(JKG,NPT) = .5 * EN(JKG,NPT)	3350
	EN(J,NPT) = EN(JKG,NPT)	3360
	GO TO 165	3370
C		3380
C	WRONG PHASE INCLUDED FOR T INTERVAL. SWITCH EN	3390

C		3400
1165	EN(J,NPT) = EN (J,KG, NPT)	3410
	IUSE(J) = -IUSE(J)	3420
	IUSE (J,KG) = -IUSE(J,KG)	3430
	EN(J,KG,NPT)= 0.	3440
	GO TO 40	3450
153	IF (TT.LT.TEMP(INC,1) .AND.TEMP(INC,1).NE.TLOW) GO TO 169	3460
	IF (TT.GT.TEMP(INC,2)) GO TO 169	3470
C		3480
C		3490
	SUM = 0.	3500
	DO 167 I = 1,L	3510
	SUM = SUM + A(I,J)*X(I)	3520
167	CONTINUE	3530
	DELF = H0(J)-S(J)-SUM	3540
	IF(IDEBUG) WRITE(6,168)DELF,SIZEF	3550
168	FORMAT (17H GO-SUM(AIJ*PI) =E15.7,10X,18HPREVIOUS DELTA G =,E15.7)	3560
	IF(DELF.GE.SIZEF .OR. DELF.GE.0.) GO TO 169	3570
	SIZEF = DELF	3580
	JDELF = J	3590
169	IF(INC.EQ.NC) GO TO 1160	3600
170	CONTINUE	3610
1160	IF (SIZEF.EQ.0.) GO TO 143	3620
	J = JDELF	3630
165	IQ1 = IQ1 + 1	3640
166	IUSE(J) = - IUSE(J)	3650
40	CONVG = .FALSE.	3660
143	TN = NUMB	3670
	WRITE(6,771)NPT,(X(IL),IL=1,L),TN	3680
771	FORMAT (I3,14F9.3)	3690
	ITNUMB = ITN	3700
	GO TO 43	3710
C		3720
C	CALCULATE EQUILIBRIUM PROPERTIES	3730
C		3740
171	SSUM(NPT) = 0.	3750
	IF(JLIQ.NE.0) EN(JSOL,NPT)=ENSOL	3760
	DO 183 J=1,NS	3770

IF (NPT.EQ.1) SS0 = SS0 + EN(J,1)*S(J)	3780
WRITE(6,7689)SS0,EN(J,1),S(J)	
7689 FORMAT(1H0,4HSS0=E10.3,2X,3HEN=E10.3,2X,2HS=E10.3)	
SS = S(J)	3790
IF(IUSE(J).EQ.0) SS=SS-ENLN(J)-TM	3800
SSUM(NPT) = SSUM(NPT)+SS*EN(J,NPT)	3810
183 CONTINUE	3820
IF(.NOT.IC) GO TO 178	3830
DLVPT(NPT) = -1.	3840
DLVTP(NPT) = 1.	3850
CPR(NPT) = CPSUM	3860
GO TO 199	3870
178 SUM = 0.	3880
DO 179 J = 1,L	3890
SUM = SUM + PROW(J)*X(J)	3900
179 CONTINUE	3910
DLVPT(NPT) = -2.+SUM/ENN+ X(IQ1)	3920
184 IF(JLIQ.EQ.0) GO TO 199	3930
IUSE(JLIQ) = -IUSE(JLIQ)	3940
HSUM(NPT) = HSUM(NPT)+EN(JLIQ,NPT)*(H0(JLIQ)-H0(JSOL))	3950
IQ1 = IQ1+1	3960
GAMMAS(NPT) = -1./DLVPT(NPT)	3970
GO TO 186	3980
199 GAMMAS(NPT) = -1./((DLVPT(NPT)+(DLVTP(NPT)**2)*ENN/CPR(NPT))	3990
186 TTT(NPT) = TT	4000
PPP(NPT) = PP	4010
CPRF(NPT) = CPSUM	4020
HSUM(NPT) = HSUM(NPT)*TT	4030
WM(NPT) = 1./ENN	4040
200 IF (.NOT.IDEBUG) RETURN	4050
WRITE(6,201) NPT,PCP(NPT),PP,TT,HSUM(NPT),SSUM(NPT),WM(NPT),CPR(NP	4060
IT),DLVPT(NPT),DLVTP(NPT),GAMMAS(NPT)	4070
201 FORMAT (7H0POINT=13.3X,4HPCP=E13.6,3X,2HP=E13.6,3X,2HT=E13.6,3X,4H	4080
1H/R=E13.6,3X,4HS/R=E13.6//3X,3HMW=E13.6,3X,5HCP/R=E13.6,3X,6HDLVPT	4090
2=E13.6,3X,6HDLVTP=E13.6,3X,9HGAMMA(S)=E13.6)	4100
GO TO 1000	4110
C	4120
C ERROR, SET TT=0	4130

C
873 TT=0.
NPT = NPT-1
1000 RETURN
END

4140
4150
4160
4170
4180

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$IBFTC CECS17  DECK
C
      SUBROUTINE FROZEN
C
C      (FROZEN COMPOSITION EXPANSION ONLY)
C
C      LOGICAL EQL,FROZ,CONVG
C
      COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
1  ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)
2 ,TOTN(13)
      COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),HO(150)
1  ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)
      COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),B0P(15,2)
1  ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)
2  ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
3  ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4  ,RHOP,RMW(15),TLN
      COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM
1  ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEW,NSUB,NSUP,ITN,CPCVFR,CPCVEQ
2  ,IONS,NC,INSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1
      COMMON/PERF/PCP(26),VMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13)
1  ,CPRF(13),AEAT(13),CSTR,EQL,FROZ,SS0
      COMMON/OUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4)
1  ,FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMTI9,FA1,FA2
2  ,FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,F0,FRI(2)
      ITR0T = 3
      EQL = .FALSE.
      NPT = 2
      TT = TTT(1)
      TLN=ALOG(TT)
      WRITE(6,9009)TT,SS0,CPRF(1),PCP(1),WM(1),TLN,GAMMAS(1)
9009  FORMAT(1H0,3HTT=E10.3,4HSS0=E10.3,5HCPRF=E10.3,4HPCP=E10.3,
13HWM=E10.3,4HTLN=E10.3,7HGAMMAS=E10.3)
      GAMMAS(1) = CPRF(1)/(CPRF(1)-1./WM(1))
      CPR(1) = CPRF(1)
      PCP(2) = ((GAMMAS(1)+1.)/2.)*((GAMMAS(1)/(GAMMAS(1)-1.))
      DATA(1) = 2./(GAMMAS(1) + 1.)

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	TLN = TLN + ALOG(DATA(1))	350
	DO 902 IP=2,NP	360
	IF(NPT.EQ.2) GO TO 45	370
	PCP(NPT) = P(1)/P(IP)	380
45	CONVG = .FALSE.	390
	PCPLN= ALOG(PCP(NPT))	400
	S0 = SS0 -PCPLN/WM(1)	410
	SUMH = 0.	420
51	TT=EXP(TLN)	430
	SUMS=0.	440
	JS1 = 1	450
	NNN = NPT	460
	NPT = 1	470
	CALL CPHS	480
	NPT = NNN	490
	DO 60 J=1,NS	500
	IF(EN(J,1).EQ.0.) GO TO 60	510
	SUMS = SUMS + S(J)*EN(J,1)	520
	IF(CONVG) SUMH=SUMH+H0(J)*EN(J,1)	530
60	CONTINUE	540
	IF (CONVG) GO TO 81	550
	DLNT=(SUMS-S0)/CPSUM	560
	TLN=TLN-DLNT	570
	IF(DLNT.LT.0.) DLNT=-DLNT	580
	IF(DLNT.LT.0.5E-4) CONVG=.TRUE.	590
	GO TO 51	600
81	TTT(NPT)= TT	610
	SSUM(NPT)= SSUM(1)	620
	HSUM(NPT)= TT*SUMH	630
	GAMMAS(NPT)= CPSUM/(CPSUM-1./WM(1))	640
	IF(IP.GT.2) GO TO 90	650
C		660
C	THROAT CALCULATIONS	670
C		680
	DH = HSUM(1)-HSUM(2)	690
	DHSTAR = DH-(GAMMAS(2)*TT/(2.*WM(1)))	700
	DH = DHSTAR/DH	710
	IF(DH.LT.0.) DH=-DH	720

IF(DH.LE.0.4E-4.OR.ITROT.EQ.0) GO TO 90	730
PCP(2) = PCP(2)/(1.+2.*DHSTAR*WM(1)/(TT*(GAMMAS(2)+1.)))	740
P(2) = P(1)/PCP(2)	750
ITROT = ITROT-1	760
GO TO 45	770
90 WM(NPT)= WM(1)	780
PPP(NPT) = P(IP)	790
CPR(NPT)= CPSUM	800
K = 0	810
IF (TT.LT.(TLOW-150.))GO TO 903	820
IF(NC.EQ.0) GO TO 700	830
INC =0	840
DO 901 I=1,NS	850
IF(IUSE(I).EQ.0.OR.IUSE(I).EQ.-10000) GO TO 901	860
INC = INC+1	870
IF(EN(I,1).EQ.0.) GO TO 901	880
IF (TT.LT.(TEMP(INC,1)-50.).OR.TT.GT.(TEMP(INC,2)+50.))GO TO 903	890
901 CONTINUE	900
700 IF (IP.EQ.NP) GO TO 863	910
K = NPT	920
IF (NPT.NE.13) GO TO 870	930
GO TO 863	940
903 NPT = NPT - 1	950
863 CALL RKTOUT	960
GO TO 1000	
865 IF (K.EQ.0) GO TO 1000	980
NPT = 2	990
870 NPT = NPT + 1	1000
902 CONTINUE	1010
1000 RETURN	1020
END	1030

\$IBFTC CECS9	DECK	
C		10
	SUBROUTINE HCALC	20
C		30
C	CALCULATE ENTHALPY FOR PROPELLANT USING COEFFICIENTS	40
C		50
	LOGICAL MOLES	60
	DIMENSION NUM(15,5),WS(2)	70
C		80
	COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)	90
1	,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)	100
	COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),B0P(15,2)	110
1	,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)	120
2	,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)	130
3	,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)	140
4	,RHOP,RMW(15),TLN	150
	COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM	160
1	,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEW,NSUB,NSUP,ITN,CPCVFR,CPCVEQ	170
2	,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1	180
C		190
	EQUIVALENCE (ANUM,NUM),(L,NLM),(J,JS1)	200
C		210
	DATA AG/1HG/,IZERO/2H00/,OX/1HO/	220
C		230
C	IS TT IN RANGE	240
C		250
	IF(TT.LT.(TLOW-100.).OR.TT.GT.(THIGH+1000.))GO TO 75	260
	WS(1) = 0.	270
	WS(2) = 0.	280
	HPP(1)=0.	290
	HPP(2)=0.	300
	AC(1)=0.	310
	AC(2)=0.	320
	DO 900 N=1,NREAC	330
	K=2	340
	IF(FOX(N).EQ.OX)K=1	350
	PCWT=PECWT(N)	360
	IF(MOLES)PCWT=PCWT*RMW(N)	370

WS(K) = WS(K) + PCWT	380
IF(NAME(N,5).NE.IZERO)GO TO 500	390
J = NUM(N,5)	400
IF (J.NE.0) GO TO 90	410
DO 10 J=1,L	420
DATA(J)=0.	430
10 CONTINUE	440
DO 40 I=1,4	450
IF(ANUM(N,I).EQ.0.)GO TO 50	460
DO 20 J=1,L	470
IF(LLMT(J).EQ.NAME(N,I)) GO TO 30	480
20 CONTINUE	490
30 DATA(J)=ANUM(N,I)	500
40 CONTINUE	510
50 IS=0	520
DO 70 J=1,NS	530
IF(IUSE(J).EQ.0)GO TO 55	540
IS = IS+1	550
IF(FAZ(N).EQ.AG)GO TO 70	560
IF(TT.GT.TEMP(IS,2).AND.TEMP(IS,2).NE.THIGH) GO TO 70	570
IF(TT.LT.TEMP(IS,1).AND.TEMP(IS,1).NE.TLOW) GO TO 70	580
GO TO 56	590
55 IF(FAZ(N).NE.AG) GO TO 70	600
56 DO 60 I=1,L	610
IF(A(I,J).NE.DATA(I)) GO TO 70	620
60 CONTINUE	630
NUM(N,5) = J	640
GO TO 90	650
70 CONTINUE	660
DELN(J)= EN(J,NPT)	700
EN(J,NPT) = 1.	710
CALL CPHS	720
EN(J,NPT) = DELN(J)	730
NS = NSS	740
IF (H0(J).GT.-.01 .AND. H0(J).LT..01) H0(J) = 0.	750
RTEMP(N) = TT	760
ENTH(N) = H0(J)*R*TT	770
AC(K)=AC(K)+CPSUM*PCWT/RMW(N)	780

500	HPP(K)=Hf P(K)+ENTH(N)*PCWT/RMW(N)	790
900	CONTINUE	800
	DO 950 K=1,2	810
	IF(WS(K).EQ.0.)GO TO 950	820
	HPP(K)=HPP(K)/WS(K)	830
	AC(K)=AC(K)/WS(K)	840
	GO TO 80	670
90	NSS = NS	680
	NS = J	690
950	CONTINUE	850
	HSUBO = (WP(1)*HPP(1)+WP(2)*HPP(2))/(WP(1)+WP(2))	860
	GO TO 1000	870
75	WRITE(6,76)	880
76	FORMAT(50H0REACTANT TEMPERATURE OUT OF RANGE OF THERMO DATA)	890
80	WRITE(6,85) N	900
85	FORMAT(1H0,I2,34H TH REACTANT IS NOT IN THERMO DATA)	910
1000	RETURN	920
	END	930

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$IBFTC CECS14  DECK
C
C  ROCKET PERFORMANCE PERAMETERS
C
C      SUBROUTINE RKTOUT
C
C      LOGICAL EQL,FROZ ,TP,HP,SP,HPSP,TPSP,SHOCK
C
C      DIMENSION NV(13),Z(10,4),RHOISP(13)
C
C      COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
1  ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)
2  ,TOTN(13)
C      COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)
1  ,DELN(150),A(15,150),SUB(150,3),9USE(150),TEMP(50,2)
C      COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),B0P(15,2)
1  ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)
2  ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
3  ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4  ,RHOP,RMW(15),TLN
C      COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM
1  ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEWNR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ
2  ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1
C      COMMON/PERF/PCP(26),VMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13)
1  ,CPRF(13),AEAT(13),CSTR,EQL,FROZ,SS0
C      COMMON/OUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4)
1  ,FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMT19,FA1,FA2
2  ,FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,F0,FR1(2)
C      COMMON/GASES/TAB(3,12,13),NMIX
C      COMMON/SUNUP/SUN(3,40,2)
C      COMMON/CASENO/LST
C      COMMON/TAPE/IPROT
C      COMMON/MOLFRC/ZFRAC(40),KF
C
C      EQUIVALENCE (V,NV),(Z,H0)
C
C      DATA EXIT/4HEXIT/
C

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      LSP=LST
      IF(EQL) WRITE (6,37)
37  FORMAT(1H1/24X,84HTHEORETICAL ROCKET PERFORMANCE ASSUMING EQUILIBR
      IUM COMPOSITION DURING EXPANSION          //)
      IF (.NOT.EQL) WRITE (6,38)
38  FORMAT(1H1,26X,78HTHEORETICAL ROCKET PERFORMANCE ASSUMING FROZEN C
      OMPOSITION DURING EXPANSION          //)
      IF (TPSP) WRITE (6,737)
737 FORMAT (52X,28HAT AN ASSIGNED TEMPERATURE
      V(1) = PPP(1)*14.696006
      WRITE (6,40) V(1)
40  FORMAT(5H PC = ,F8.1,5H PSIA)
      CALL OUT1
      NEX = NPT - 2
      DO 862 I = 1,NEX
862  V(I) = EXIT
      WRITE(6,48) (V(I),I=1,NEX)
48  FORMAT(1H0,16X,16HCHAMBER   THROAT   ,11(5X,A4))
C
C      PRESSURE RATIOS
C
      DO 45 I=1,NPT
      K= 2*I+3
      FMT(K)= F3
      IF (PCP(I).GE.1000.) FMT(K)=F2
      IF (PCP(I).GE.10000.)FMT(K)=F1
      IF (PCP(I).GE.1000000.)FMT(K) = F0
45  CONTINUE
      WRITE (6,FMT) FR1,FB,FB,FB,(PCP(J),J=1,NPT)
      CALL OUT2
C
      AGV = 9.80665
      DO 202 K=2,NPT
      SPIM(K) = (2.*RR*(HSUM(1)-HSUM(K)))*.5/AGV
C
C      AW (A/W) IN UNITS OF SEC/ATM
C
      AW = RR*TTT(K)/(PPP(K)*
                                WM(K)*SPIM(K)*AGV**2)

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IF(K.NE.2)GO TO 200	700
AWT=AW	710
CSTR=32.174*P(1)*AWT	720
200 AEAT(K)=AW/AWT	730
VACI(K)=SPIM(K)+PPP(K)*AW	740
IF (SONVEL(K).NE.0.) VMOC(K)=SPIM(K)*AGV/SONVEL(K)	750
NV(K)= CSTR + .5	760
202 CONTINUE	770
C	780
C MACH NUMBER	790
C	800
VMOC(1)=0.	810
IF(GAMMAS(2).EQ.0.) VMOC(2)=0.	820
FMT(7) = F3	830
WRITE(6,FMT)(FN(1),I=1,4),(VMOC(J),J=1,NPT)	840
DO 520 JAB=1,NPT	
520 TAB(LSP,4,JAB)=VMOC(JAB)	
WRITE (6,208)	850
208 FORMAT (1H)	860
C	870
C C*	880
C	890
FMT(4) = FMT9X	900
FMT(5) = FMT13	910
FMT(6) = FMT19	920
FMT(7) = FB	930
WRITE(6,FMT)(FR(1),I=1,4),(NV(J),J=2,NPT)	940
C	950
C CF - THRUST COEFICIENT	960
C	970
FMT(6) = FMT(8)	980
FMT(7) = F3	990
DO 212 I=2,NPT	1000
212 V(I)=32.174*SPIM(I)/CSTR	1010
WRITE(6,FMT)FC1,FB,FB,FB,(V(J),J=2,NPT)	1020
C	1030
C AREA RATIO	1040
C	1050

FMT(5) = FB	1060
DO 214 I = 2,NPT	1070
K = 2*I+3	1080
FMT(K) = F4	1090
IF (AEAT(I).GE.1.) FMT(K) = F3	1100
IF (AEAT(I).GE.10.) FMT(K) = F2	1110
IF (AEAT(I).GE.100.) FMT(K) = F1	1120
214 CONTINUE	1130
WRITE(6,FMT)FA1,FA2,FB,FB,(AEAT(J),J=2,NPT)	1140
DO 530 JAB=1,NPT	
530 TAB(LSP,2,JAB)=AEAT(JAB)	
C	1150
C VACUUM IMPULSE	1160
C	1170
FMT(5) = FMT13	1180
FMT(7) = F1	1190
WRITE(6,FMT)(FA(I),I=1,4),(VACI(J),J=2,NPT)	1200
C	1210
C SPECIFIC IMPULSE	1220
C	1230
WRITE(6,FMT)(FI(I),I=1,4),(SPIM(J),J=2,NPT)	1240
DO 308 J = 2,NPT	1250
308 RHOISP(J) = SPIM(J) * RHOP	1260
WRITE (6,FMT) (FRI(I),I=1,2),FB,FB,(RHOISP(J),J=2,NPT)	1270
WRITE (6,208)	1280
FMT(4) = FB	1290
FMT(5) = FMT13	1300
FMT(7) = F5	1310
IF(EQL) GO TO 312	1320
WRITE(6,310)	1330
310 FORMAT(15H0MOLE FRACTIONS //)	1340
C	1350
C MOLE FRACTIONS - FROZEN	1360
C	1370
LINE = 0	1380
KF=0	
DO 430 K =1,NS	1390
V(LINE+1) = EN(K,1)/TOTN(1)	1400

IF (V(LINE+1).LT.(5.E-6)) GO TO 424	1410
LINE = LINE+1	1420
Z(LINE,1) = SUB(K,1)	1430
Z(LINE,2) = SUB(K,2)	1440
Z(LINE,3) = SUB(K,3)	1450
Z(LINE,4) = V(LINE)	1460
IF(V(LINE).LE..05) GO TO 561	
KF=KF+1	
ZFRAC(KF)=V(LINE)	
DO 560 JAB=1,NPT	
560 TAB(LSP,KF+8,JAB)=V(LINE)	
SUN(LSP,KF,1)=SUB(K,1)	
SUN(LSP,KF,2)=SUB(K,2)	
WRITE(6,562)KF,SUN(LSP,KF,1),SUN(LSP,KF,2),SUB(K,1),SUB(K,2),	
\$ZFRAC(KF),V(LINE)	
562 FORMAT(1H0,15,5X,2A6,5X,2A6,5X,E10.3,5X,E10.3)	
561 CONTINUE	
424 IF (LINE.NE.4.AND.K.NE.NS) GO TO 430	1470
IF (LINE.EQ.0) GO TO 312	1480
WRITE (6,426) (Z(LN,1),Z(LN,2),Z(LN,3),Z(LN,4),LN=1,LINE)	1490
426 FORMAT (1H,4(3A4,F9.5,7X))	1500
LINE = 0	1510
430 CONTINUE	1520
312 CALL OUT3	1530
1000 RETURN	1540
END	1550

\$IBFTC	CECS19	DECK	
	BLOCK DATA		
	COMMON/OUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4)		100
1	,FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMT19,FA1,FA2		110
2	,FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,F0,FR1(2)		120
C			540
C	INFORMATION USED IN VARIABLE OUTPUT FORMAT		550
C			560
	DATA FMT/3H(1H,4H,3A4,4H,A2,,3HF9,,1H ,3HF9,,1H ,3HF9,,1H ,3HF9,,1		570
	1H ,3HF9,,1H ,3HF9,,1H ,3HF9,,1H ,3HF9,,1H ,3HF9,,1H ,3HF9,,1H ,3HF		580
	29,,1H ,3HF9,,1H ,3HF9,,1H ,1H)/, FB,F0,F1,F2,F3,F4,F5/1H ,2H0,,2H		590
	31,,2H2,,2H3,,2H4,,2H5/,FMT13/2H13/,FMT9X/3H9X/,FMT19/3H19,/		600
	DATA FP/4HP, A,4HTM ,2H ,1H /		610
	1,FT/4HT, D,4HEG K,4H ,2H /,FH/4HH, C,4HAL/G,2H ,1H /		620
	2,FS/4HS, C,4HAL/((,4HG)(K,2H) /,FM/4HM, M,4HOL W,2HT ,1H /		630
	3,FV/4H(DLV,4H/DLP,4H)T ,2H /,FD/4H(DLV,4H/DLT,2H)P,1H /		640
	4,FC/4HCP, ,4HCAL/,4H(G)(,2HK)/,FG/4HGAMM,4HA (S,2H) ,1H /		650
	5,FL/4HSON ,4HVEL,,4HM/SE,2HC /		660
C			670
C	INFORMATION USED IN PERFORMANCE OUTPUT		680
C			690
	DATA FR1/4HPC/P/, FC1/2HCF/, FN/4HMACH,4H NUM,4HBER ,1H /		700
	1,FR/4HCSTA,4HR, F,4HT/SE,2HC /,FI/4HI, L,4HB-SE,4HC/LB,1H /		710
	2,FA/4HIVAC,4H,LB-,4HSEC/,2HLB /,FA1/4HAE/A/,FA2/1HT/		720
	3,FRI/4HRHOI,2HSP/		730
	END		

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$ORIGIN      F
$*
$IBFTC CECS8  DECK
      SUBROUTINE OUT1
C
      DOUBLE PRECISION G,X
      LOGICAL EQL,FROZ ,TP,HP,SP,HPSP,TPSP,MOLES
C
      DIMENSION NV(13),Z(10,3),HEAD(15),YX(5),YN(5)
C
      COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
1  ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)
2  ,TOTN(13)
      COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)
1  ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)
      COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),B0(15),BOP(15,2)
1  ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)
2  ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
3  ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4  ,RHOP,RMW(15),TLN
      COMMON /DOUBLE/ G(20,21), X(20)
      COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM
1  ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEW,NSUB,NSUP,ITN,CPCVFR,CPCVEQ
2  ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1
      COMMON/PERF/PCP(26),VMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13)
1  ,CPRF(13),AEAT(13),CSTR,EQL,FROZ,SS0
      COMMON/OUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4)
1  ,FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMT19,FA1,FA2
2  ,FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,F0,FR1(2)
C
      EQUIVALENCE (V,NV),(Z,H0),(IB,FR)
      COMMON/GASES/TAB(3,12,13),NMIX
      COMMON/CASENO/LST
C
      HEAD=(1H ,2A4,5  (A2,F8.5,3X),5  X,F7.5,F13.3,4X,A1,F10.2,F9.4)
C
      DATA HEAD/4H(1H ,4H,2A4,2H,5,4H(A2,,4HF8.5 ,4H,3X),2H,5 ,2HX,
1  ,4HF7.5 ,4H,F13 ,4H,3,4 ,4HX,A1 ,4H,F10 ,4H,2,F ,4H9.4)/

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DATA FUEL/4HFUEL/,OXID/4HOXID/,ANT/3HANT/,OX/1HO/,IZ/2HOO/      340
1      ,YN/2H,1, 2H,2, 2H,3, 2H,4, 2H,5 /,F75/4HF7.5/           350
2      ,YX/3H,57,3H,44,3H,31,3H,18,2H,5 /,F73/4HF7.3/           360
LSP=LST                                                                370
C                                                                    380
  IF(KASE.NE.0) WRITE (6,3) KASE                                     390
3  FORMAT (9H CASE NO. ,I5)                                         400
  IF(.NOT.MOLES) WRITE(6,5)                                         410
5  FORMAT (77X,46HWT FRACTION ENTHALPY STATE TEMP DENSITY/      420
1  10X,16HCHEMICAL FORMULA,51X,21H(SEE NOTE) CAL/MOL,10X,5HDEG K, 430
2  4X,4HG/CC )
  IF(MOLES) WRITE(6,6)                                             440
6  FORMAT (79X,5HMOLES,7X, 33HENTHALPY STATE TEMP DENSITY/      450
1  10X,16HCHEMICAL FORMULA,66X,7HCAL/MOL,10X,13HDEG K G/CC )    460
  DO 15 N=1,NREAC                                                  470
  IF(FOX(N).EQ.FOX(N-1))GO TO 11                                   480
  IF(FOX(N).NE.OX)GO TO 10                                         490
  HD1 = OXID                                                        500
  HD2 = ANT                                                         510
  GO TO 11                                                          520
10 HD1 = FUEL                                                       530
  HD2 = FB                                                          540
11 DO 13 J=1,5                                                      550
  IF(NAME(N,J).EQ.IZ.OR.NAME(N,J).EQ.IB) GO TO 14                560
13 CONTINUE                                                         570
  J=6                                                                580
14 J=J-1                                                            590
  HEAD(3)=YN(J)                                                     600
  HEAD(7)=YX(J)                                                     610
  HEAD(9) = F75                                                      620
  IF(PECWT(N).GE.10.) HEAD(9)=F73                                   630
  WRITE(6,HEAD)HD1,HD2,(NAME(N,JJ),ANUM(N,JJ),JJ=1,J),PECWT(N),ENTH( 640
1N), FAZ(N),RTEMP(N),DENS(N)                                       650
15 CONTINUE                                                         660
  FPC = 100./(1.+WP(1))                                             670
  WRITE(6,20) WP(1),FPC,EQRAT,RHOP                                  680
20 FORMAT (1HO,15X, 4HO/F=, F8.4,4X,13HPERCENT FUEL=,F8.4,4X,    690
1  19HEQUIVALENCE RATIO=,F7.4,4X,8HDENSITY=,F8.4//)              700

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C	AGV = 9.80665	710
	DO 25 I = 1,NPT	720
	TOTN(I) = 0	730
	DO 25 J = 1,NS	740
	TOTN(I) = TOTN(I) + EN(J,I)	750
25	CONTINUE	760
	FMT(4)= FMT(6)	770
	RETURN	780
C		790
	ENTRY OUT2	800
C		810
C	PRESSURE	820
C		830
	DO 55 I=1,NPT	840
	K= 2*I+3	850
	FMT(K)= F4	860
	IF (PPP(I).GE.1.) FMT(K)=F3	870
	IF (PPP(I).GE.10.) FMT(K)=F2	880
	IF (PPP(I).GE.100.) FMT(K)=F1	890
55	CONTINUE	900
	WRITE (6,FMT)(FP(I),I=1,4),(PPP(J),J=1,NPT)	910
	DO 500 JAB=1,NPT	920
500	TAB(LSP,5,JAB)=PPP(JAB)*14.7*144.	
C		930
C	TEMPERATURE	940
C		950
	DO 65 I=1,NPT	960
	NV(I)= TTT(I)+.5	970
65	CONTINUE	980
	FMT(4)= FMT13	990
	FMT(5)= FMT19	1000
	WRITE (6,FMT)(FT(I),I=1,4),(NV(J),J=1,NPT)	1010
	DO 510 JAB=1,NPT	
510	TAB(LSP,6,JAB)=FLOAT(NV(JAB))*1.8	
C		1020
C	ENTHALPY	1030
C		1040

DO 75 I=1,NPT	1050
V(I) = HSUM(I) * R	1060
75 CONTINUE	1070
FMT(5)= FB	1080
FMT(7)= F1	1090
WRITE (6,FMT)(FH(I),I=1,4),(V(J),J=1,NPT)	1100
DO 515 JAB=1,NPT	
515 TAB(LST,1,JAB)=V(JAB)*1.8*778.*32.174	
C	1110
C ENTROPY	1120
C	1130
FMT(7)=F4	1140
DO 78 I = 1,NPT	1150
V(I) = SSUM(I) * R	1160
78 CONTINUE	1170
WRITE (6,FMT)(FS(I),I=1,4),(V(J),J=1,NPT)	1180
WRITE (6,80)	1190
80 FORMAT (1H)	1200
C	1210
C MOLECULAR WEIGHT	1220
C	1230
FMT(7)= F3	1240
WRITE (6,FMT)(FM(I),I=1,4),(WM(J),J=1,NPT)	1250
DO 550 JAB=1,NPT	
550 TAB(LSP,7,JAB)=WM(JAB)	
C	1260
C (DLV/DLP)T	1270
C	1280
FMT(7)=F5	1290
IF(EQL) WRITE(6,FMT)(FV(I),I=1,4),(DLVPT(J),J=1,NPT)	1300
C	1310
C (DLV/DLT)P	1320
C	1330
FMT(7)= F4	1340
IF(EQL) WRITE(6,FMT)(FD(I),I=1,4),(DLVTP(J),J=1,NPT)	1350
C	1360
C HEAT CAPACITY	1370
C	1380

DO 85 I=1,NPT	1390
V(I) = CPR(I) * R	1400
85 CONTINUE	1410
WRITE(6,FMT)(FC(I),I=1,4),(V(J),J=1,NPT)	1420
C	1430
C GAMMA(S)	1440
C	1450
WRITE(6,FMT)(FG(I),I=1,4),(GAMMAS(J),J=1,NPT)	1460
DO 540 JAB=1,NPT	
540 TAB(LSP,3,JAB)=GAMMAS(JAB)	
C	1470
C SONIC VELOCITY	1480
C	1490
FMT(7)= F1	1500
DO 95 I = 1,NPT	1510
SONVEL(I) = SQRT(RR*GAMMAS(I)*TTT(I)/WM(I))	1520
95 CONTINUE	1530
WRITE(6,FMT)(FL(I),I=1,4),(SONVEL(J),J=1,NPT)	1540
RETURN	1550
C	1560
ENTRY OUT3	1570
IF(.NOT.EQL) GO TO 331	1580
C	1590
C MOLE FRACTIONS - EQUILIBRIUM	1600
C	1610
WRITE (6,80)	1620
FMT(7)= F5	1630
WRITE(6,310)	1640
310 FORMAT(15HMOLE FRACTIONS //)	1650
DO 330 K=1,NS	1660
DO 315 I=1,NPT	1670
V(I) = EN(K,I) /TOTN(I)	1680
315 CONTINUE	1690
DO 316 I=1,NPT	1700
IF (V(I).GE.(5.E-6)) GO TO 320	1710
316 CONTINUE	1720
GO TO 330	1730
320 WRITE (6,FMT) SUB(K,1),SUB(K,2)	1740
	,FB,(V(I),I=1,NPT)

330	CONTINUE	1750
331	WRITE(6,335)	1760
335	FORMAT(118H0ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MO	1770
	LE FRACTIONS WERE LESS THAN .000005 FOR ALL ASSIGNED CONDITIONS//)	1780
	LINE= 0	1790
	DO 350 K=1,NS	1800
	DO 340 I=1,NPT	1810
	IF ((EN(K,I)/TOTN(I)).GE.(5.E-6)) GO TO 343	1820
340	CONTINUE	1830
	LINE= LINE+1	1840
	Z(LINE,1)= SUB(K,1)	1850
	Z(LINE,2)= SUB(K,2)	1860
	Z(LINE,3)= SUB(K,3)	1870
343	IF ((LINE.NE.10) .AND. K.NE.NS) GO TO 350	1880
	IF (LINE.EQ.0) GO TO 1000	1890
	WRITE(6,345) (Z(LN,1),Z(LN,2),Z(LN,3),LN=1,LINE)	1900
345	FORMAT (10(1X,3A4))	1910
	LINE= 0	1920
350	CONTINUE	1930
	IF(.NOT.MOLES) WRITE(6,360)	1940
360	FORMAT(78H0NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXI	1950
	2DANT IN TOTAL OXIDANTS)	1960
1000	RETURN	1970
	END	1980

\$ORIGIN	F	
\$IBFTC CEC55	DECK	
C		10
	SUBROUTINE CPHS	20
C	CALCULATES THERMODYNAMIC PROPERTIES FOR INDIVIDUAL SPECIES	30
C		40
	COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)	50
1	,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)	60
	COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),B0(15),BOP(15,2)	70
1	,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EGRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)	80
2	,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)	90
3	,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)	100
4	,RHOP,RMW(15),TLN	110
	COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM	120
1	,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEW,NSUB,NSUP,ITN,CPCVFR,CPCVEQ	130
2	,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1	140
C		150
	EQUIVALENCE (J,JS1)	160
C		170
	K = 1	180
	IF(TT,LE,TMID)K = 2	190
	KK = 0	200
	CPSUM=0.	210
90	IF(COEF(K,1,J).NE.0.)GO TO 97	220
	IF (IUSE(J).LT.0) GO TO 100	230
	KK = K	240
	K = 1	250
	IF (KK.EQ.1) K = 2	260
97	S(J) = (((COEF(K,5,J)/4.)*TT+ COEF(K,4,J)/3.)*TT+ COEF(K,3,J)/2.	270
1)* TT+COEF(K,2,J))*TT+ COEF(K,1,J)*TLN + COEF(K,7,J)	280
	H0(J) = (((COEF(K,5,J)/5.)*TT+ COEF(K,4,J)/4.)*TT+ COEF(K,3,J)/3.	290
1)* TT+ COEF(K,2,J)/2.)*TT+ COEF(K,1,J) + COEF(K,6,J)/TT	300
	CPSUM= CPSUM+(((COEF(K,5,J)*TT+ COEF(K,4,J))*TT+ COEF(K,3,J))*TT	310
1	+ COEF(K,2,J))*TT+ COEF(K,1,J))*EN(J,NPT)	320
	IF (KK.EQ.0) GO TO 100	330
	K = KK	340
	KK = 0	350
100	IF(J.EQ.NS) GO TO 200	360
	J=J+1	370
	GO TO 90	380
200	RETURN	390
	END	400

\$IBFTC CECS6	DECK	10
	SUBROUTINE MATRIX	20
C		30
C	DOUBLE PRECISION G,X	40
	LOGICAL HP,SP,TP,IDEBUG,CONVG,NEWR	50
C		60
	COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)	70
	1 ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)	80
	2 ,TOTN(13)	90
	COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)	100
	1 ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)	110
	COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),B0(15),BOP(15,2)	120
	1 ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)	130
	2 ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)	140
	3 ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)	150
	4 ,RHOP,RMW(15),TLN	160
	COMMON /DOUBLE/ G(20,21), X(20)	170
	COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM	180
	1 ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEWR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ	190
	2 ,IONS,NC,INSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1	200
C		210
	EQUIVALENCE (L,NLM)	220
C		230
	IQ2 = IQ1 + 1	240
	IQ3 = IQ2 + 1	250
	KMAT = IQ3	260
	IF(.NOT.CONVG.AND.TP) KMAT = IQ2	270
	IMAT = KMAT - 1	280
C		290
C	CLEAR MATRIX STORAGES TO ZERO	300
C		310
	DO 211 I=1,IMAT	320
	DO 211 K=1,KMAT	330
	G(I,K)= 0.0D0	340
211	CONTINUE	350
	SSS = 0.	360
	HSUM(NPT) = 0.	370

C		380
C	BEGIN SET UP OF ITERATION MATRIX	390
C		400
	KK = L	410
	DO 65 J=1,NS	420
	H=H0(J)*EN(J,NPT)	430
	IF (IUSE(J)) 65,11,70	440
11	F = (H0(J)-S(J)+ENLN(J)+TM)*EN(J,NPT)	450
	SS = H-F	460
	TERM1 = H	470
	IF (KMAT .EQ. IQ2) TERM1 = F	480
	DO 55 I = 1, L	490
C		500
C	CALCULATE THE ELEMENTS R(I,K)	510
C		520
	IF (A(I,J) .EQ. 0.) GO TO 55	530
	TERM= A(I,J)*EN(J,NPT)	540
	DO 15 K=1, L	550
	G(I,K)= G(I,K) + A(K,J)*TERM	560
15	CONTINUE	570
C		580
	G(I,IQ1)=G(I,IQ1)+TERM	590
	G(I,IQ2)=G(I,IQ2)+A(I,J)*TERM1	600
	IF (CONVG .OR. TP) GO TO 55	610
	G(I,IQ3)= G(I,IQ3)+A(I,J)*F	620
	IF (SP) G(IQ2,I) = G(IQ2,I) + A(I,J)*SS	630
55	CONTINUE	640
	IF (KMAT .EQ. IQ2) GO TO 64	650
	IF (CONVG .OR. HP) GO TO 59	660
	G(IQ2,IQ1) = G(IQ2,IQ1) + SS	670
	G(IQ2,IQ2)=G(IQ2,IQ2)+H0(J)*SS	680
	G(IQ2,IQ3) = G(IQ2,IQ3)+(S(J) - ENLN(J)-TM)*F	690
	GO TO 62	700
59	G(IQ2,IQ2)=G(IQ2,IQ2)+H0(J)*H	710
	IF (CONVG) GO TO 64	720
	G(IQ2,IQ3)=G(IQ2,IQ3)+H0(J)*F	730
62	G(IQ1,IQ3)=G(IQ1,IQ3)+F	740
64	G(IQ1,IQ2)=G(IQ1,IQ2)+TERM1	750

GO TO 65	760
C	770
C CONDENSED SPECIES	780
C	790
70 KK = KK + 1	800
DO 75 I = 1,L	810
G(I,KK) = A(I,J)	820
G(I,KMAT) = G(I,KMAT) - A(I,J)*EN(J,NPT)	830
75 CONTINUE	840
G(KK,IQ2) = H0(J)	850
G(KK,KMAT) = H0(J) - S(J)	860
HSUM(NPT) = HSUM(NPT) + H	870
IF(.NOT.SP) GO TO 65	880
SSS = SSS + S(J)*EN(J,NPT)	890
G(IQ2,KK) = S(J)	900
65 CONTINUE	910
SSS = SSS + G(IQ2,IQ1)	920
HSUM(NPT) = HSUM(NPT) + G(IQ1,IQ2)	930
G(IQ1,IQ1) = SUMN - ENN	940
C	950
C REFLECT SYMMETRIC PORTIONS OF THE MATRIX	960
C	970
ISYM = IQ1	980
IF(HP.OR.CONVG) ISYM=IQ2	990
DO 102 I=1,ISYM	1000
DO 102 J=I,ISYM	1010
G(J,I)=G(I,J)	1020
102 CONTINUE	1030
C	1040
C COMPLETE THE RIGHT HAND SIDE	1050
C	1060
IF(CONVG) GO TO 175	1070
DO 145 I=1,L	1080
X(1)=B0(1)-G(I,IQ1)	1090
G(I,KMAT) = G(I,KMAT)+X(1)	1100
145 CONTINUE	1110
G(IQ1,KMAT) = G(IQ1,KMAT)+ENN-SUMN	1120
C	1130

C	COMPLETE ENERGY ROW AND TEMPERATURE COLUMN	1140
C		1150
	IF (KMAT .EQ. IQ2) GO TO 185	1160
	IF (SP)ENERGY = S0+ENN-SUMN - SSS	1170
	IF(HP)ENERGY=HSUB0/TT - HSUM(NPT)	1180
	G(IQ2,IQ3)=G(IQ2,IQ3)+ ENERGY	1190
175	G(IQ2,IQ2)= G(IQ2,IQ2)+CPSUM	1200
185	RETURN	1210
	END	1220

\$IBFTC	CECS7	DECK	
	SUBROUTINE	MGAUSD	10
C			20
C	SOLVE ANY LINEAR SET OF UP TO 20 EQUATIONS		30
C			40
	DOUBLE PRECISION G,X,COEFX(20),SUM,Z		50
C			60
	COMMON/DOUBLE/G(20,21),X(20)		70
	COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM		80
	1 ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEW,NSUB,NSUP,ITN,CPCVFR,CPCVEQ		90
	2 ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1		100
C			110
	EQUIVALENCE (IUSE,IMAT)		120
C			130
	DATA BIGNO/1.E+38/		140
C			150
C	BEGIN ELIMINATION OF NNTH VARIABLE		160
C			170
	IUSE1=IUSE+1		180
	6 DO 45 NN=1,IUSE		190
	IF (NN=IUSE) 8,83,8		200
	83 IF(G(NN,NN))31,23,31		210
C			220
C	SEARCH FOR MAXIMUM COEFFICIENT IN EACH ROW		230
C			240
	8 DO 18 I=NN,IUSE		250
	COEFX(I) = BIGNO		260
	IF(G(I,NT).EQ.0.) GO TO 18		270
	COEFX(I) = 0.		280
	DO 10 J=NN,IUSE1		290
	SUM = G(I,J)		300
	IF(SUM.LT.0.) SUM=-SUM		310
	IF(J.NE.NN) GO TO 9		320
	Z = SUM		330
	GO TO 10		340
	9 IF(SUM.GT.COEFX(I)) COEFX(I)=SUM		350
	10 CONTINUE		360
	COEFX(I) = COEFX(I)/Z		370

18	CONTINUE	380
	TEMP = BIGNO	390
	I=0	400
20	DO 22 J=NN,IUSE	410
	IF (COEFX(J)-TEMP) 87,22,22	420
87	TEMP=COEFX(J)	430
	I=J	440
22	CONTINUE	450
	IF(I) 28,23,28	460
C		470
C	INDEX I LOCATES EQUATION TO BE USED FOR ELIMINATING THE NTH	480
C	VARIABLE FROM THE REMAINING EQUATIONS	490
C		500
C	INTERCHANGE EQUATIONS I AND NN	510
C		520
	28 IF(NN-I) 29,31,29	530
	29 DO 30 J=NN,IUSE1	540
	Z=G(I,J)	550
	G(I,J)=G(NN,J)	560
	G(NN,J)=Z	570
	30 CONTINUE	580
C		590
C	DIVIDE NTH ROW BY NTH DIAGONAL ELEMENT AND ELIMINATE THE NTH	600
C	VARIABLE FROM THE REMAINING EQUATIONS	610
C		620
	31 K = NN + 1	630
	DO 36 J = K, IUSE1	640
	IF(G(NN,NN).EQ.0.) GO TO 23	650
	G(NN,J) = G(NN,J) / G(NN,NN)	660
	36 CONTINUE	670
	IF(K-IUSE1) 88,45,88	680
	88 DO 44 I = K, IUSE	690
	40 DO 44 J = K, IUSE1	700
	G(I,J) = G(I,J) - G(I,NN)*G(NN,J)	710
	44 CONTINUE	720
	45 CONTINUE	730
C		740
C	BACKSOLVE FOR THE VARIABLES	750

C	K = IUSE	760
	47 J = K + 1	770
	X(K) = 0.0D0	780
	SUM = 0.0	790
	IF(IUSE - J) 51,48,48	800
	48 DO 50 I = J,IUSE	810
	SUM = SUM + G(K,I)* X(I)	820
	50 CONTINUE	830
	51 X(K) = G(K,IUSEI) - SUM	840
	K = K - 1	850
	IF (K) 47,151,47	860
	23 IUSE = IUSE-1	870
	151 RETURN	880
	END	890
		900

\$ORIGIN	E	
\$IBFTC CECS2	DECK	
C		10
	SUBROUTINE REACT	20
C		30
	DOUBLE PRECISION G,X	40
	LOGICAL HP,SP,TP,IDEBUG,CONVG,NEWR,IONS,MOLES,EQL,FROZ	50
C		60
	DIMENSION ANAME(15,5),V(15)	70
C		80
	COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),B0P(15,2)	90
	1 ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)	100
	2 ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)	110
	3 ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)	120
	4 ,RHOP,RMW(15),TLN	130
	COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM	140
	1 ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEWR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ	150
	2 ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1	160
C		170
	EQUIVALENCE (NAME,ANAME),(NLM,L)	180
C		190
	DATA MOL/1HM/,OX/1HO/,LANK/1H /,IZERO/2H00/	200
	DATA MOLE/1H /	
C		210
	DO 10 K=1,2	220
	WP(K)=0.	230
	HPP(K)=0.	240
	RHO(K)=0.	250
	VPLS(K)=0.	260
	VMIN(K)=0.	270
	AC(K)=0.	280
	AM(K)=0.	290
	DO 8 J=1,15	300
	LLMT(J)=0	310
	BOP(J,K)=0.	320
	8 CONTINUE	330
	10 CONTINUE	340
	N=1	350

L=1	360
20 CONTINUE	
21 FORMAT(5(A2,F7.5),F7.5,A1,F9.5,A1,F8.5,A1,F8.5)	390
IF(NAME(N,1).EQ.LANK) GO TO 200	400
IF(L.EQ.0)GO TO 20	410
WRITE (6,31)(NAME(N,I),ANUM(N,I),I=1,5),PECWT(N),MOLE,ENTH(N),FAZ	420
1 (N),RTEMP(N),FOX(N),DENS(N)	430
31 FORMAT(1X,5(A2,1X,F7.4,2X),F8.4,2X,A1,F11.2,2X,A1,2X,F8.3,2X,	440
1A3,3X,F8.5)	
35 IF(MOLE.EQ.MOL) MOLES=.TRUE.	460
K=2	470
IF(FOX(N).EQ.OX)K=1	480
DO 38 J=1,15	490
DATA(J) = 0.	500
38 CONTINUE	510
RM=0.	520
DO 100 JJ=1,5	530
IF(ANUM(N,JJ).EQ.0.)GO TO 101	540
DO 41 J=1,15	550
NJ = J	560
IF(LLMT(J).EQ.0) GO TO 45	570
IF(NAME(N,JJ).EQ.LLMT(J))GO TO 46	580
41 CONTINUE	590
45 L = NJ	600
LLMT(J)=NAME(N,JJ)	610
46 DO 48 KK=1,101	620
IF(ATOM(1,KK).EQ.ANAME(N,JJ))GO TO 50	630
48 CONTINUE	640
L=0	650
GO TO 20	660
50 RM=RM+ANUM(N,JJ)*ATOM(2,KK)	670
V(J)=ATOM(3,KK)	680
DATA(J)=ANUM(N,JJ)	690
100 CONTINUE	700
101 PCWT=PECWT(N)	710
IF(MOLES) PCWT=PCWT*RM	720
WP(K)=WP(K) + PCWT	730
IF(NAME(N,5).NE.IZERO)HPP(K)=HPP(K)+ENTH(N)*PCWT/RM	740

AM(K)=AM(<)+PCWT/RM	750
DO 110 J=1,L	760
BOP(J,K)=DATA(J)*PCWT/RM +BOP(J,K)	770
110 CONTINUE	780
IF(DENS(N).NE.0.)GO TO 115	790
GO TO 117	800
115 RHO(K)=RHO(K)+PCWT/DENS(N)	810
117 RMW(N) = RM	820
N = N+1	830
IF(N.NE.16) GO TO 20	840
200 NREAC =N-1	850
IF(L.EQ.0) GO TO 1000	860
DO 220 K=1,2	870
IF(WP(K).EQ.0.)GO TO 220	880
HPP(K)=HPP(K)/WP(K)	890
AM(K) = WP(K)/AM(K)	900
IF(RHO(K).NE.0.)RHO(K)=WP(K)/RHO(K)	910
DO 215 J=1,L	920
BOP(J,K)=BOP(J,K)/WP(K)	930
IF(V(J).LT.0.)VMIN(K)= VMIN(K)+BOP(J,K)*V(J)	940
IF(V(J).GT.0.)VPLS(K)=VPLS(K)+BOP(J,K)*V(J)	950
215 CONTINUE	960
IF(MOLES) GO TO 220	970
DO 218 N=1,NREAC	980
IF(FOX(N).EQ.OX.AND.K.EQ.2) GO TO 218	990
IF(FOX(N).NE.OX.AND.K.EQ.1) GO TO 218	1000
PECWT(N) = PECWT(N)/WP(K)	1010
218 CONTINUE	1020
220 CONTINUE	1030
NEWR=.TRUE.	1040
DO 230 N = 1,NREAC	1050
IF (DENS(N).NE.0.) GO TO 230	1060
RHO (1) = 0.	1070
GO TO 1000	1080
230 CONTINUE	1090
1000 RETURN	1100
END	1110

\$IBFTC CECS3	10
SUBROUTINE SEARCH	10
C	20
C SEARCH TAPE FOR THERMO DATA FOR SPECIES TO BE CONSIDERED	30
INTEGER SUB,OMIT,END	40
C	50
LOGICAL NEWR	60
C	70
DIMENSION DATE(2,3),MT(4),B(4),OMIT(3,3)	80
C	90
COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)	100
1 ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)	110
COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),BO(15),BOP(15,2)	120
1 ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)	130
2 ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)	140
3 ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)	150
4 ,RHOP,RMW(15),TLN	160
COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM	170
1 ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEWR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ	180
2 ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1	190
C	200
EQUIVALENCE (DATE,EN),(OMIT,ENLN),(ENDD,END),(L,NLM)	210
COMMON/TAPE/IPROT	220
C	230
DATA GAS/1HG/,END/3HEND/	240
C	250
NC= 0	260
IX= 0	270
COEF(1,1,1) = ENDD	280
I = 1	290
DO 3 I=1,150	300
IF(A(1,I).EQ.ENDD) GO TO 4	310
DO 3 J=1,L	320
A(J,I) = 0.	330
3 CONTINUE	340
4 MAXNS = I	
REWIND 8	
REWIND 10	

GO TO 50	
IF(IPROT.EQ.1)GO TO 50	
READ(8)TLOW,TMID,THIGH	
5 FORMAT (3F10.3)	370
NS = 1	380
7 READ(8) (SUB(NS,I),I=1,2),DATE(1,NS),DATE(2,NS),(MT(J),B(J),	
1 J=1,4),PHAZ,T1,T2	
10 FORMAT(2A6,6X,2A3,4(A2,F3.0),A1,2F10.3)	410
IF(SUB(NS,1).EQ.END) GO TO 171	420
READ(8) ((COEF(I,J,NS),J=1,7),I=1,2)	
GO TO 75	
50 CONTINUE	
READ(10,5)TLOW,TMID,THIGH	
NS = 1	
8 CONTINUE	
READ(10,10) (SUB(NS,I),I=1,2),DATE(1,NS),DATE(2,NS),(MT(J),B(J),	
1 J=1,4),PHAZ,T1,T2	
IF(SUB(NS,1).EQ.END) GO TO 171	
READ(10,20) ((COEF(I,J,NS),J=1,7),I=1,2)	
75 CONTINUE	
20 FORMAT (5E15.8)	440
IF(NOMIT.EQ.0) GO TO 810	450
DO 805 I=1,NOMIT	460
DO 804 J=1,3	470
IF(OMIT(J,I).NE.SUB(NS,J)) GO TO 805	480
804 CONTINUE	490
GO TO 8	
IF(IPROT.EQ.1)GO TO 8	
GO TO 7	500
805 CONTINUE	510
810 DO 820 K=1,4	520
IF(B(K).EQ.0.) GO TO 825	530
DO 168 I=1,L	540
IF(LLMT(I).EQ.MT(K)) GO TO 820	550
168 CONTINUE	560
DO 819 J=1,L	570
819 A(J,NS) = 0.	580
GO TO 8	

IF(IPROT.EQ.1)GO TO 8	
GO TO 7	590
820 A(I,NS)= B(K)	600
825 IF(NS.EQ.MAXNS) GO TO 870	610
IUSE(NS)= 0	620
IF(PHAZ.EQ.GAS) GO TO 170	630
NC= NC+1	640
TEMP(NC,1)= T1	650
TEMP(NC,2)= T2	660
IX= IX+1	670
IF(IUSE(NS-1).EQ.0 .OR. NC.EQ.1) GO TO 145	680
DO 830 I=1,L	690
IF(A(I,NS).NE.A(I,NS-1)) GO TO 145	700
830 CONTINUE	710
IX= IX-1	720
145 IUSE(NS)= -IX	730
170 NS= NS+1	740
GO TO 8	
IF(IPROT.EQ.1)GO TO 8	
GO TO 7	750
870 WRITE(6,871) (SUB(NS,J),J=1,2)	
871 FORMAT (45HODIMENSIONS IN/SPECES/TOO SMALL TO CONSIDER ,2A6)	770
GO TO 8	
IF(IPROT.EQ.1)GO TO 8	
GO TO 7	780
171 NS= NS-1	790
NEWNR= .FALSE.	800
WRITE(6,172)	810
172 FORMAT(42HOSPECIES BEING CONSIDERED IN THIS SYSTEM	820
DO 174 I=1,NS,5	830
I5= I+4	840
IF(NS.LT.I5) I5=NS	850
174 WRITE (6,176)(DATE(1,J),DATE(2,J),SUB(J,1),SUB(J,2)	8
1 I5)	870
176 FORMAT(5(5X,2A3,2X,2A6))	88
RETURN	890
END	900

,J=1,

```

$DATA
      3      3      0      0      0      0      1
+•0314      +•1      +20•0      +0•0
+•314      +20•      +0•0      +100•
H +13•0220 2•17040N 4•34070
N 2•173600 4•3472
      10•      11•      12•      1•0

```

```

F L      •5      -5900•      298•15
O L      •5      +27560•      298•15

```

(2) NMIX= 2 (1) NPTS= 5 TRIAL RUN SIMULATION SELECTION
 IP= 0 IT= 0 IG= 0 IFLG1= 0 ITYPE= 1

(3) NOZZLE GEOMETRY FOLLOWS

THRJET AREA	THRJET RADIUS	AREA RATIO	LIP ANGLE
0.314E-01	0.100E 00	0.200E 02	0.000E-38

(4) - - - - -

INITIAL CHAMBER TEMP= 0.100E 04 PRESSURE= 0.200E 03

(5) PROTOTYPE INFORMATION

RADP= 0.314E 00AETP= 0.200E 02ANGP= 0.000E-38PREP= 0.100E 03

(6) REGION OF PLUME TO BE DUPLICATED

XP1= 0.100E 02 XP2= 0.110E 02 XP3= 0.120E 02

(7)

ERROR MULTIPLICATION FACTOR = 0.100E 01

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LMSC/HREC D162424

```
PC= 100 0 PSIA
JAS= V0 *****
```

CHEMICAL FORMULA
FUEL H ***** 0 2.17040
OXIDANT V 2 17350 0 + 34720

WT FRACTION (SEE NOTE)	ENTHALPY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
*****	-5900.000	L	298.15	-0.0000
*****	27560.000	L	298.15	-0.0000

Ø/F= 1.0000 PERCENT FUEL= 50.0000 EQUIVALENC RATIO= 0.9445 DENSITY= -0.0000

[illegible]

1	H2	H2	0.736E-01	0.736E-01
---	----	----	-----------	-----------

1	H20 Q000	0.02+5>	H20 H02	Q000	0 00003	0.482E-00	H2 Q000	0.07756	H20 Q000	0.48203
4	J Q000	0 00001	N2 N2	Q000	0 30077	0 301E-00	N2 Q000	0.01412	N02 Q000	0.00001
8	2H Q000	0.01225	2H 2H	Q000	0 03036	0 504E-01	2L Q000	0.03222		

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MFLC FRACTIONS WERE LESS THAN 000005 FOR ALL ASSIGNED CONDITIONS

4210 _____ 0000 H2O1 _____ 0000 VH _____ 0000 VMO _____ 0000 NM1 _____ 0000 N2H4 _____ 0000 N2O _____ 0000 N2O4 _____ 0000 _____
 VOT= WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

(9)

H FT2/S2	A/A*	GAMMA	M NO.	P PSF	T DEG R	MOL WT
0.499E 07	-0.000E- 9	0.122E 01	0.000E-35	0.144E 05	0.565E 04	0.200E 02
-0.273E 07	0.100E 01	0.122E 01	0.100E 01	0.806E 04	0.508E 04	0.200E 02
-0.271E 04	0.402E 0	0.125E 01	0.267E 01	0.576E 05	0.306E 04	0.200E 02

(10)

PROTOTYPE EXIT PLANE REYNOLDS NO. IS 0.230E 05

(11)

ORIGIN OF SOURCE FLOW AT X=-0.121E 00

(12)

WITH THETA= 0.148E 01

(13)	(14)	(15)	(16)	(17)	(18)	(19)	(20)	(21)
------	------	------	------	------	------	------	------	------

S2	MACH NO	Re NO	GAMMA	KNUDSEN NO	T0	T	P0	P
----	---------	-------	-------	------------	----	---	----	---

0.499E 07	0.4793E 01	0.3874E 05	0.1322E 01	0.1415E-04	0.7124E 04	0.1598E 04	0.6535E 04	0.6018E 02
0.7617E 01	0.3774E 01	0.0129E 05	0.1344E 01	0.4561E-03	0.7124E 04	0.1018E 04	0.6585E 04	0.2535E 02
0.1043E 07	0.6585E 01	0.3232E 05	0.1356E 01	0.7323E-03	0.7124E 04	0.8038E 03	0.6585E 04	0.7098E 01

(22)

PROTOTYPE CONDENSATION OCCURS AT 0.502E 03

(23) THERMAL ROCKET PERFORMANCE ASSUMING FROZEN COMPOSITION DURING EXPANSION

AT ALL ASSIGNED TEMPERATURE

P₀ = 200.0 PSIA
CAS. NO. 1

CHEMICAL FORMULA
FJ L C 1.00000 F 4.00000
FJ L V 2.00000
FJ L C 1.00000 J 2.00000

WT FRACTION (SEE NOTE)	ENTHALPY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
*****	-217200.000	G	298.15	-0.0000
*****	0.000	G	298.15	-0.0000
*****	-94051.800	G	298.15	-0.0000

Y/F= 0.0000 PERCENT FULL=***** EQUIVALENCE RATIO= 1.0000 DENSITY= 0.0000

	CHAMBER	THROAT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT
P ₀ /P	1.000	1.776	25.000	300.000	1000.00	2000.00	3000.00	4000.00	5000.00	7000.00
P, ATM	13.61	7.664	0.5444	0.0454	0.0136	0.0068	0.0045	0.0034	0.0027	0.0019
T, DEG K	1000	907	563	339	258	219	198	184	174	159
T, CAL/G	-1242.2	-1267.7	-1356.7	-1408.0	-1424.6	-1432.3	-1436.2	-1438.8	-1440.6	-1443.2
S, CAL/(G)(K)	1.4026	1.4026	1.4026	1.4026	1.4026	1.4026	1.4026	1.4026	1.4026	1.4026
M, MOL WT	+2.793	+2.793	42.793	42.793	42.793	42.793	42.793	42.793	42.793	42.793
S ₀ , CAL/(G)(K)	0.2767	0.2715	0.2434	0.2123	0.1977	0.1898	0.1855	0.1825	0.1803	0.1770
GAMMA (S)	1.2017	1.2053	1.2358	1.2799	1.3070	1.3238	1.3340	1.3413	1.3470	1.3556
STN VEL, M/SEC	483.2	+61.1	367.8	290.5	256.1	237.2	226.5	219.0	213.3	204.8
MACH NUMBER	0.000	1.000	2.660	4.054	5.823	5.316	5.625	5.955	6.041	6.332
OSTAR, FT/SEC		2227	2227	2227	2227	2227	2227	2227	2227	2227
UF		0.579	442	1.735	1.820	1.858	1.877	1.889	1.898	1.910
AE/AT		1.000	1.120	1.475	59.85	99.32	133.4	154.3	193.1	246.1
IVAC, LB-SEC/LB		86.0	111.2	125.8	130.1	132.0	133.0	133.6	134.1	134.7
I, LB-SEC/LB		47.0	99.8	120.1	126.0	128.6	129.9	130.8	131.4	132.2
STISP		0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0

MOLE FRACTIONS

1	CF4	CF4	0.145E-00	0.145E-00
2	CHF3	CHF3	0.995E-01	0.995E-01
3	C2F2	C2F2	0.145E-00	0.145E-00
4	N2	N2	0.611E-00	0.611E-00
5	O2	O2	0.0995E-01	0.0995E-01
6	N2F2	N2F2	0.14471	0.14471
7	N2O	N2O	0.61103	0.61103

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN .000005 FOR ALL ASSIGNED CONDITIONS

(S)	0000 CF	0000 CF2	0000 CF3	0000 CN	0000 CV2	0000 C4	0000 C8F	0000 C2	0000 C2F2	0000
C1	0000 C2N2	0000 C2O	0000 C2F	0000 F	0000 FCN	0000 F8	0000 F82	0000 F2	0000 N	0000
V	0000 NF2	0000 NF3	0000 N8	0000 N8F	0000 N82	0000 N8ZF	0000 N2C	0000 N2O	0000 N2O4	0000
3	0000 O2	0000								

NOTE: WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

(24)

(30)

H FT ² /S ²	A/A*	GAMMA	M NØ.	P PSF	T DEG R	MØL WT
-0.560E 03	-0.000E-19	0.120E 01	0.000E-33	0.289E 05	0.180E 04	0.428E 02
-0.571E 08	0.100E 01	0.121E 01	0.100E 01	0.162E 05	0.163E 04	0.428E 02
-0.511E 08	0.412E 01	0.124E 01	0.266E 01	0.115E 04	0.101E 04	0.428E 02
-0.534E 04	0.247E 02	0.128E 01	0.405E 01	0.960E 02	0.610E 03	0.428E 02

(25)

TABLE OF THERMODYNAMIC PROPERTIES FOR COMPONENT 1

H FT ² /S ²	A/A*	GAMMA	M NØ.	P PSF	T DEG R	MØL WT
-0.101E 09	-0.000E-19	0.111E 01	0.000E-38	0.288E 05	0.180E 04	0.733E 02
-0.102E 09	0.100E 01	0.111E 01	0.100E 01	0.168E 05	0.170E 04	0.733E 02
-0.105E 09	0.483E 01	0.112E 01	0.261E 01	0.115E 04	0.129E 04	0.733E 02
-0.107E 09	0.350E 02	0.113E 01	0.374E 01	0.960E 02	0.977E 03	0.733E 02

(26)

TABLE OF THERMODYNAMIC PROPERTIES FOR COMPONENT 2

H FT ² /S ²	A/A*	GAMMA	M NØ.	P PSF	T DEG R	MØL WT
-0.110E 08	-0.000E-19	0.130E 01	0.000E-38	0.288E 05	0.180E 04	0.302E 02
-0.127E 08	0.100E 01	0.132E 01	0.100E 01	0.156E 05	0.156E 04	0.302E 02
-0.175E 08	0.354E 01	0.135E 01	0.271E 01	0.115E 04	0.805E 03	0.302E 02
-0.200E 08	0.184E 02	0.139E 01	0.440E 01	0.960E 02	0.407E 03	0.302E 02
-0.207E 08	0.423E 02	0.139E 01	0.539E 01	0.288E 02	0.292E 03	0.302E 02

SIMULANT RN AT EXIT = 0.104E 06

GROUP 11

- ORIGIN OF SOURCE FLOW AT X= 0.136E-01 WITH THETA= 0.160E 01

GROUP 12

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S2	MACH NØ	RE NØ	GAMMA	KNUDSEN NØ	TØ	T	PO	P
0.1394E 01	0.4681E 01	0.5738E 08	0.1304E 01	0.2587E-05	0.2113E 04	0.4878E 03	0.1923E 05	0.1278E 03
0.2239E 01	0.5592E 01	0.8812E 07	0.1333E 01	0.8181E-05	0.2236E 04	0.3602E 03	0.1494E 05	0.3548E 02
0.3183E 01	0.6433E 01	0.4103E 07	0.1356E 01	0.2129E-04	0.2331E 04	0.2785E 03	0.1221E 05	0.9935E 01
0.4078E 01	0.7105E 01	0.2753E 07	0.1356E 01	0.3494E-04	0.2331E 04	0.2336E 03	0.1221E 05	0.3676E 01

SIMULANT CONDENSATION PT. IS 0.225E 02

LMSC/HREC D162424